

# NOx Modelling and Emission Reduction

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## Outline / Introduction

- Current models for biomass combustion
- Realized projects for small scale furnaces
- Ongoing development
  - New technology with low oxygen concentration in the fuel bed
- Areas of model improvement
  - Gas phase reaction modelling
  - Volatiles release behaviour
- Example of current development
- Summary / Outlook



# Current models for biomass combustion

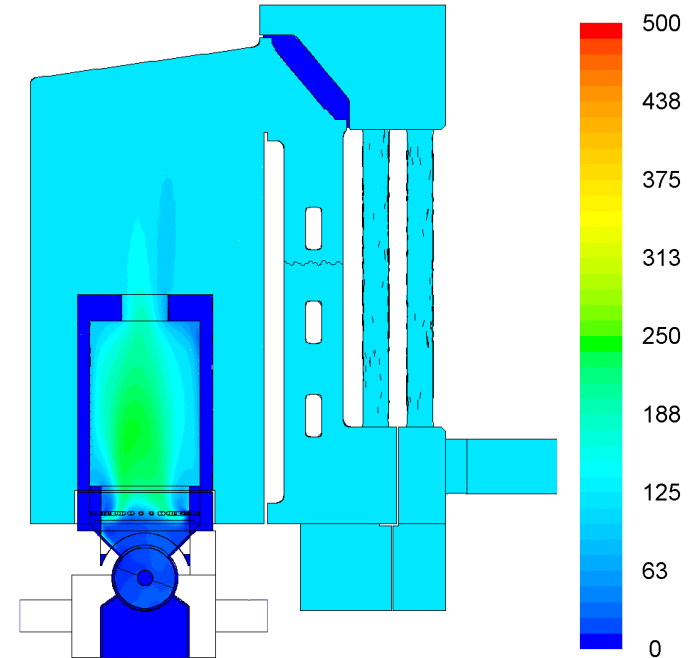
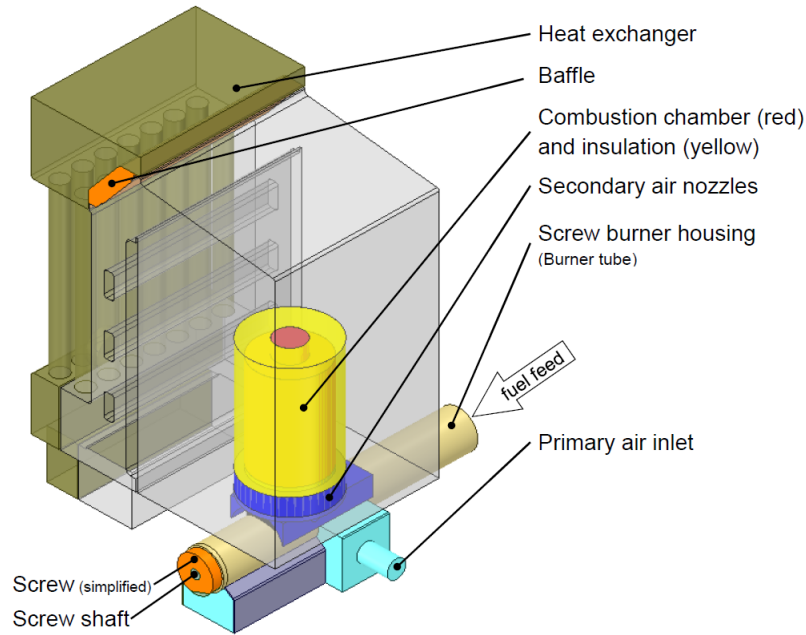
used at BEST research

- Our current models are developed for typical reducing conditions in the fuel bed ( $\lambda_{prim} = 0.6 - 0.9$ ) of furnaces with air staging.
- The gas phase reactions are modelled via a skeletal reaction mechanism (29 species, 104 reactions).
- The solid biomass is modelled as a discrete phase via representative particles.
- The thermal degradation of the representative particles is realized via a layer approach, where each layer represents a distinct process (drying, pyrolysis, char burnout).
- The models are applied for small and large scale furnaces (30kW – 40MW).



