


# BEST Centre's Day 2024

26. September 2024



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# GreenCarbon Lab, Lab-scale Pyrolysis





## Green Carbon Liquids: Staged Condensation from Lab-Scale Pyrolysis

BEST – Center's Day  
Graz, 26.09.2024

Goxhabelli Ana  
Area 1.1 Thermochemical Technologies



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# Pyrolysis Plant – Lab Scale

Feedstock: Poplar Wood Pellets



Staged Condensation Unit



# Staged Condensation



## Setup Parameters

1 <sup>st</sup> Condenser	2 <sup>nd</sup> Condenser	3 <sup>rd</sup> Condenser
80°C	R.T.	-20°C

- Condensable Gases from the pyrolysis process are separated based on their *boiling points*
- As the vapors are gradually cooled, *different compound* will condense at *different T*
- Improved efficiency of separation

# Products from Staged Condensation



Oily Fraction (80°C)



Aqueous Fraction (R.T)



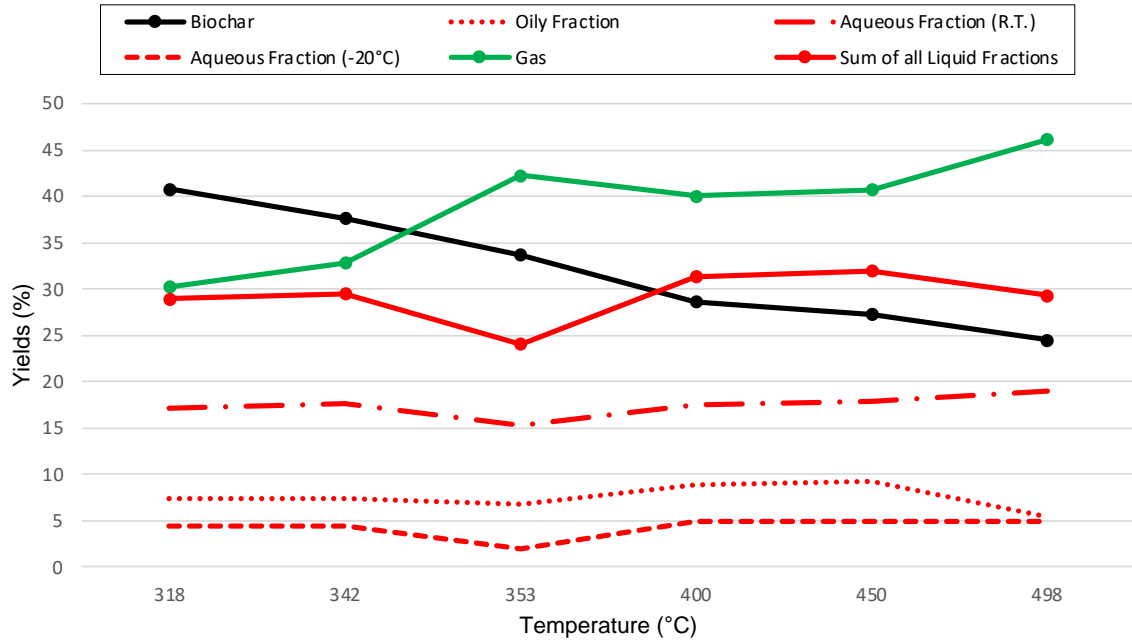
Aqueous Fraction (-20°C)



# Products from Staged Condensation



Product Yields



**GAS FRACTION** → Increases with T

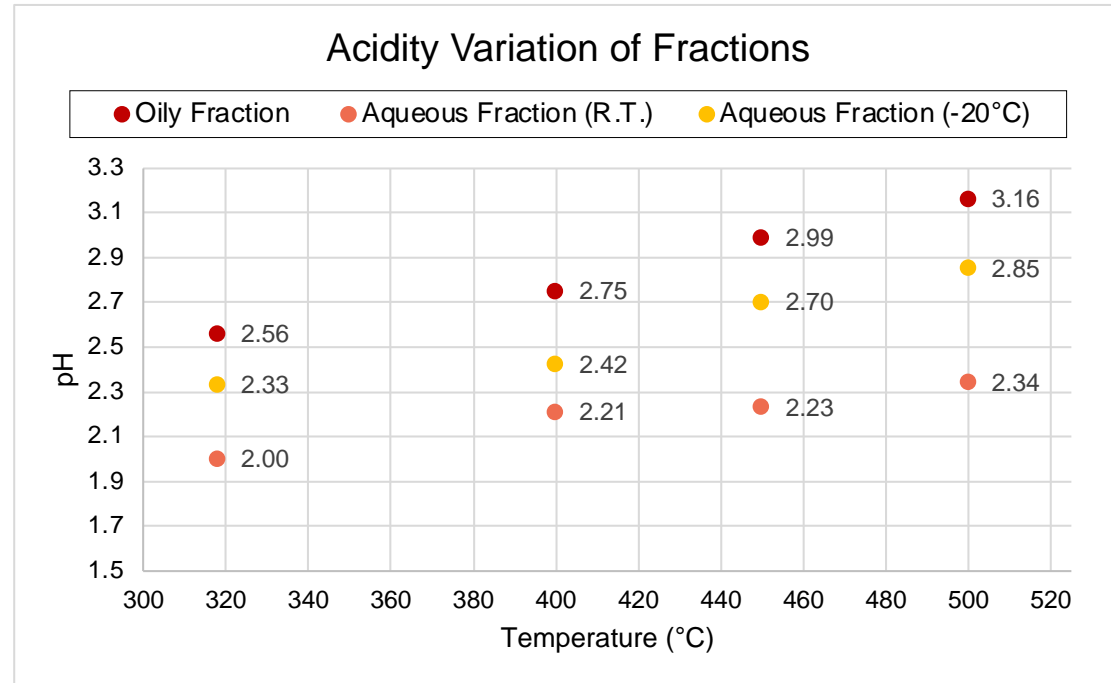
**LIQUID FRACTIONS** → Increase with T

**BIOCHAR** → Decreases with T

# Products Properties - Acidity



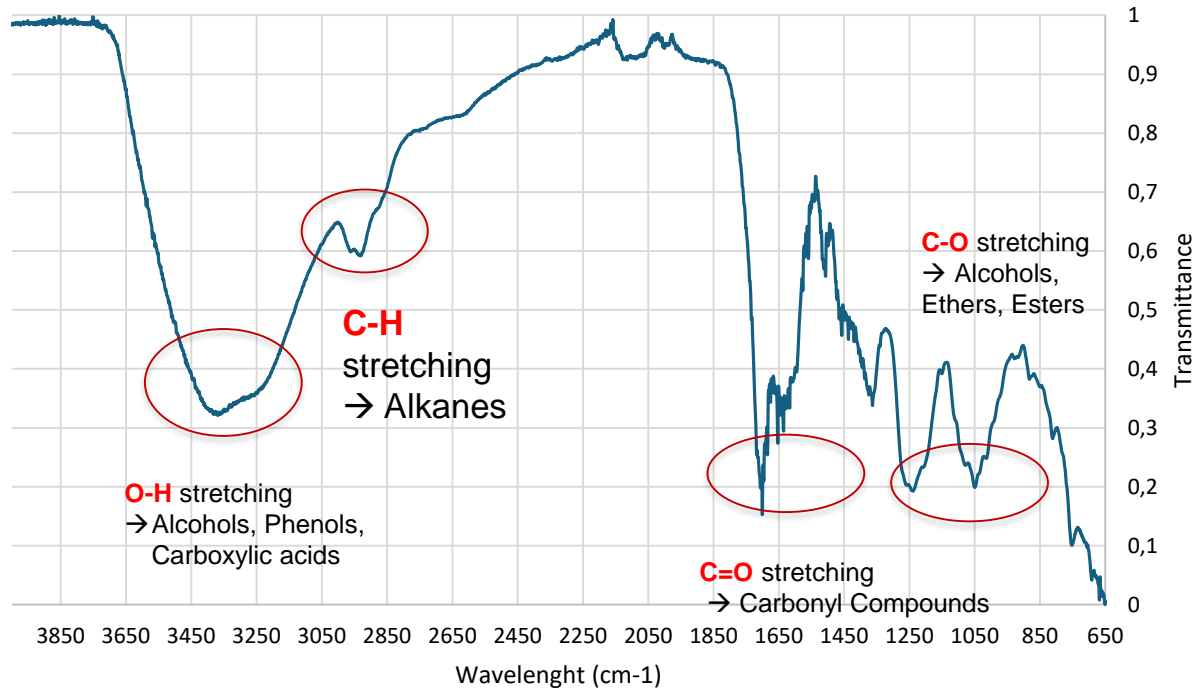
- At lower T → higher yields of oxygenated compounds, like carboxylic acids, which lower the bio-oil's pH
- Higher T → reduced acidic components and higher bio-oil's pH



# Spectral Analysis of Oily Fraction



Oily fraction IR Spectrum



Main components from literature:

- ORGANIC ACIDS
- KETONES
- ESTERS
- ALDEHYDES
- ALKANES COMPOUNDS
- PHENOLS and DERIVATES

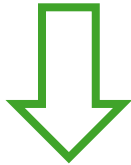


# Aging Effect: FT-IR investigation

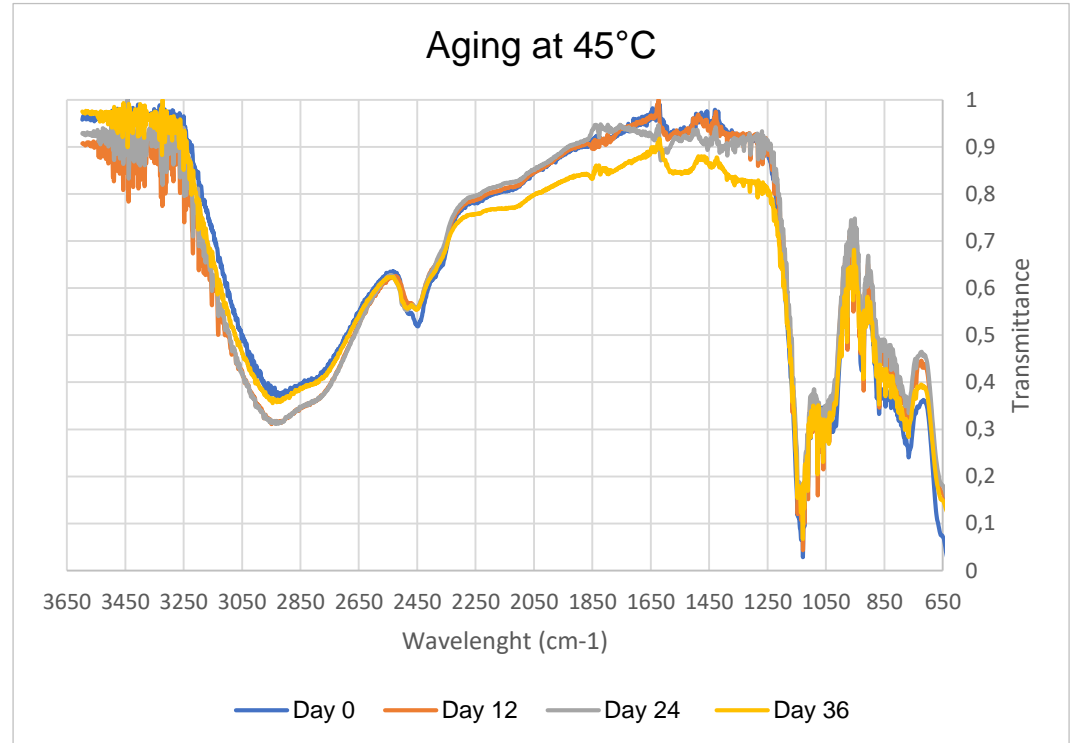


FT-IR analysis has been explored as a method to assess the **Aging Effect** of Bio-oil

Over time a decrease in transmittance is observed...