# Realized projects with the current models

## 30 kW screw burner with combustion conditions



Contours of NOx [ppm dry]



# Ongoing development

## for low oxygen concentrations in the fuel bed - I

- The combustion of cheap fuels with higher nitrogen contents and new legal regulations require a further reduction of NOx and particulate emissions for biomass furnaces.
- For small scale furnaces secondary measures are currently too expensive.
- Therefore new technologies which apply cheaper primary measures are under development → double air staging with flue gas recirculation (FGR)



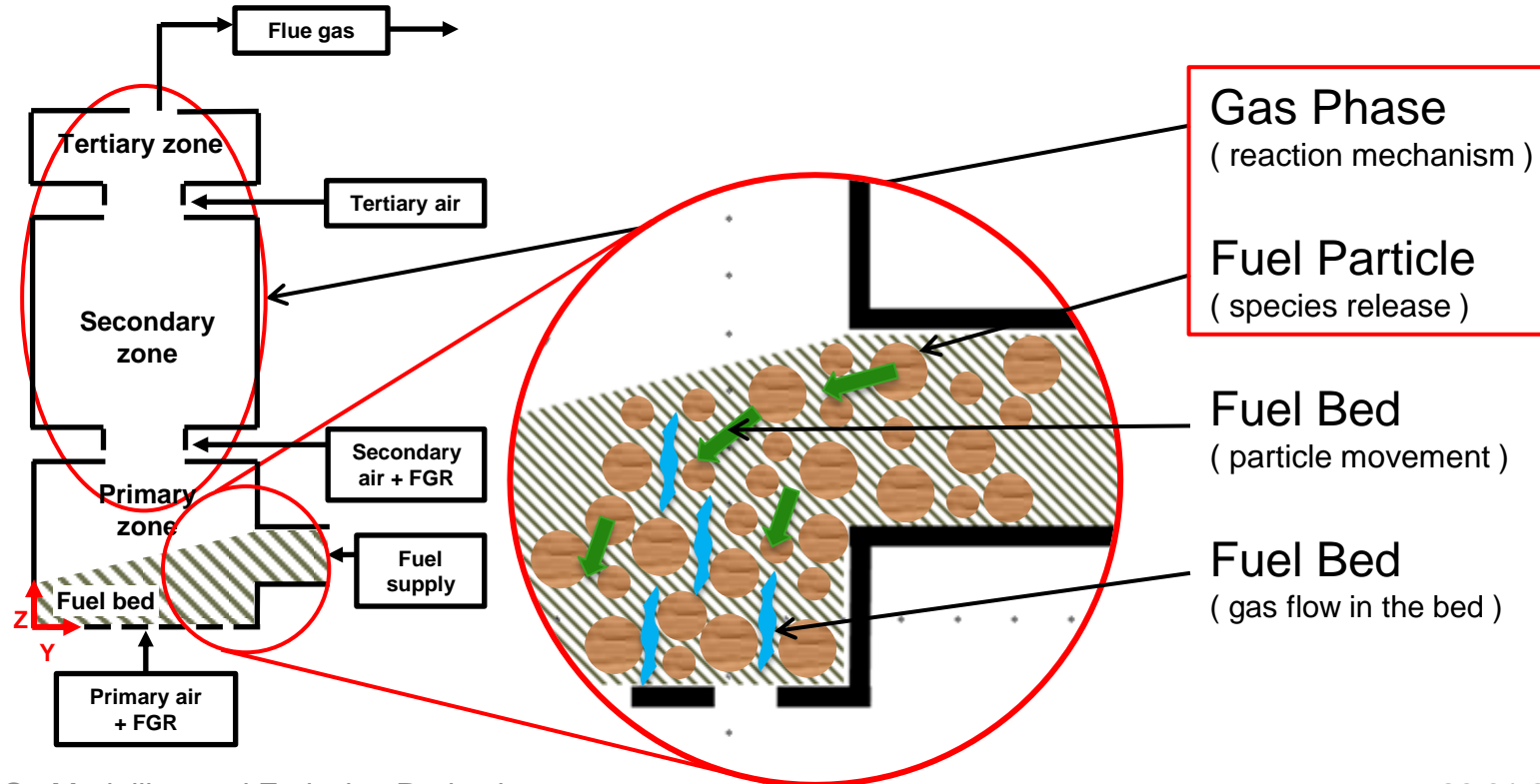
# Ongoing development

## for low oxygen concentrations in the fuel bed - II

- Advantages:
  - Reduced particulate matter (fine dust) emissions and slag formation due to lower fuel bed temperatures
  - Reduced NO<sub>x</sub> emissions due to reducing conditions in the primary and secondary combustion zone
- Disadvantages:
  - Tar formation and cracking has to be considered → higher reaction times are needed
  - Soot formation and decomposition has to be considered
  - Increased fuel bed height → slow response, sluggish combustion