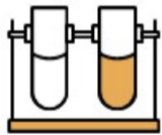
**... ONGOING INVESTIGATION**



# Conclusions and Future Work



**Increased efficiency in fraction separation**



**Enhanced Production of different condensate liquids for specific application**



**Improving of Temperature Control to achieve purer fraction**




# Green Gas – Green Heat for Industry from Biogenic Waste

Graz, 26.09.2024

Jascha Keifenheim



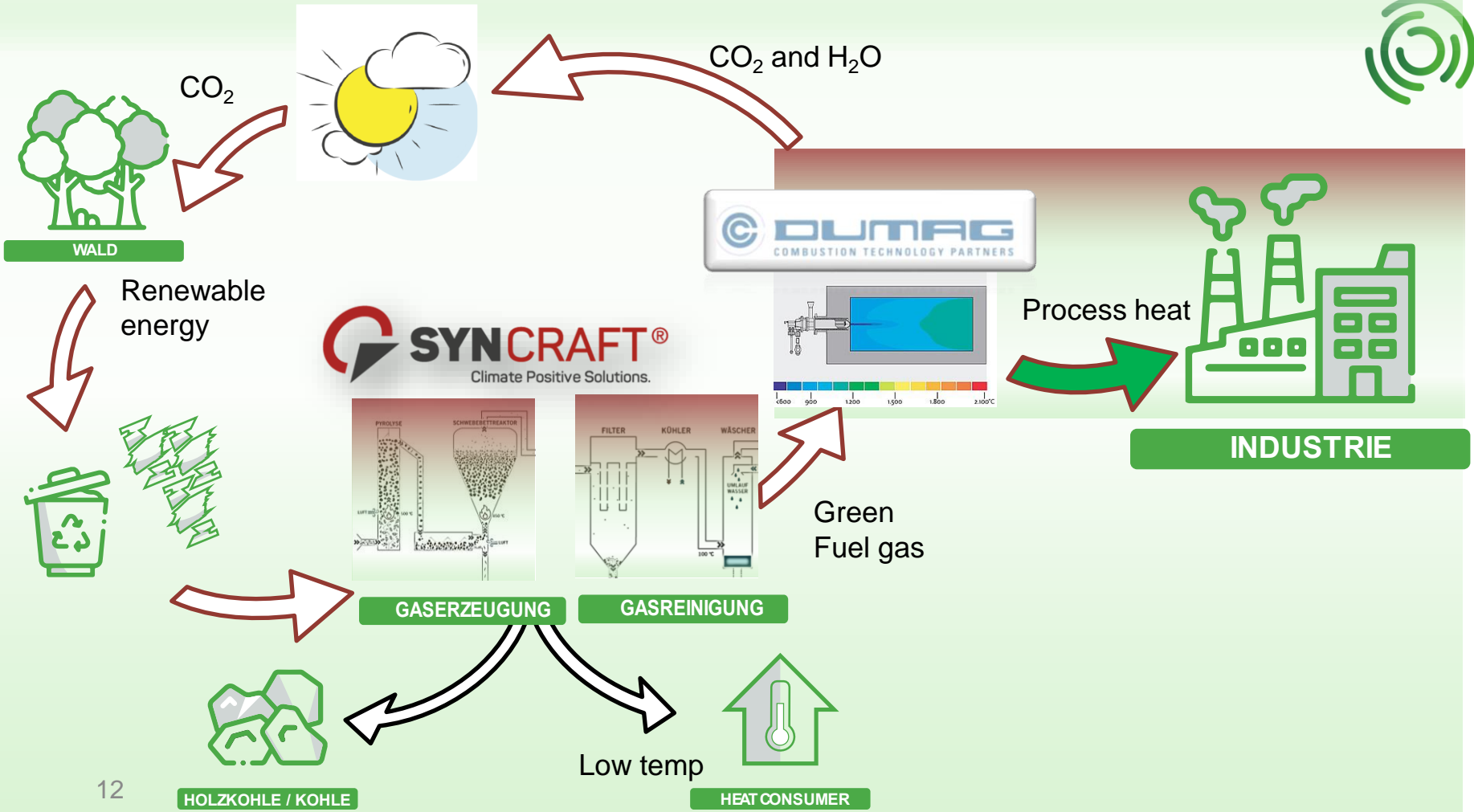
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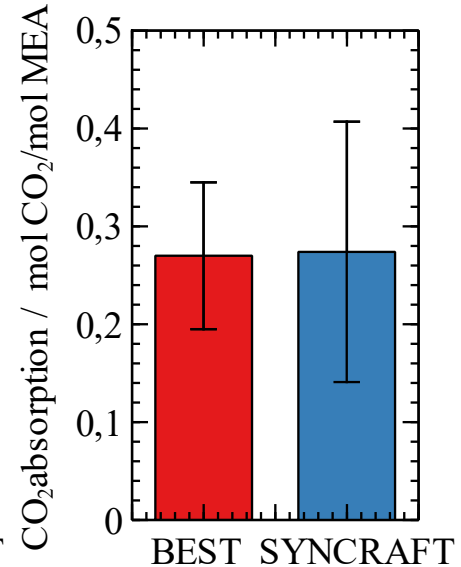
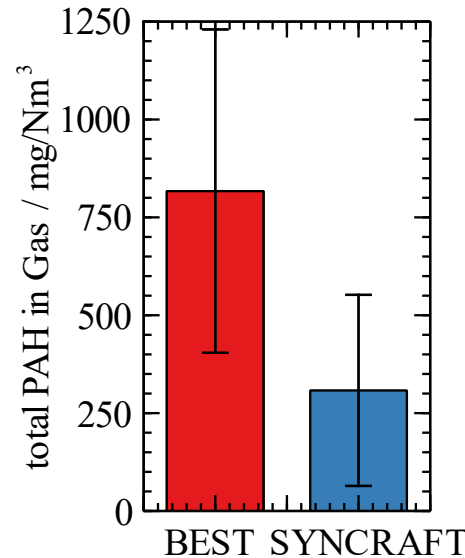
Gas Cleaning

**CO<sub>2</sub> and PAH Removal for  
Enhanced Gas Usability and  
Heating Value**

# PAH-Dependency on CO<sub>2</sub> Absorption



- More PAHs in the BEST gasifier
- Average absorption in BEST and SYNCRAFT gasifiers similar
- CO<sub>2</sub> absorption not PAH-dependent
- Proven concept of pre combustion CO<sub>2</sub> removal from the syngas

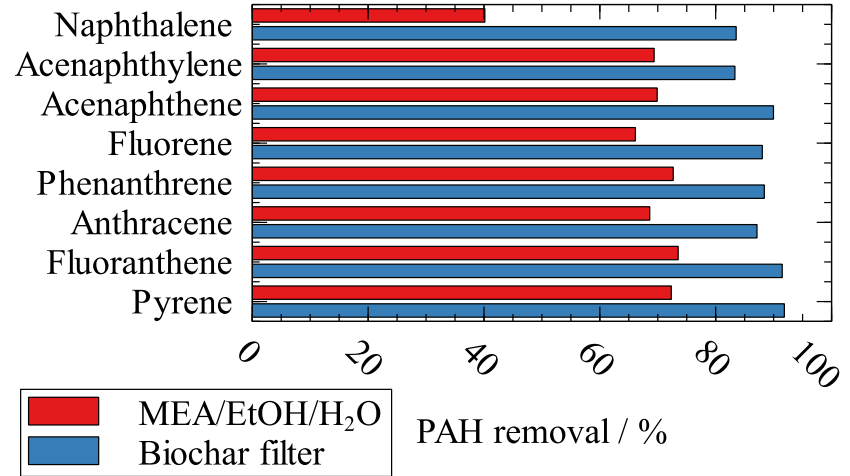


# PAH Removal with MEA/EtOH/H<sub>2</sub>O and Biochar



Two attempts for PAH removal:

1. Combined CO<sub>2</sub> and PAH removal
  - MEA/EtOH/H<sub>2</sub>O mixture
  - Good removal of larger PAHs
  - Only 40 % Naphthalene
2. Biochar filter
  - Biochar directly from the process
  - > 80 % removal





# Pilot Scale Scrubber (Re-)Activation

- Adaption of existing NH<sub>3</sub> scrubber for CO<sub>2</sub>-removal ~120 Nm<sup>3</sup>/h Syngas
  - Batch operation
  - Continuous operation later possible
- Extended sump vessel to circulate 1 m<sup>3</sup> solvent
- Stripper to remove CO<sub>2</sub> from solvent

Scrubber  
(adapted)



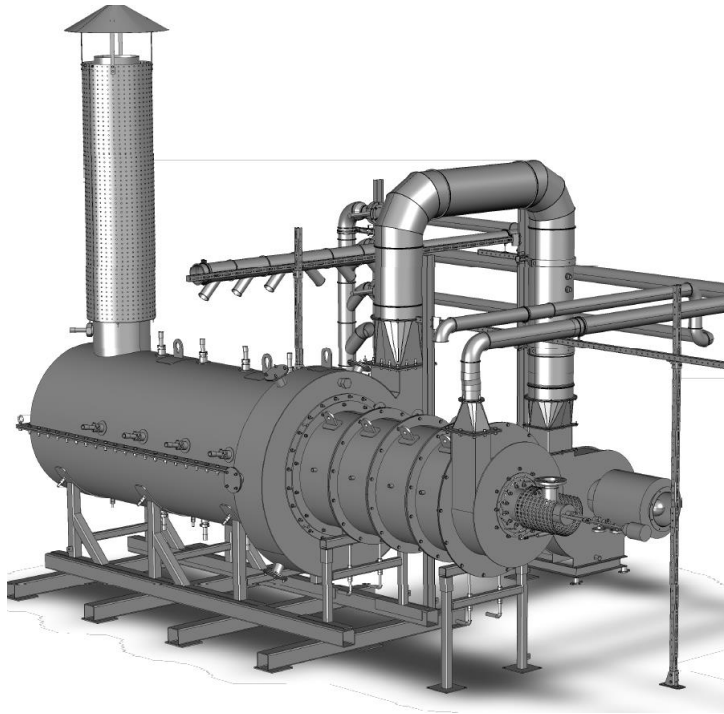
Sump/Stripper  
(new)





Gas Utilization

## Valorization of Low Heating Value Gas for High-Temperature Heat in Industry

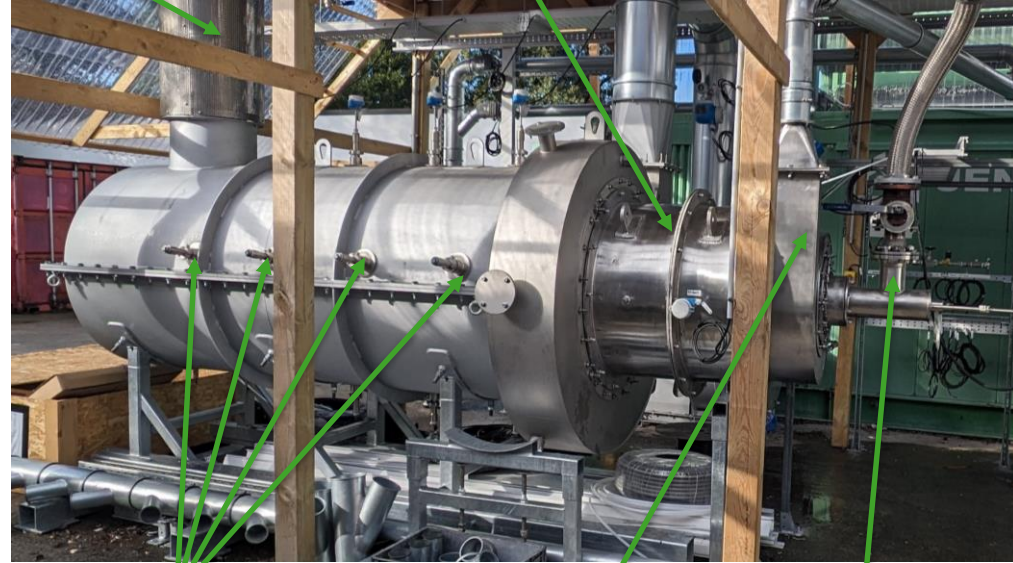


Mobile standard container sized burner test rig

Cooling air

Exhaust gas cooler

Variable length of the pre-combustion zone



Sight glasses

Air-cooled double-jacket combustion chamber to simulate different operating conditions

Measurements of the temperature profile

Primary air (adjustable swirl intensity)

Gas intake 150 – 750 kW

# Outlook



- Further testing of biochar filter in lab scale in october
- Launch of burner test rig in beginning of october
- First measurement campaign end of october
- Launch of scrubber in end of october
- First measurements in november






# Biohydrogen – Implementation of Dark Fermentation for Industrial Wastewater Treatment

Graz, September 26<sup>th</sup>, 2024

Mario Preidelt, Matthias Neubauer, Richard Pummer, Wilfried Neuhauser, Bernhard Drosig



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# Introduction

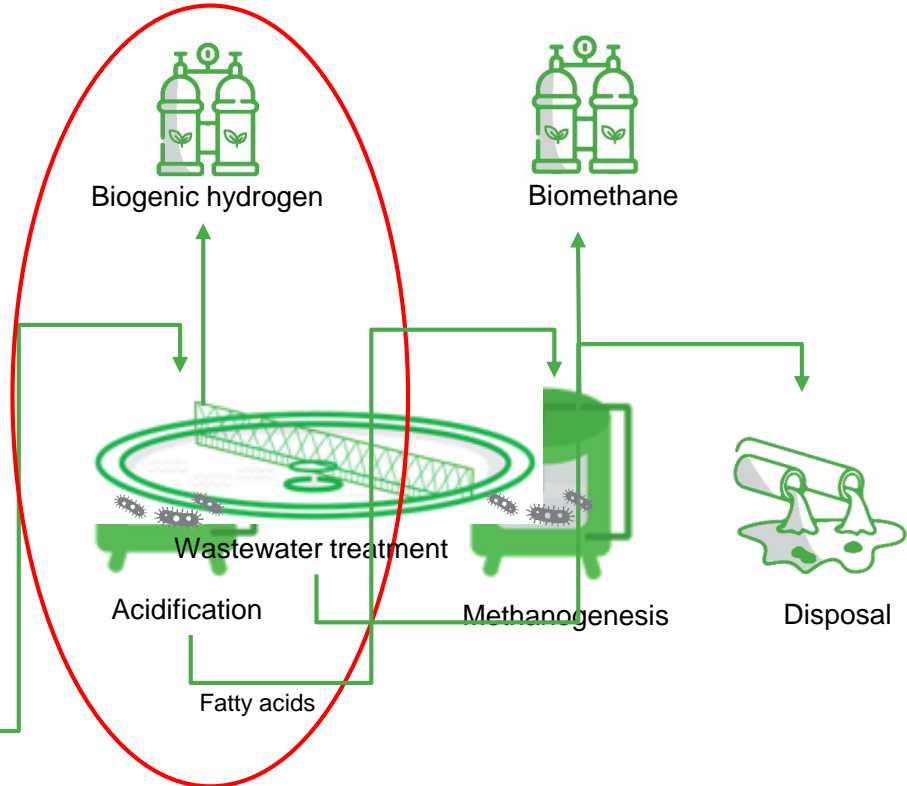
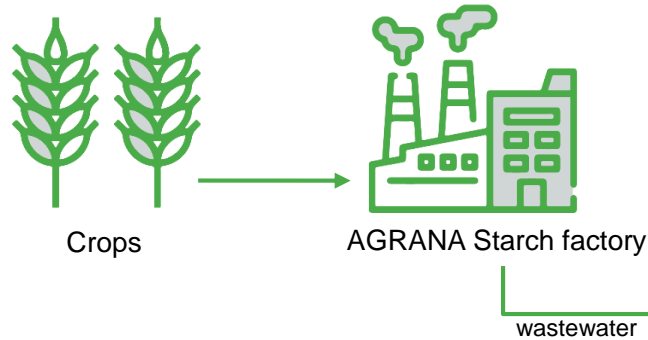
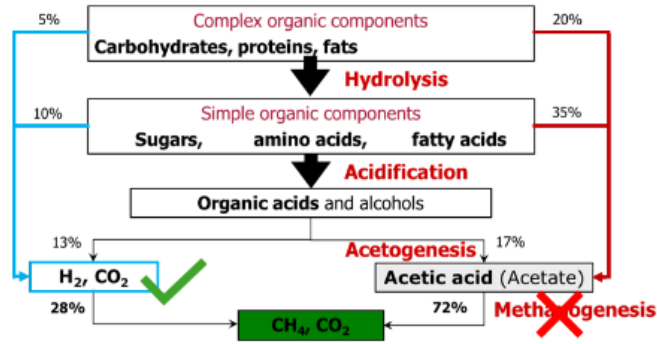


- Project “Wastewater to Hydrogen”
- Partners:
  - Agrana Starch (Aschach, Upper Austria)
  - Agrana Research and Innovation Center (ARIC)
- Goal: Implement a treatment for organic wastewaters





# Aims and objectives





# Experimental Setup

Pre-trials in serum bottles (A)

- Testing of media
- Complex nutrient sources tested
- Wastewaters screening (B)



Scale up – Pilot plant (C)

- Start with synthetic media
- Wastewater as carbon source (glucose)
- Complex nutrients sources (corn steep liquor, urea) + commercial trace element solution



Figure 1: Serum bottles for pre-trials (A), the selected wastewater (B) and the operated pilot plant (C)



# Experimental Setup – Pilot Plant

## Cultivation parameters

- Temp.= 55 °C
- pH = 5.5 (2 M NaOH)
- Filling level = 13 L
- mixed consortium
- N<sub>2</sub> stripping
- Circulation pump

## Analysis parameters

- Fatty acids and glucose
- pH
- N + P content
- Next generation sequencing
- AWITE - gas composition

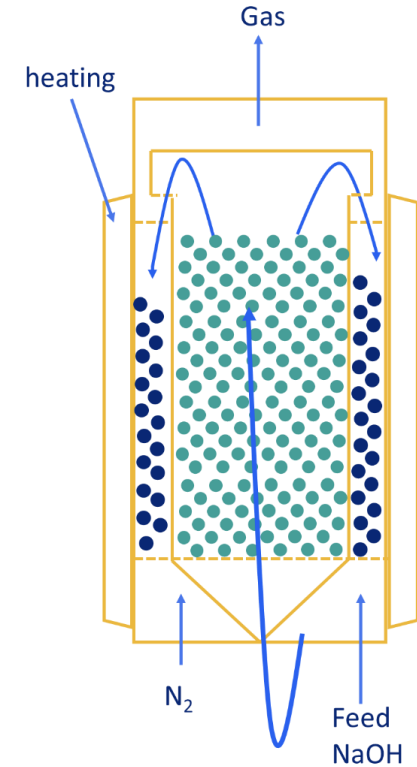


Figure 2: Sketch of the trickle bed pilot plant reactor





# Problems

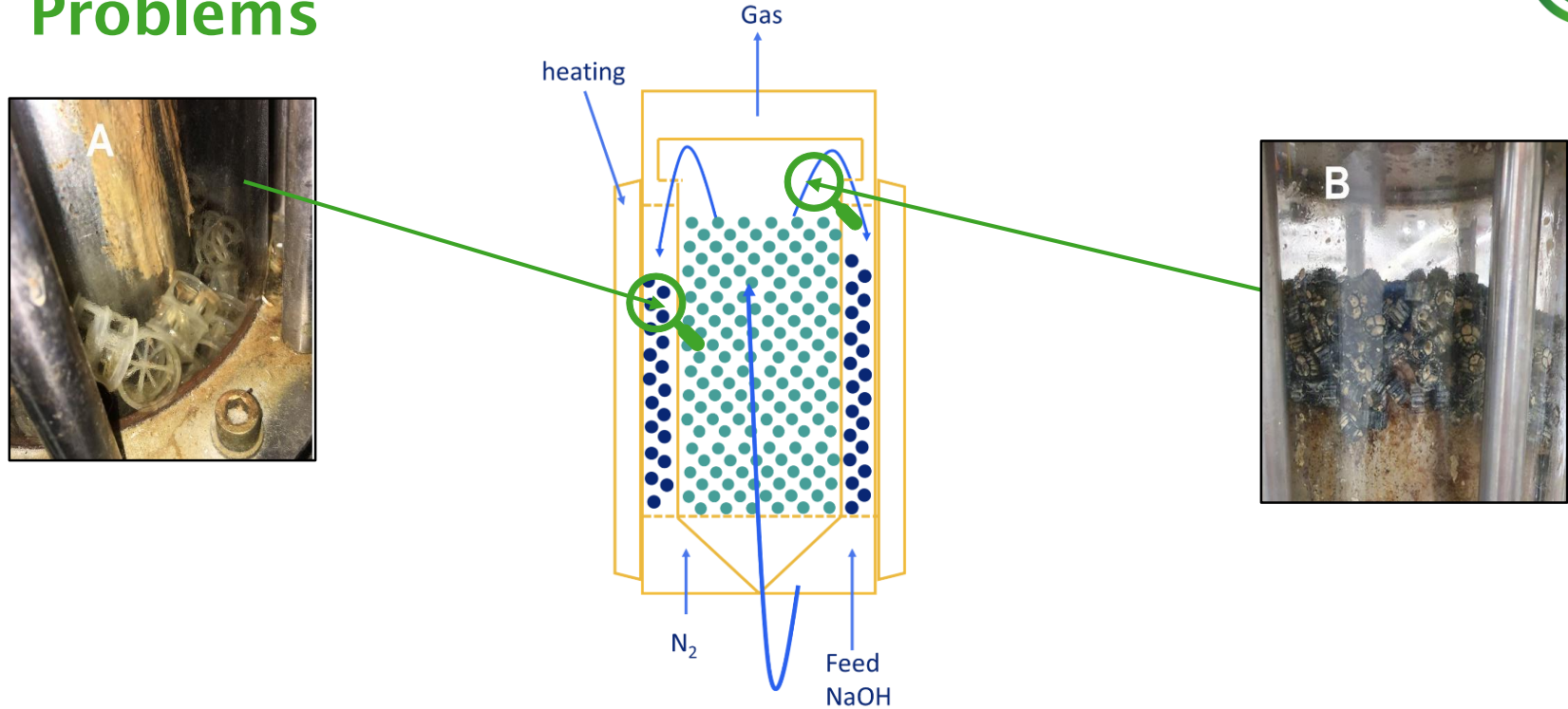


Figure 3: Filling bodies with accumulated wastewater solids. (A outer cyclinder, B center tube/top)



# Results

- Stable operation at a maximum substrate flow of 200 mL/h.
- For a duration of 2 weeks:
  - Wastewater diluted (~ 15 g/L glucose) and acidified to prevent degradation
  - Nutrient solution (CSL, urea, trace elements) supplied
- 4.8 L media/day → HRT 2.7 days
- Observed blockage from solids
- Glucose degradation ~95 %

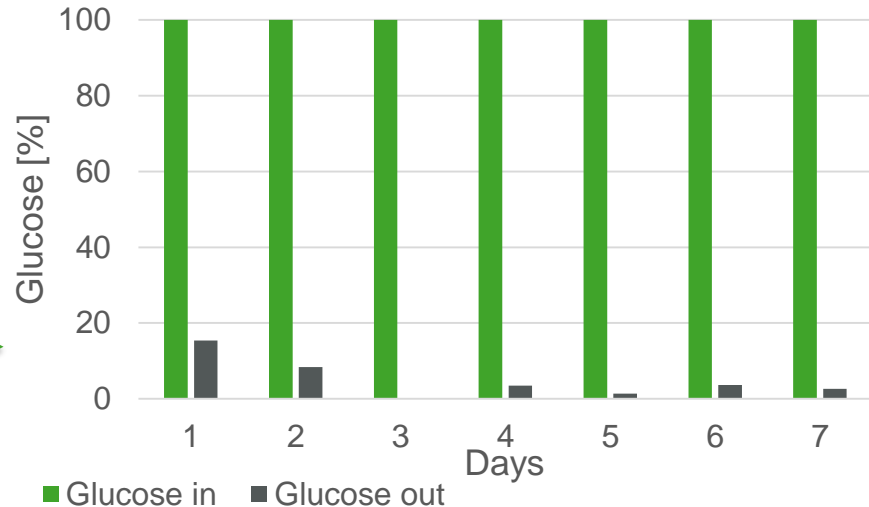


Figure 4: Glucose degradation



# Results

Acetic acid  $\varnothing$  2 g/L

Butyric acid  $\varnothing$  4 g/L

Acids available for methanogenesis

- 9.5 g/d acetic acid
- 19.3 g/d butyric acid

Average = 20 NI H<sub>2</sub>/d

total NI H<sub>2</sub>: 280 NI

total glucose input: 976 g

Productivity of 2.34 mol H<sub>2</sub>/mol  
glucose

„Thauer limit“ of 4 mol H<sub>2</sub>/mol  
glucose<sup>2</sup>

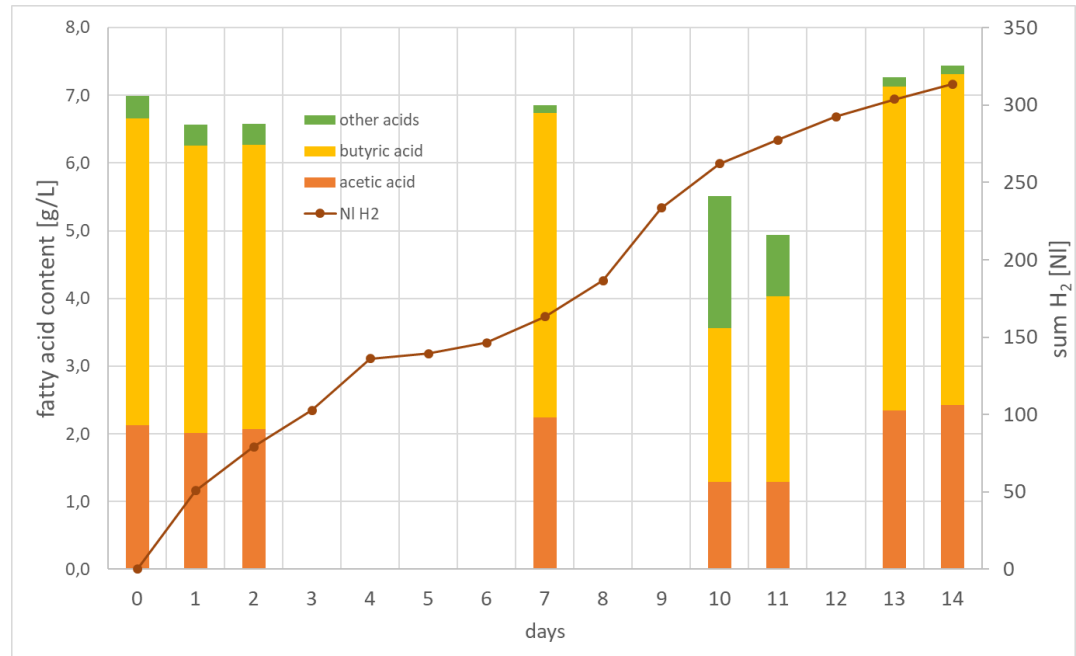


Figure 5: Fatty acid content and sum of NI H<sub>2</sub> produced during stable operation of 2 weeks at 200 mL/h media flow.