# Areas of model improvement for low oxygen conditions in the fuel bed

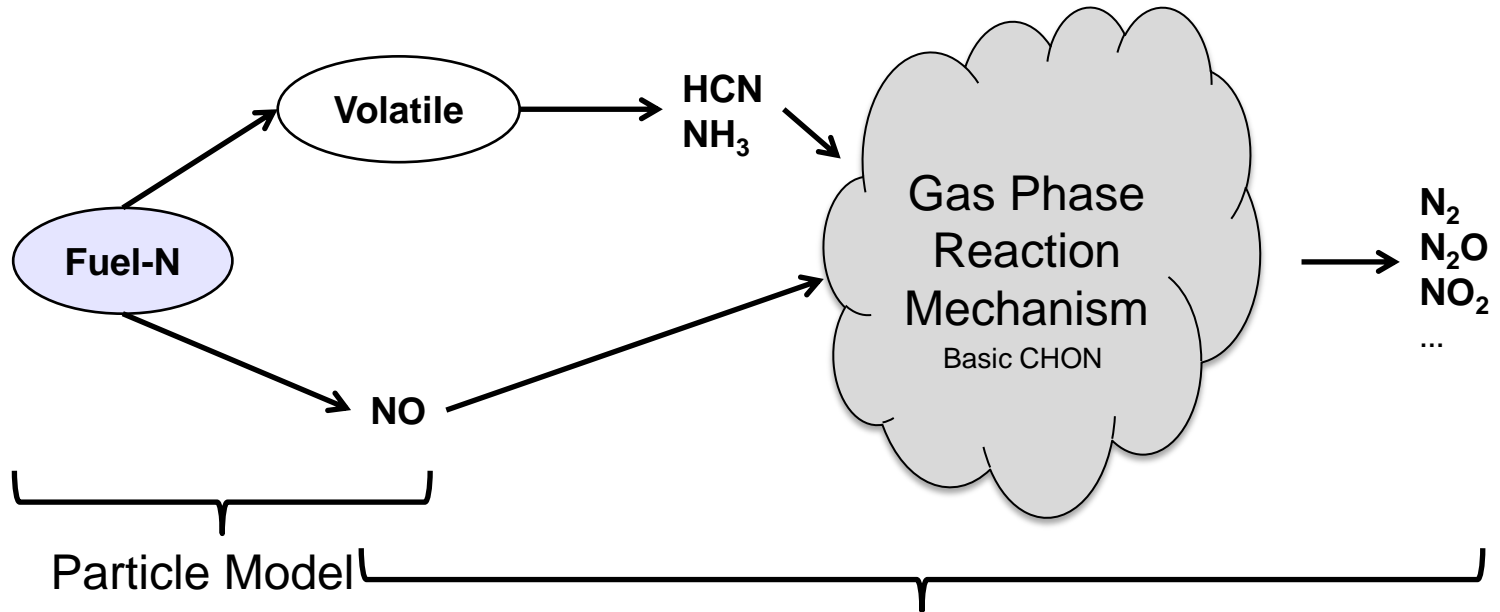




# Modelling the gas phase

reaction mechanism – applied in projects

APPLIED



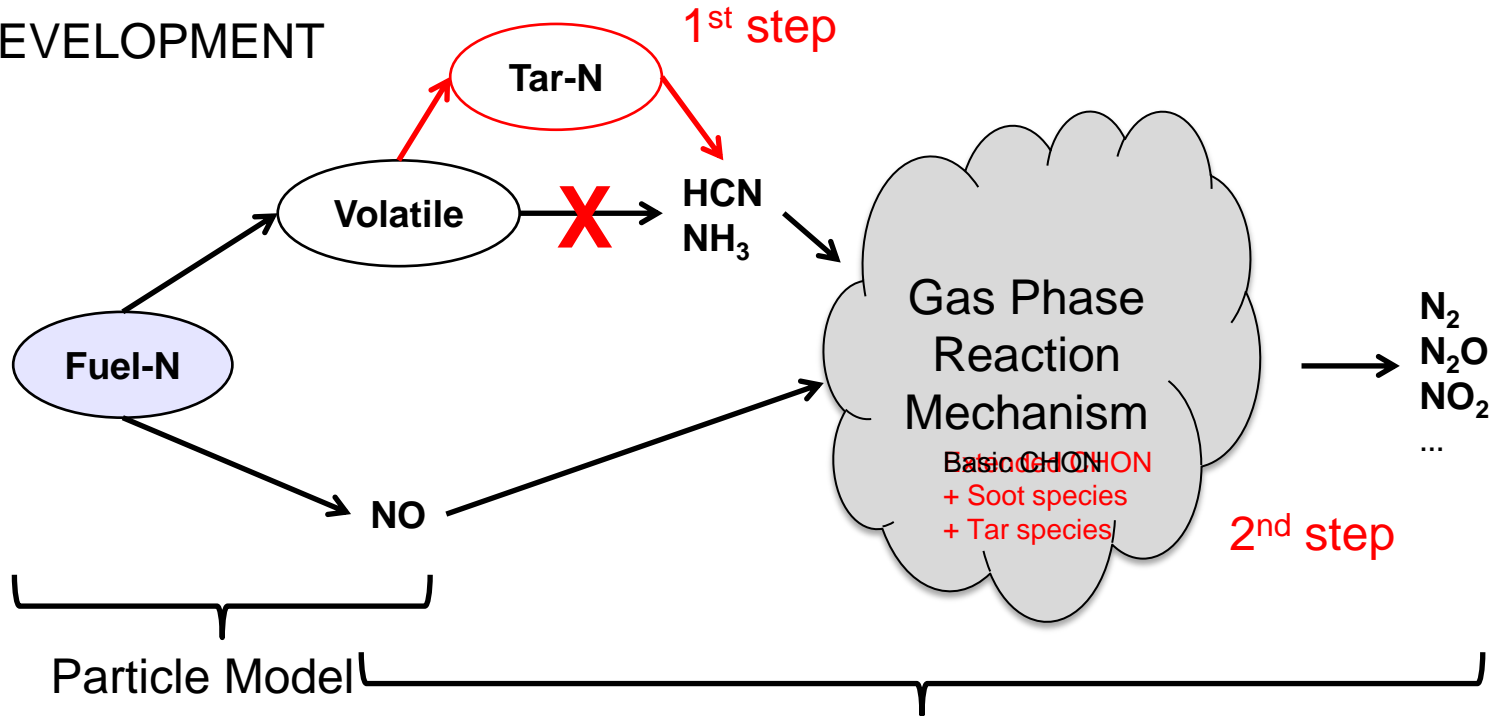




# Modelling the gas phase

reaction mechanism – under development

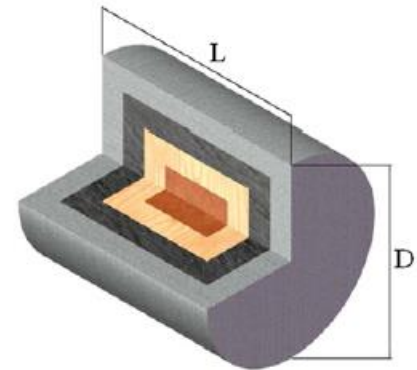
DEVELOPMENT





# Modelling the fuel particles species release

- The layer approach for the representative particles is adopted.
- The currently applied models are developed for combustion conditions.