# Outlook





Often acidification prior to methanogenesis in an industrial setting

- Possibility to provide Fatty acids for methanogenesis

However no collection of H<sub>2</sub>

- Released to environment
- Fully converted to CH<sub>4</sub> during hydrogenotrophic methanogenesis

Benefits of H<sub>2</sub> collection in an 2-stage biogas process:

-  Possible energy carrier<sup>3</sup>
-  Sustainable H<sub>2</sub> source → Reduce dependency on fossil fuels for H<sub>2</sub> production<sup>3</sup>
-  Contribute to global H<sub>2</sub> demand – ammonia, electronics<sup>4</sup>
-  More sustainable process for AGRANA → reduce use of fossil fuels<sup>5</sup>



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# Effects of the climate crisis and pesticide use on fatty acids in the food web



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Graz, September 26<sup>th</sup>, 2024

**Katharina Ludwig**, Lisa Bauer, Mario Preidelt, Emily Ruttner, Musa Elesad, Martin Kainz, Lidija Kenjeric, Michael Sulyok, Wolfgang Kandler, Ines Fritz, Bernhard Drosch



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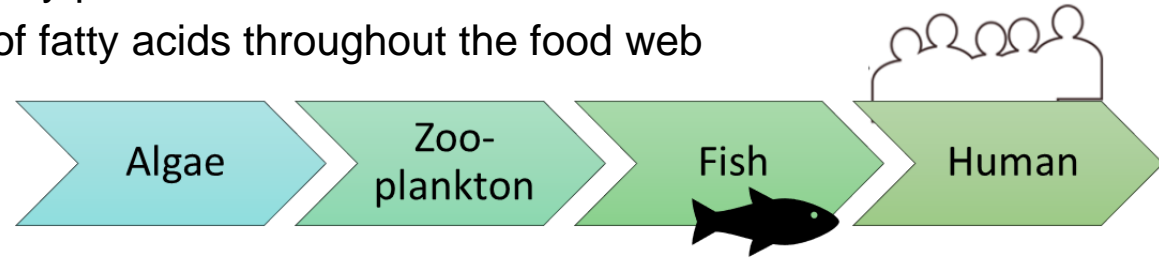
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# Fatty acids in the food web

- Phytoplankton – primary producers
  - Dietary transfer of fatty acids throughout the food web

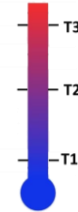


- Essential functions in living organisms
  - e.g. energy storage, cell membrane, brain development
- Polyunsaturated fatty acids (PUFA) in food/feed important for consumers
  - Limited possibilities to adapt the fatty acid pattern through bioconversion



# Influence of environmental factors

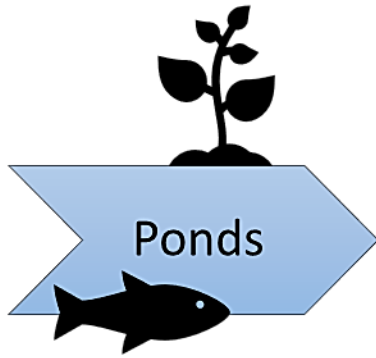
- **Fatty acid pattern in whole food web depends on environmental conditions**
- **Temperature** increase of 2-5 °C until 2100 predicted  
→ increased water temperature
  - Changes in fatty acid pattern of phytoplankton
  - Heat → less long-chain and unsaturated fatty acids
- **Contamination** of freshwater ecosystems by xenobiotics, e.g. pesticides
  - Water soluble → surface run-off to ponds after heavy rains
  - Potentially harmful for aquatic organisms
  - Pesticides target metabolism of plants  
→ similar effect on phytoplankton expected





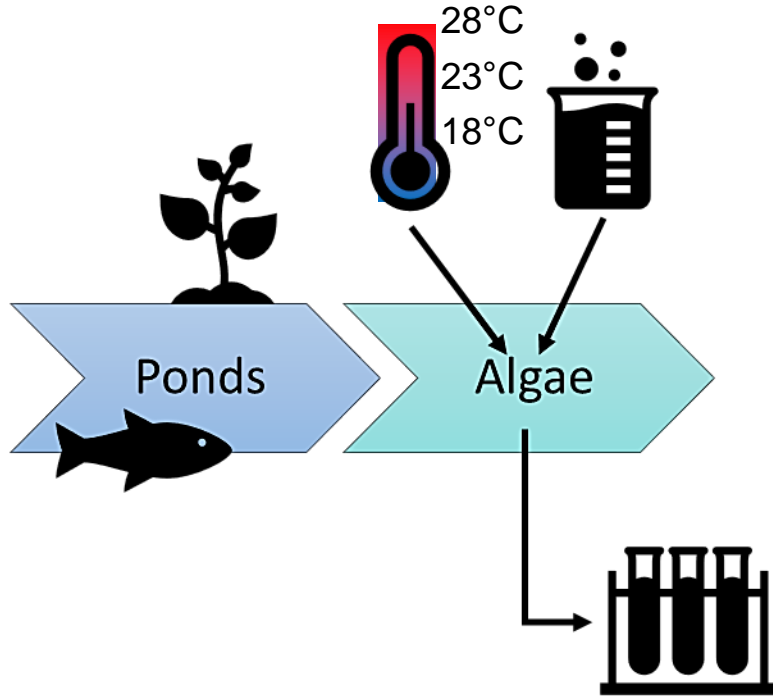


# Aims & first results



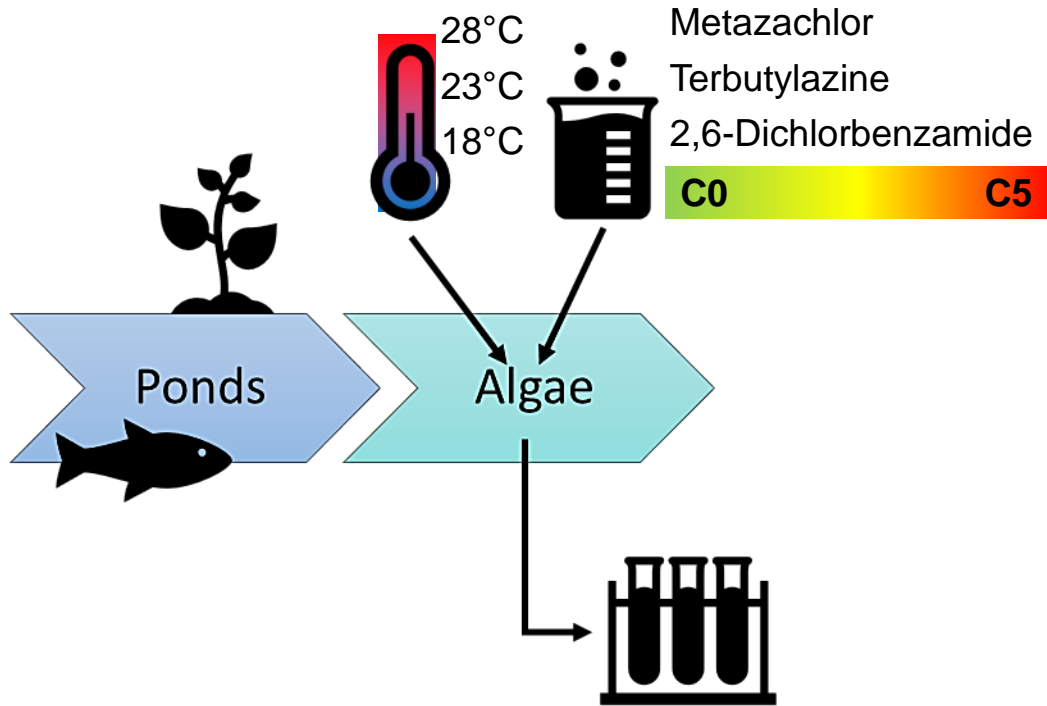


# Aims & first results





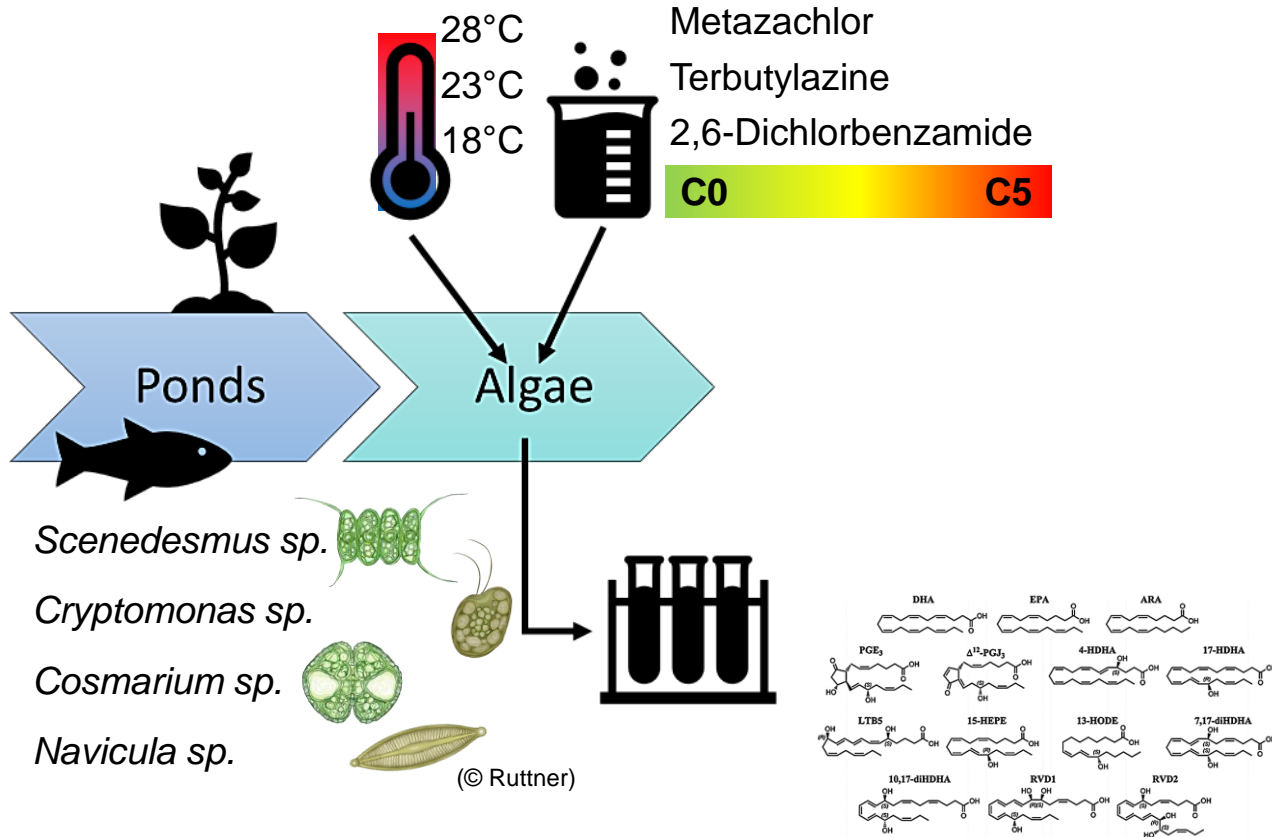
# Aims & first results





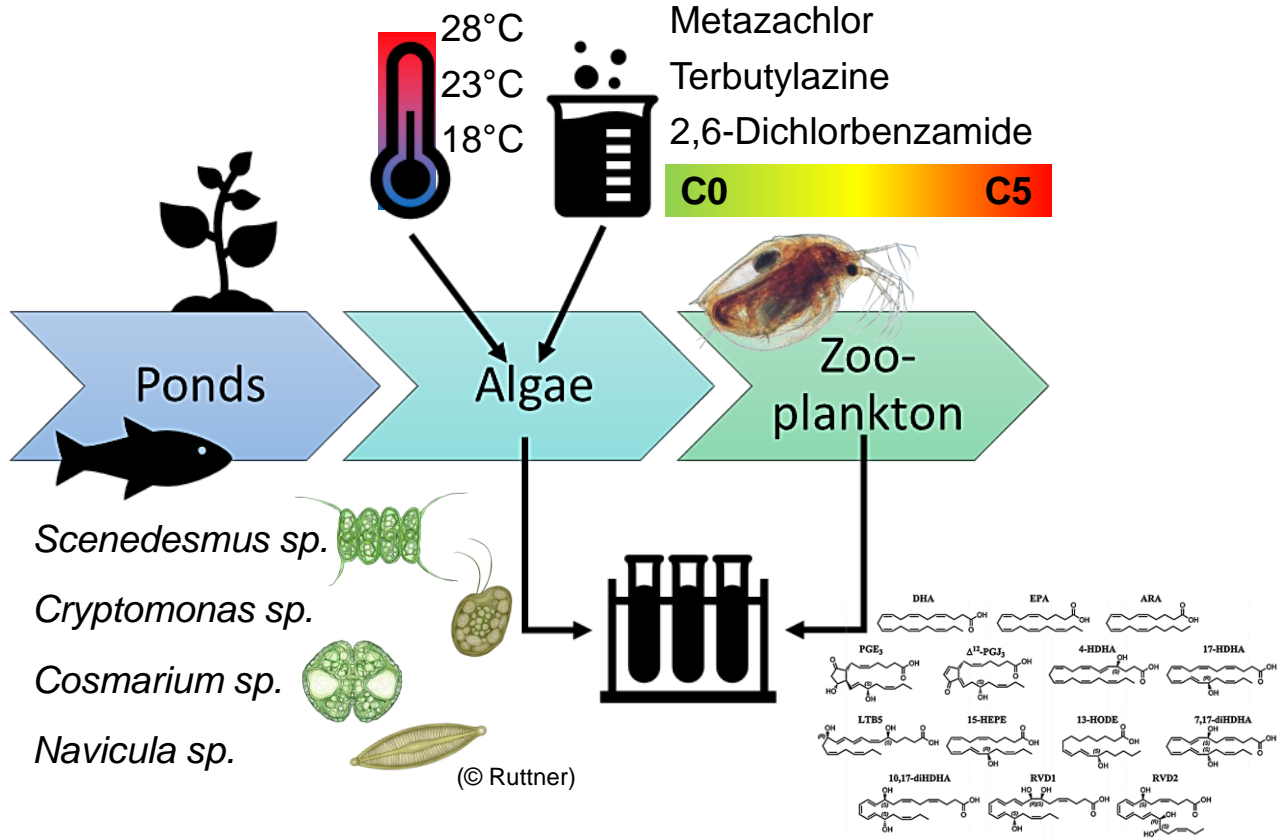


# Aims & first results



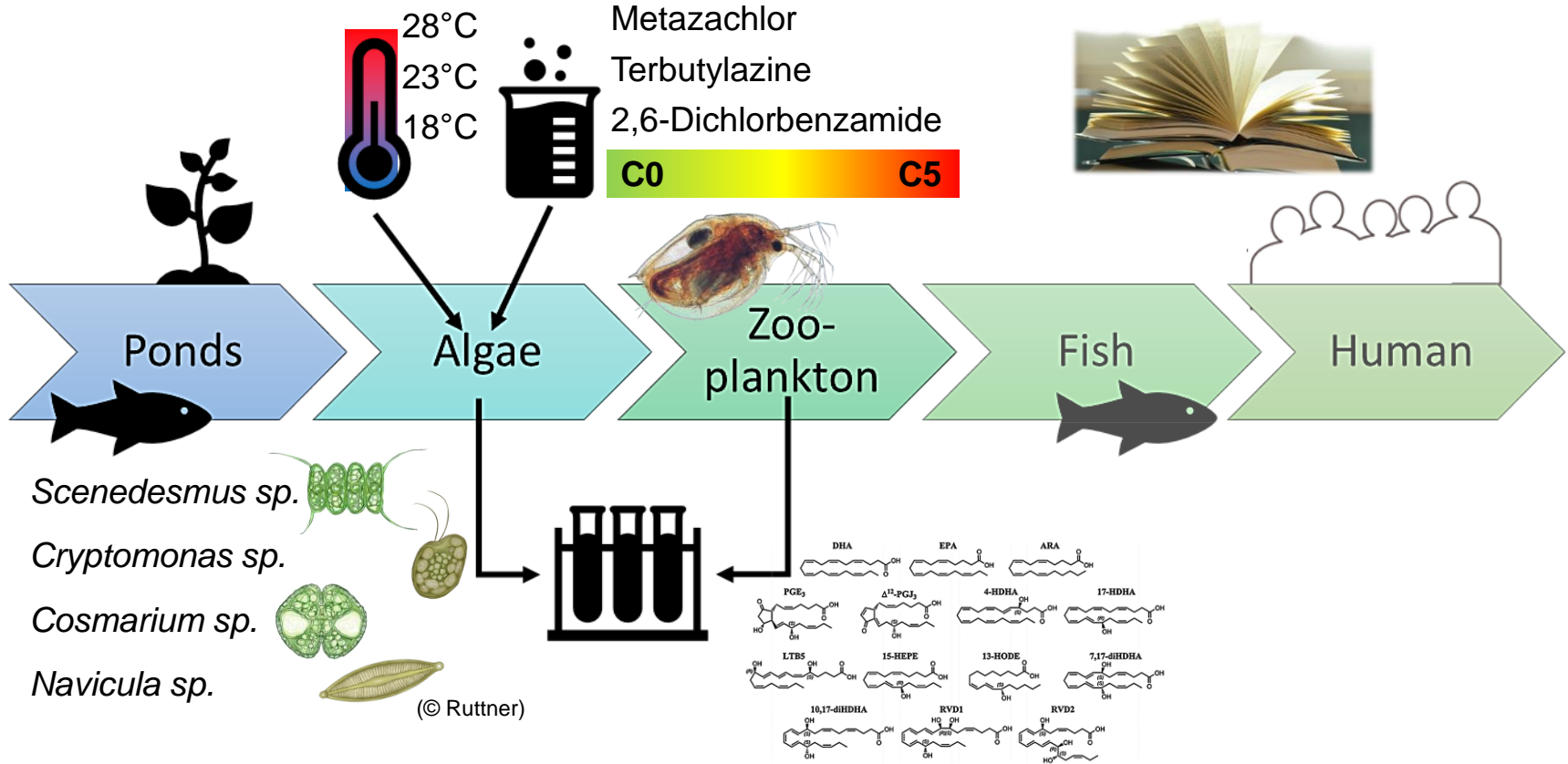


# Aims & first results





# Aims & first results



# Current experiments – algae screening

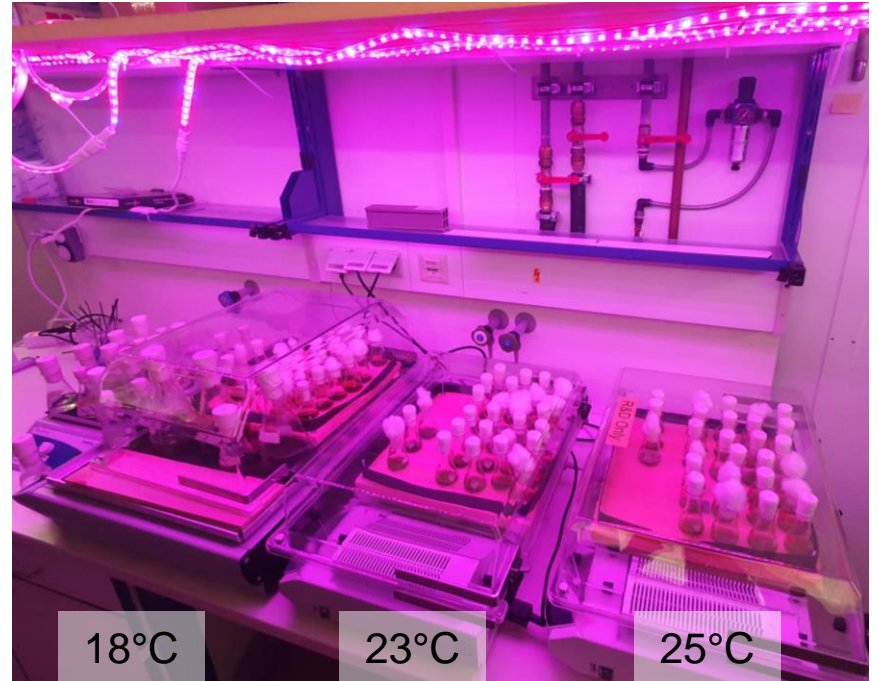
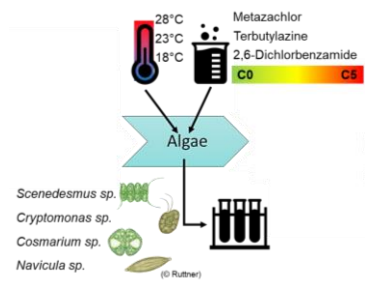


Cultivation  
in 25 mL  
shaking  
flasks  
(triplets)



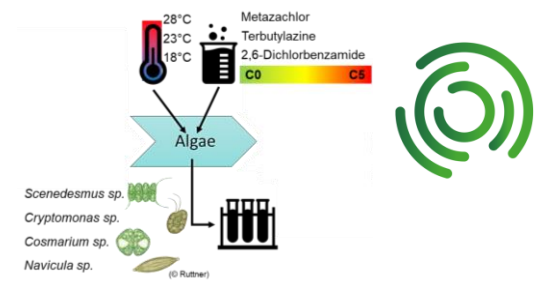
Measurement  
of  $OD_{435}$ ,  $OD_{680}$   
in 96-well plates  
via plate reader

Data analysis in

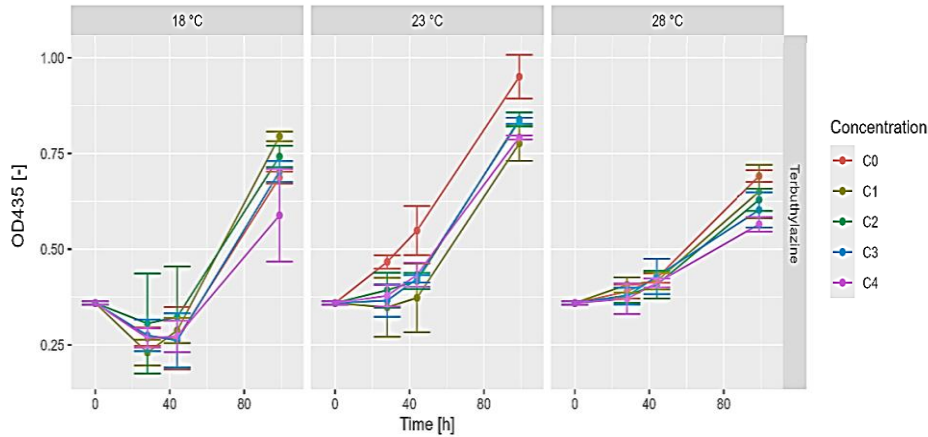




# Results – algae screening



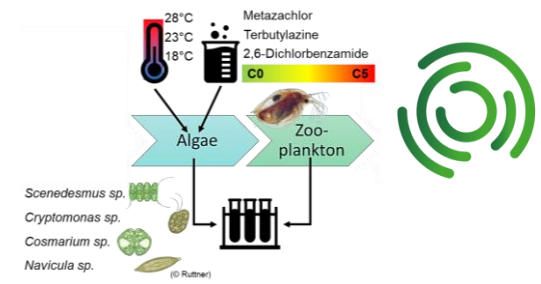
- Algae: *Scenedesmus*
- Pesticide: Terbutylazine



- The growth rate of each algae strain is different
- Temperatures >23°C affect algae growth more than
  - increasing pesticide-concentrations
  - type of pesticide

# Next steps

- Finalising algae screening and
- Data analysis
  
- Biomass production for
  - Lipid analysis and
  - Zooplankton cultivation





Thank you for your attention






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# Syngas production from biogenic residues and waste via advanced dual fluidized bed gasification

BEST Zentrumstag, Graz  
September 29<sup>th</sup>, 2024

Miriam Huber



 Bundesministerium  
Arbeit und Wirtschaft

 Bundesministerium  
Klimaschutz, Umwelt,  
Energie, Mobilität,  
Innovation und Technologie



 Für die  
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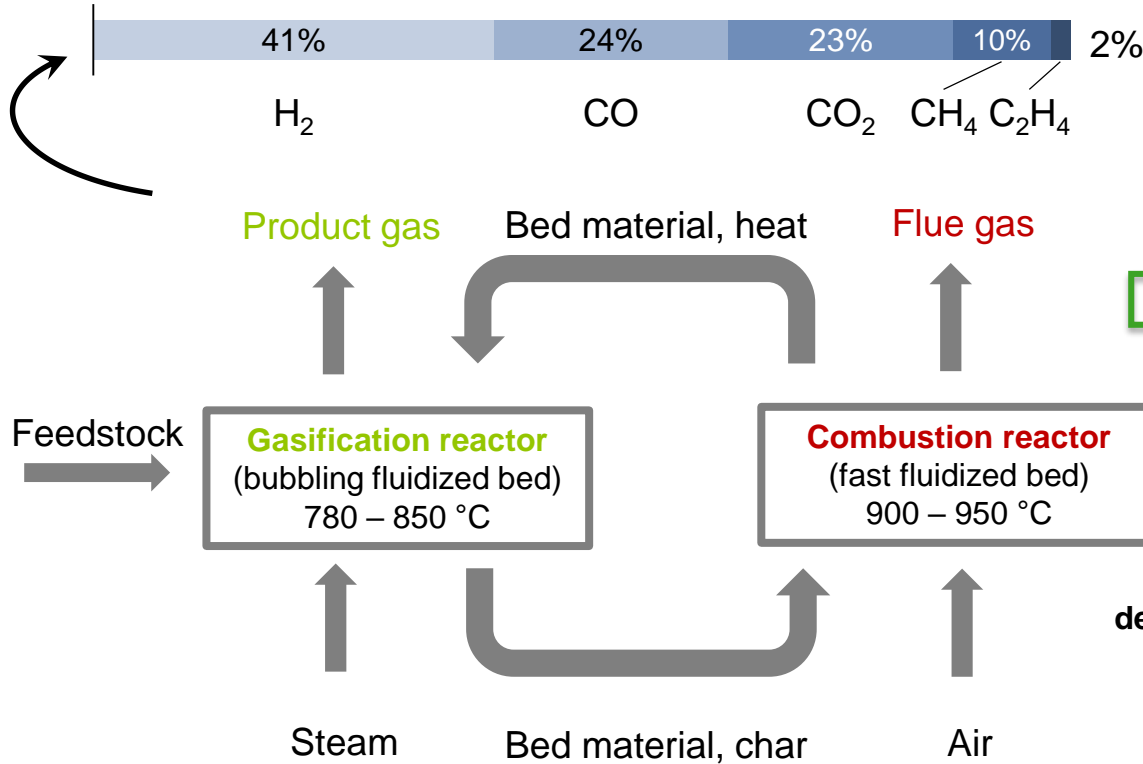
# SYNGAS PLATFORM VIENNA