- The intra particle transport processes, reactions and species release have to be adapted to describe the gasification conditions in the bed:
  - The char gasification reactions have to be adapted and extended



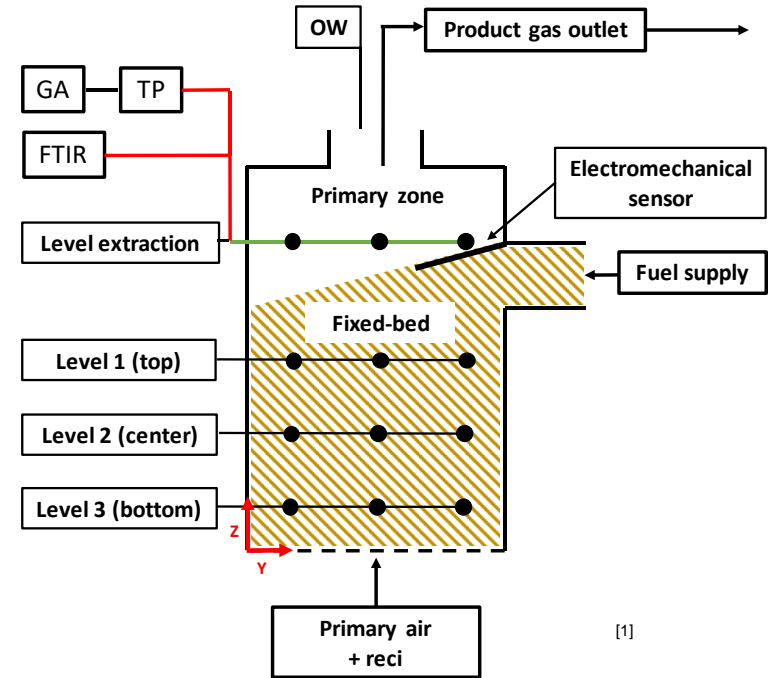


# Example of current development

## small scale application - experimental test run

### Operating conditions

- Fuel: spruce wood chips
- Moisture content: 8.04 m.%w.b.
- Fuel-N: > 0.1 m.%d.b.
- Fuel flow rate: 6.78 kg/h w.b.
- Primary air ratio: 0.2
- Secondary air ratio: 0.8
- Total air ratio: 1.8