A **research hub** featuring a Waste2Value process chain: 1 MW **aDFB gasification** + 250 kW **Fischer-Tropsch** synthesis demo

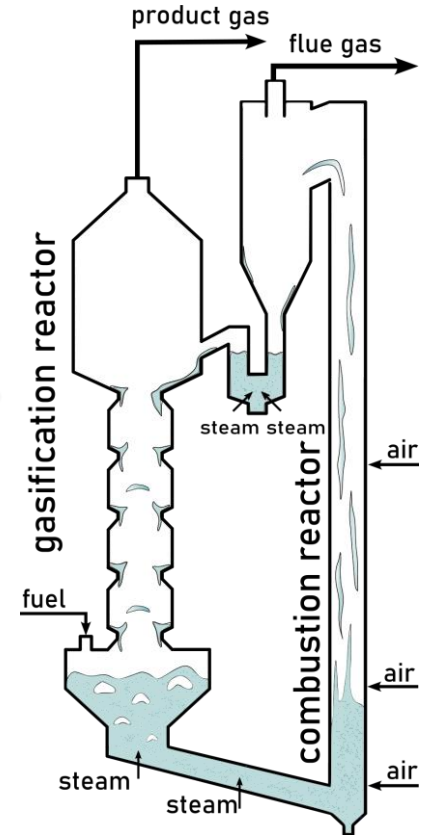
A connected **laboratory** supplied **with real syngas** for gas cleaning and upgrading



# Advanced Dual Fluidized Bed Steam Gasification

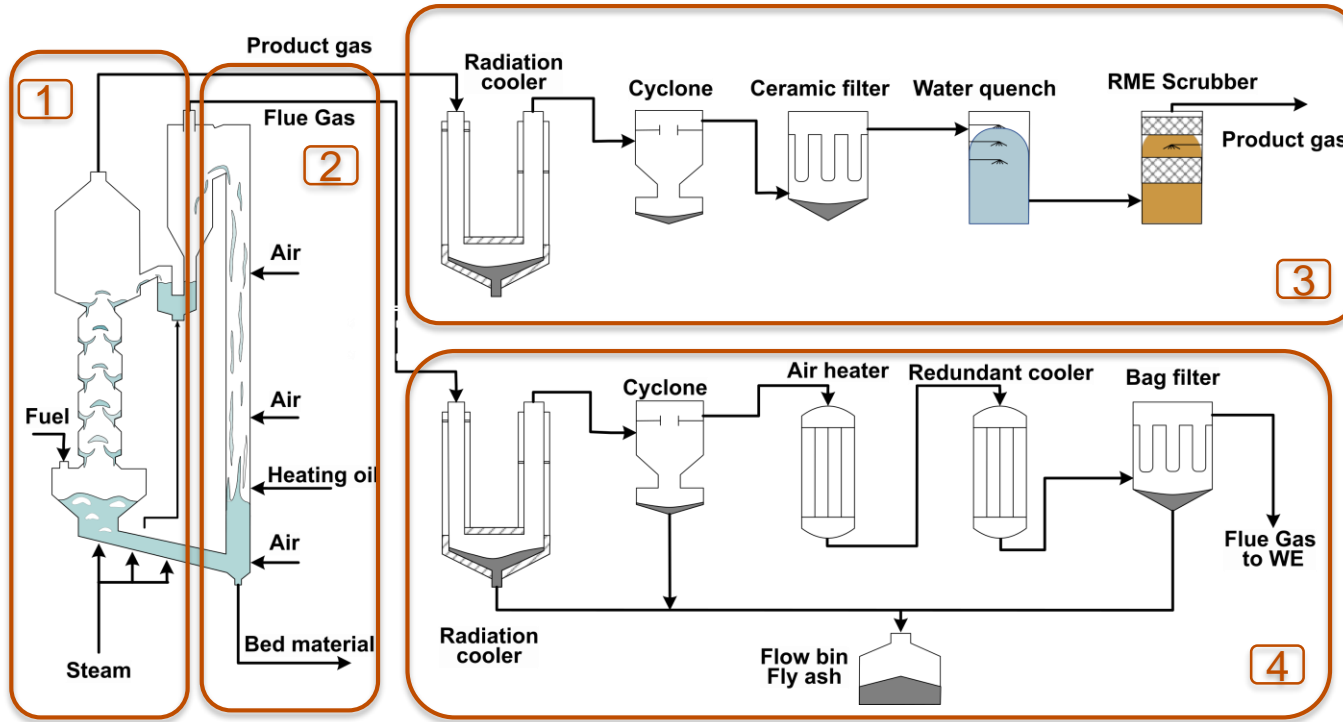


developed at



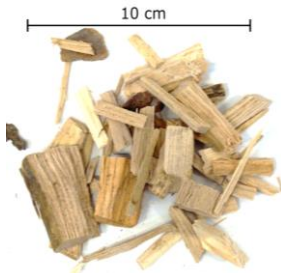


# Process Scheme - Gasifier



- 1 Gasifier
- 2 Combustor
- 3 Product Gas Cleaning
- 4 Flue Gas Cleaning

# Feedstock Variety



wood chips



plastic rejects



sewage sludge

↓ Decreasing LHV

↑ Increasing ash content



cashew husks



forestry residues



bark

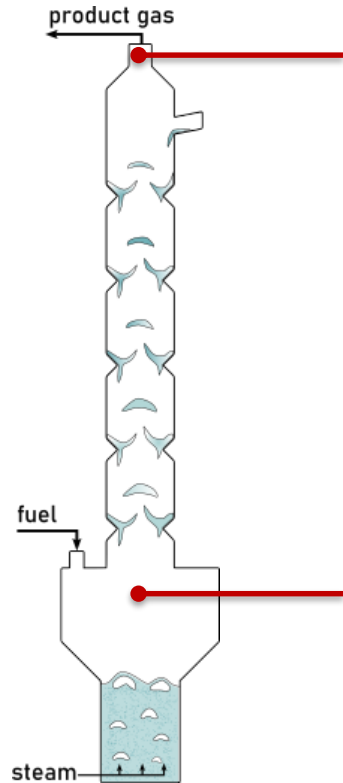


paper sludge





# Countercurrent Flow Column



Measurement Point  
After Countercurrent Column  
Gravimetric tar 8.9 g/Nm<sup>3</sup>  
GCMS tar 11.0 g/Nm<sup>3</sup>

Measurement Point  
Freeboard  
Gravimetric tar 11.5 g/Nm<sup>3</sup>  
GCMS tar 16.9 g/Nm<sup>3</sup>

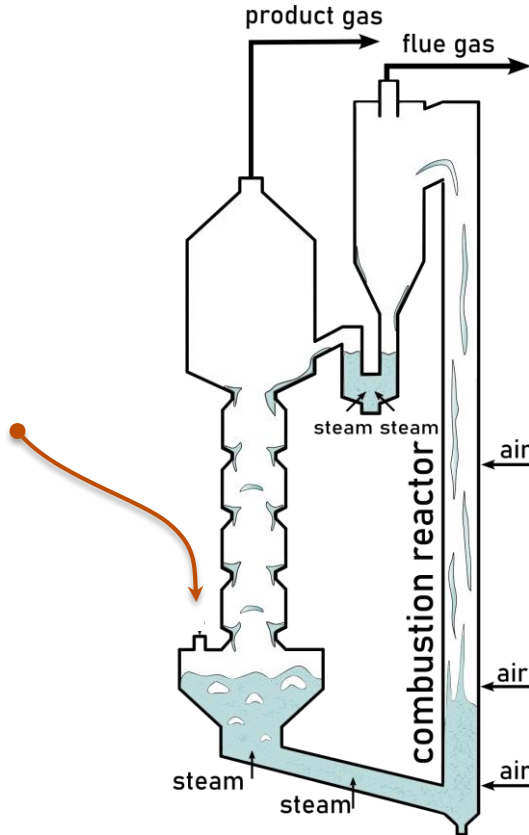
## Plastic Rejects Blend

Countercurrent column  
Increased contact of  
upstreaming product gas and  
downstreaming catalytically  
active bed material

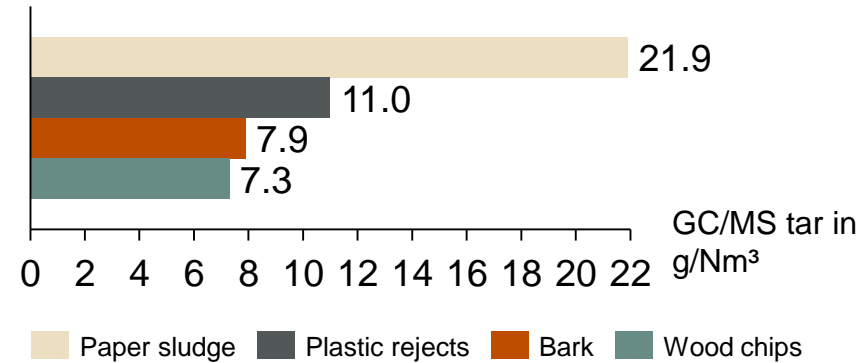
Gravimetric tar -23 %  
GCMS tar -35 %  
for plastic-rich rejects blend as  
exemplary feedstock



# Pulp and Paper Residues



## Gas Impurities Before Cleaning



Below < 1.5 g/Nm<sup>3</sup> after coarse gas cleaning

# Research Areas



Extensive demonstration campaigns with challenging waste feedstocks



Optimization of product gas composition for i.e. FT synthesis



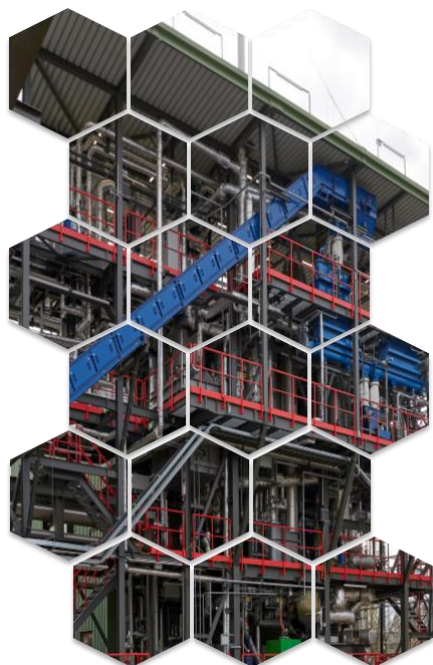
Upscaling of countercurrent column



Cold flow model investigations on fluid dynamics



# Thank You For Your Attention!



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# Area 1.3 – Syngas Platform Technologies