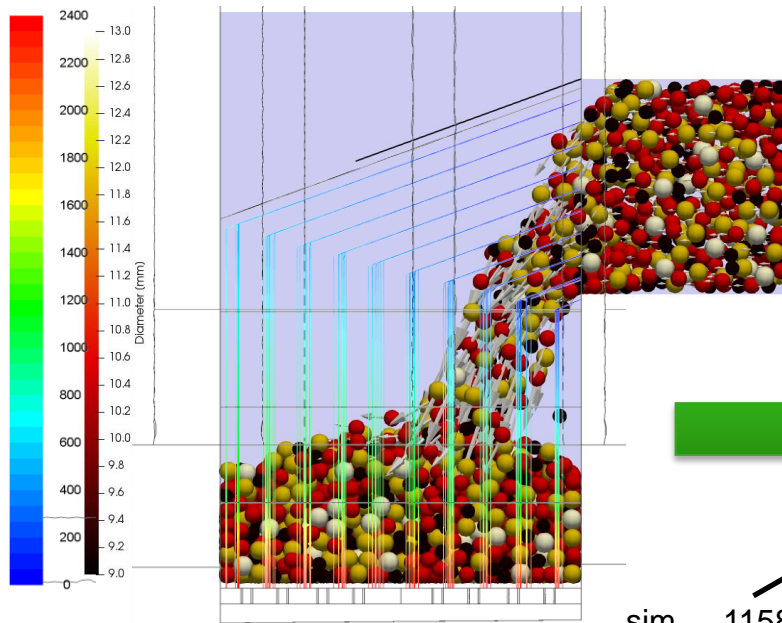
[1]



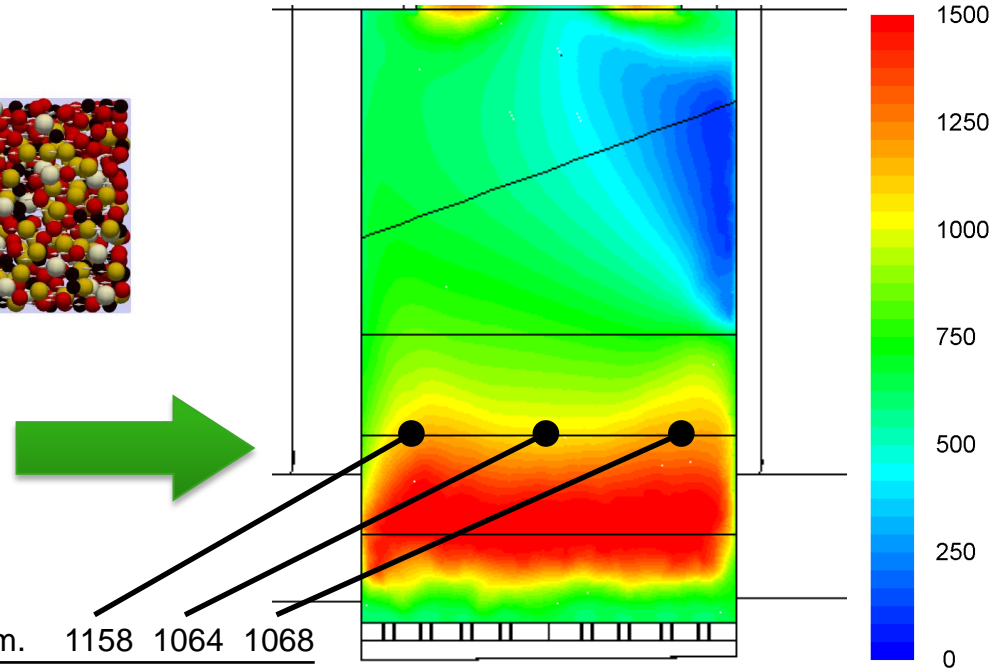
# Example of current development

## small scale application - modelling process and simulation results

Residual Element Simulation [s]



Temperature distribution [C]



sim.	1158	1064	1068
exp.	928	1057	1037



## Summary / Outlook

- The experiments showed promising results and the technology outperforms the state of the art concerning NO<sub>x</sub> emissions. [2]
- The current simulation models that are designed for combustion conditions were adapted.
  - Extension of the gas phase reaction mechanism to include tar, C<sub>2</sub>H<sub>4</sub> and soot species.
  - Adaption of the intra particle reactions and species release from the particle model.
- These modifications will then give a better match with the measured data and consequently support the understanding of the processes in the plant.