## New developments in gas cleaning for the production of C-based products and fuels via gasification

BEST – Zentrumstag, Graz, 26.9.2024

Anna Egger





# Why product gas cleaning?

## Fouling reduction

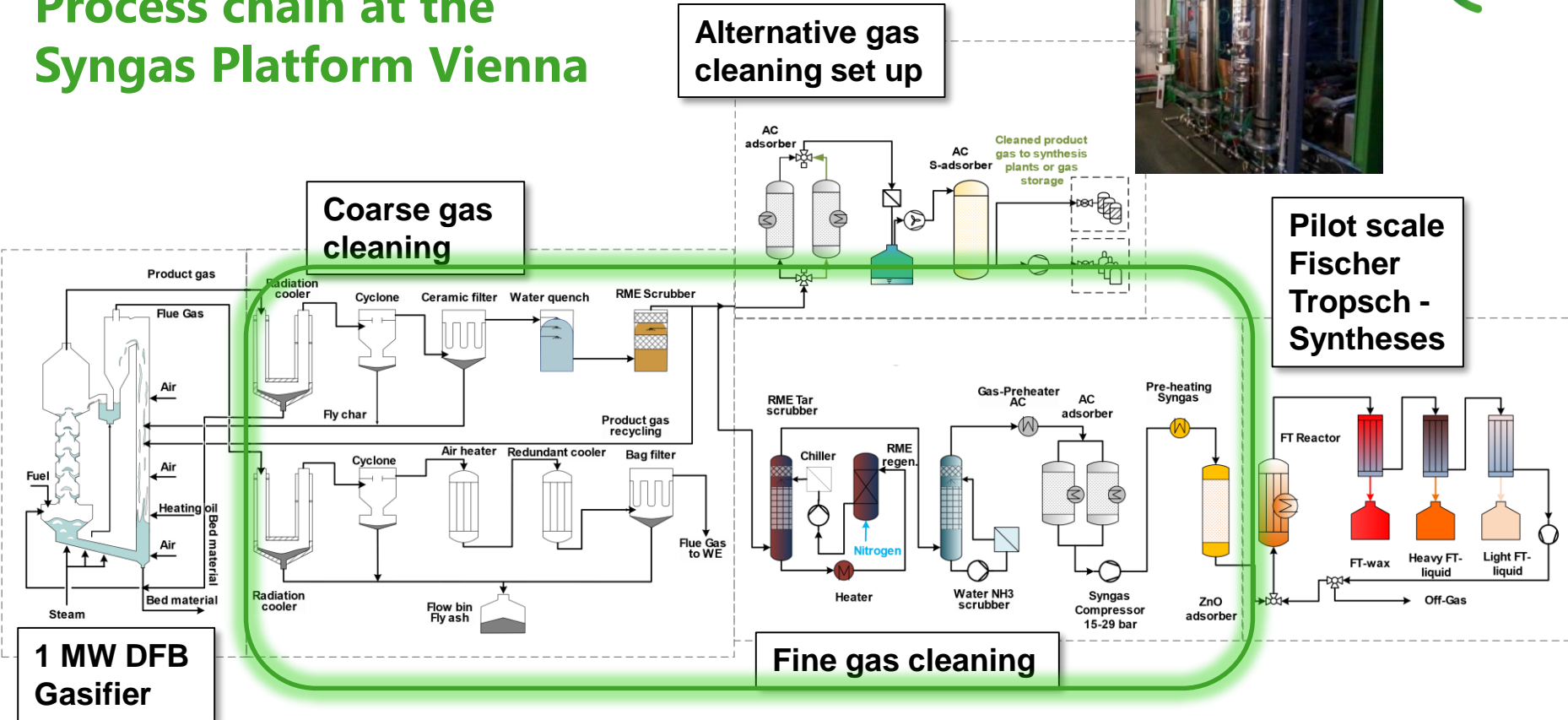
- Reduction of blockages of heat exchangers, filters, blowers and other plant parts
  - ➔ Necessary reduction of: particles, tar compounds
- Result: decreased maintenance effort

## Reaching requirements for down stream processes

- Removal of components with negative effects on downstream processes
  - ➔ Catalyst poisons: sulfur-, nitrogen- and halogen compounds
- Removal of reaction inhibiting components
- Particles, tar components and benzene



# Process chain at the Syngas Platform Vienna



**Coarse gas cleaning**

**Alternative gas cleaning set up**

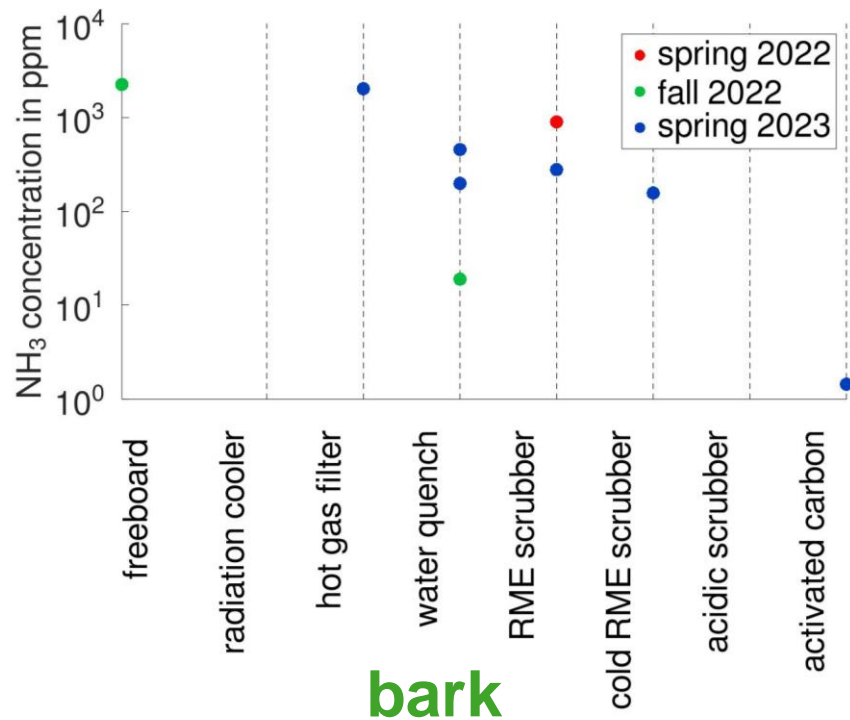
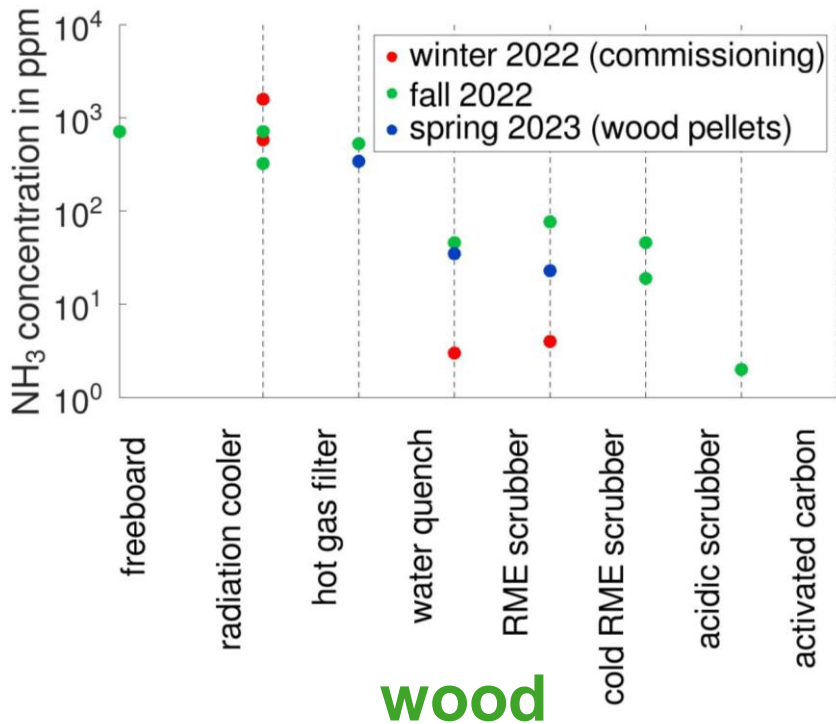
**Pilot scale Fischer-Tropsch Syntheses**

**Fine gas cleaning**

**1 MW DFB Gasifier**



# NH<sub>3</sub> concentrations observed during woody biomass gasification



# Focused research areas



## Effect on increased impurity contents on classic gas cleaning

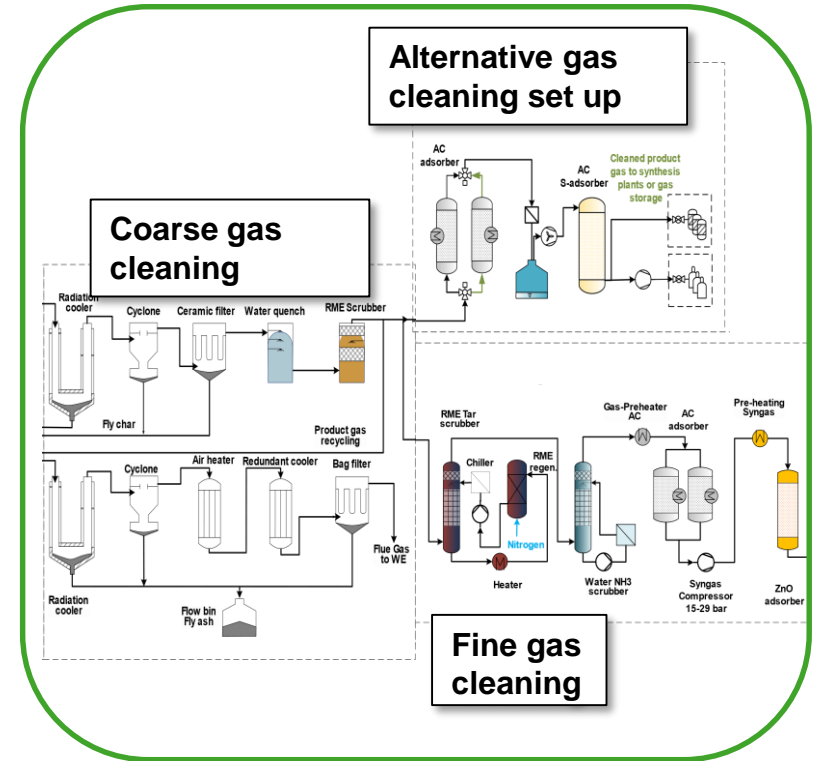
- Quench
- RME-Scrubbers
- Activated carbon (RME-alternatives)

## Impurities as value added products

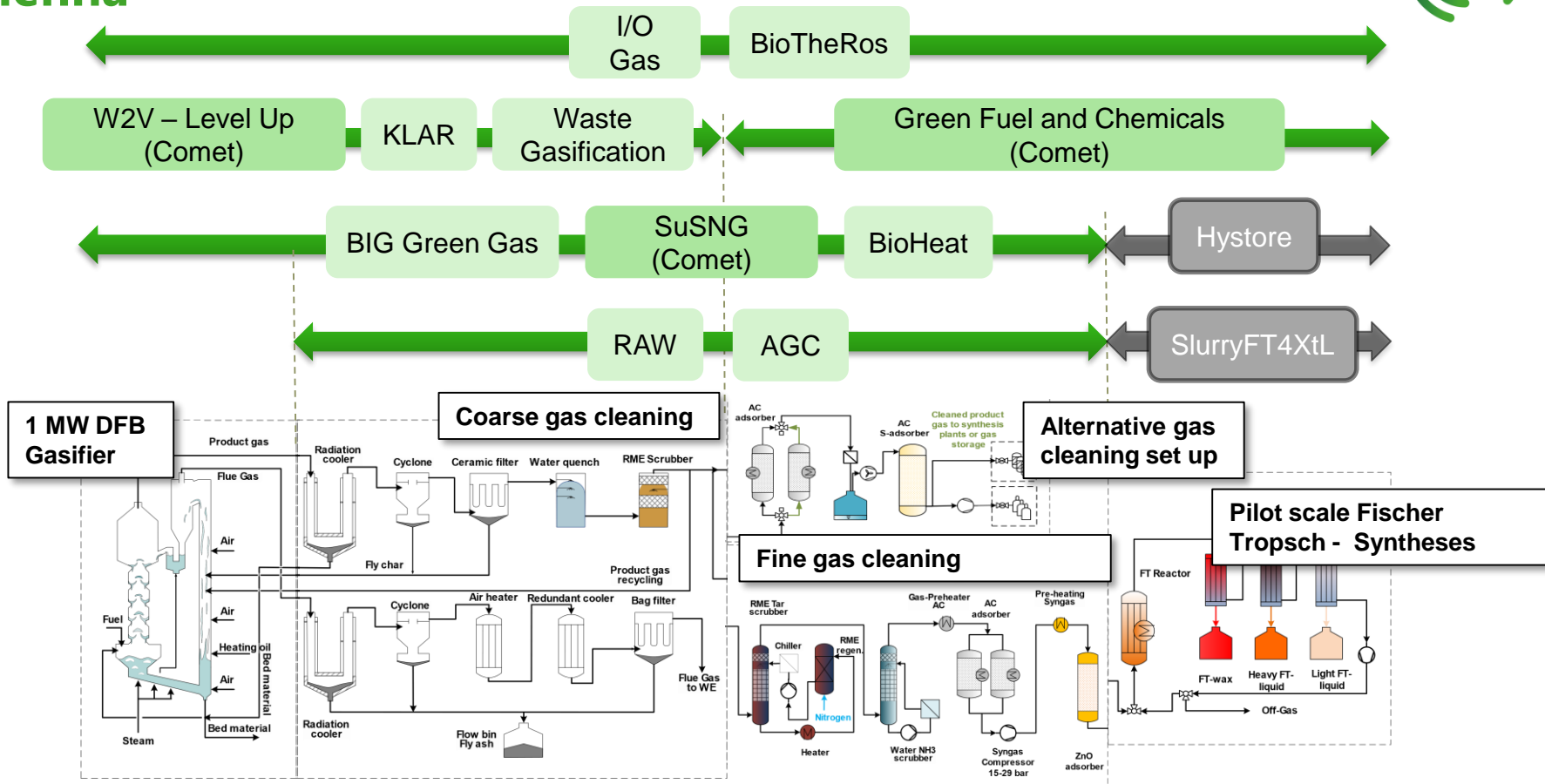
- Ashes
- Tar components
- Waste water

## Evaluation of closed loops within the process and substance accumulation

- Loaded RME
- Waste water handling
- Fly char



# Projects investigating gas cleaning at the Syngas Platform Vienna



# Area 1.3 – Syngas Platform Technologies


## Advancements in Fischer-Tropsch synthesis using a slurry bubble column reactor

BEST Zentrumstag, Graz 26.09.2024

Theresa Köffler



 Bundesministerium  
Arbeit und Wirtschaft

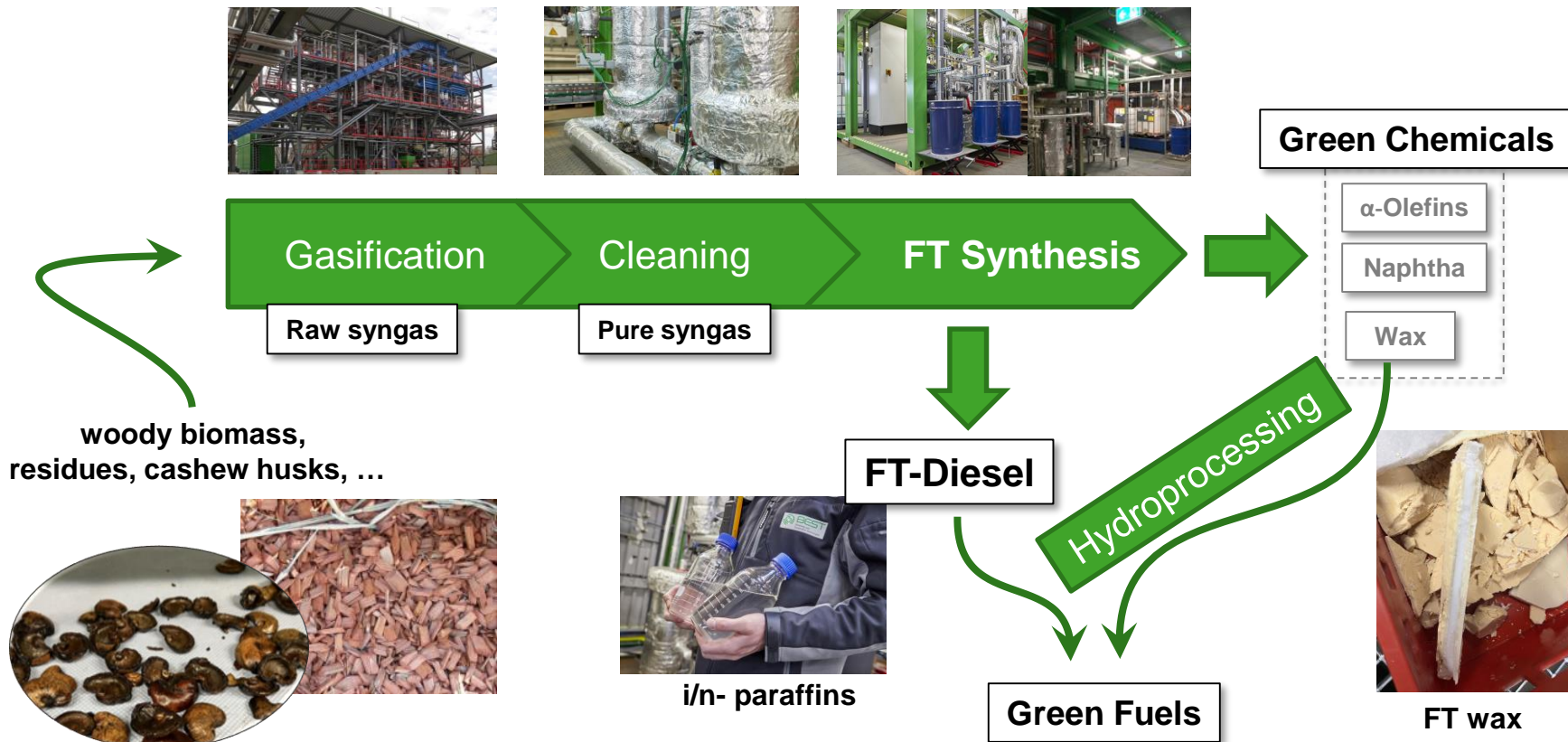
 Bundesministerium  
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Innovation und Technologie



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# FT Synthesis: Pathway to Green Fuels and Chemicals

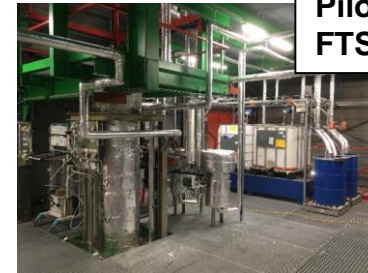
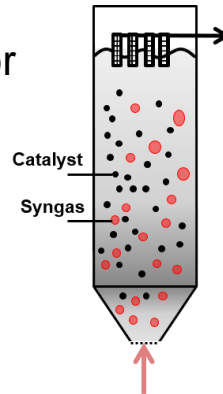




# Fischer-Tropsch Synthesis (FTS)

- Catalytic process to convert syngas ( $\text{CO} + \text{H}_2$ ) into hydrocarbons
- Process conditions:
  - Temperature: 200 - 230°C
  - Pressure: 20 - 22 bar(g)
  - Catalyst:  $\text{Co}/\gamma\text{-Al}_2\text{O}_3$  (commercial)

- Slurry Bubble Column Reactor
  - ✓ Heat and mass transfer
  - ✓ Simple reactor design
  - ✓ Load flexibility



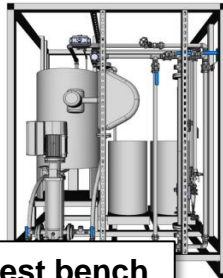




# Research area - Process optimizations

- Reactor design
  - Different reactor configurations
  - Testing of different gas distribution systems
- Product separation
  - Thermal product separation
  - Fine separation of catalyst particles

SBCR cold model



Filtration test bench

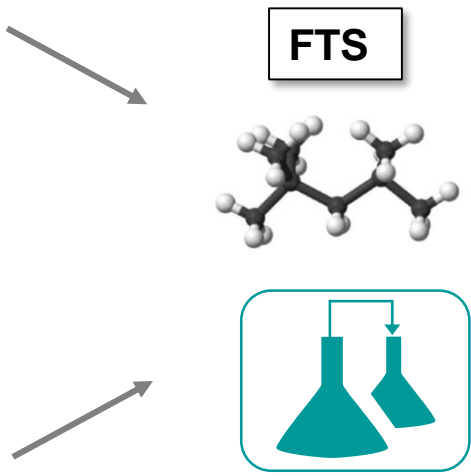
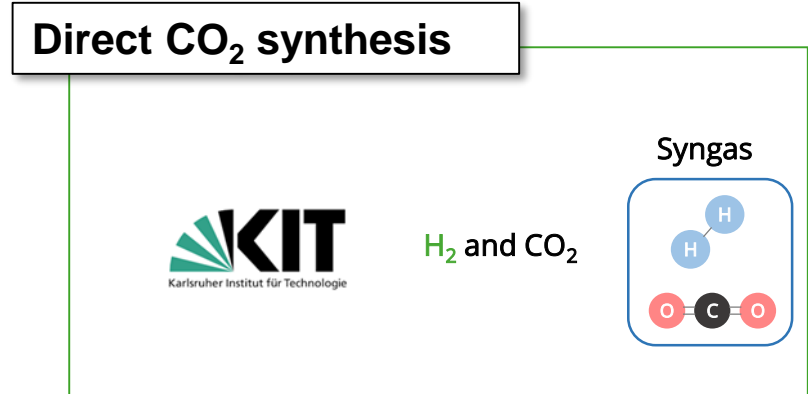
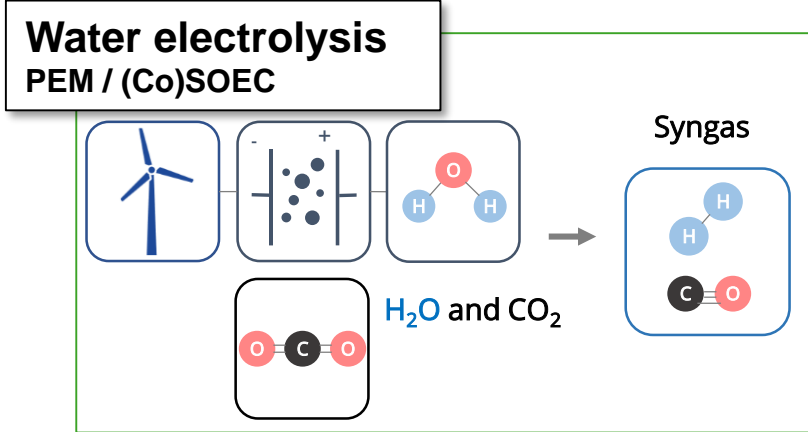
- Usage of FT water
- Tailgas Loop
- Effect of contaminations on FT synthesis

Aqueous Phase Reforming Pilot Plant





# Research area – XtL Syngas pathways



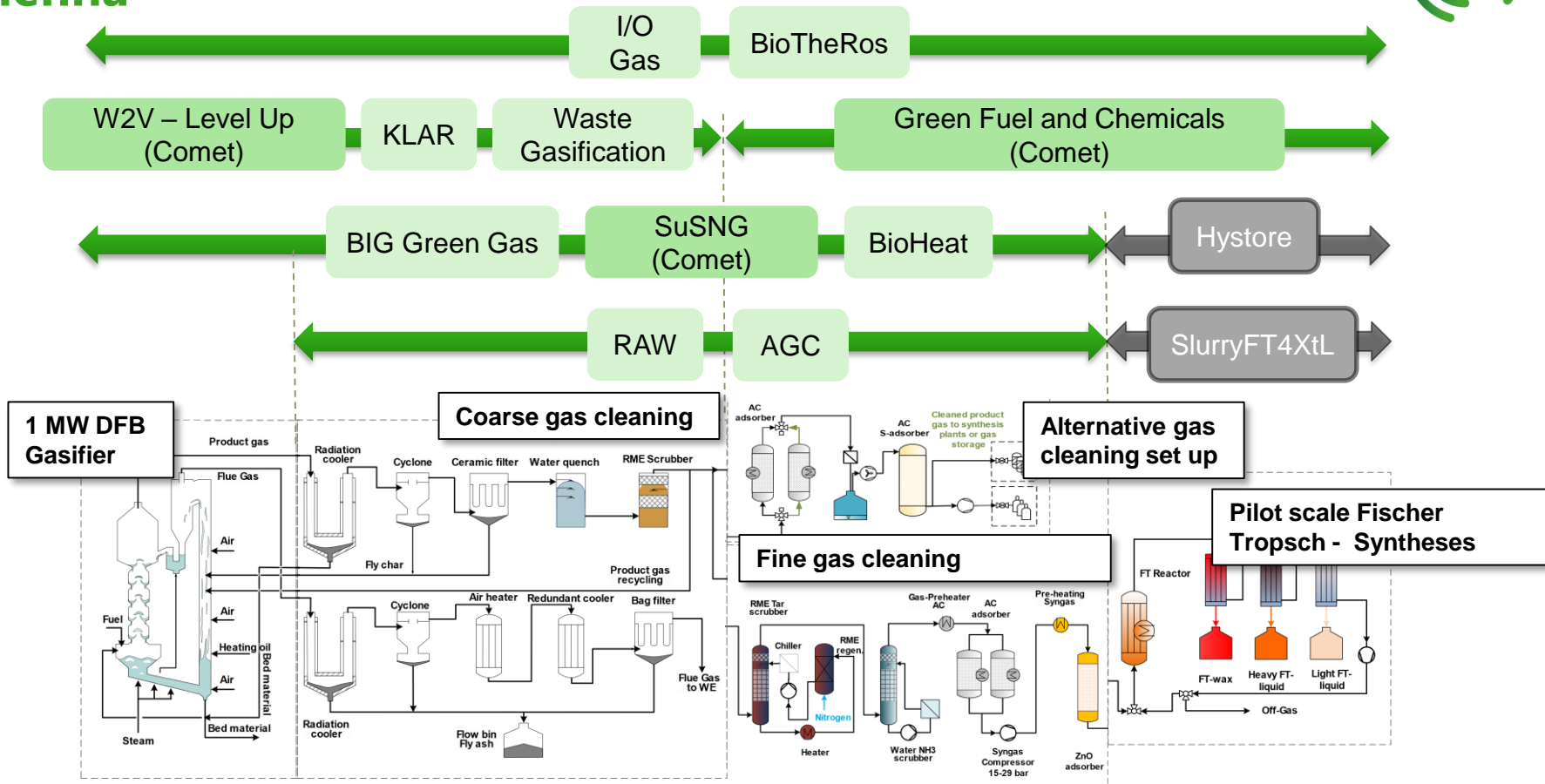
Sustainable  
(bio)refinery products



Green  
Aviation Fuel



# Projects investigating gas cleaning at the Syngas Platform Vienna



# Our industrial and scientific partners





# Biofuels – a crucial part of decarbonisation?

BEST Centre´s Day,  
26<sup>th</sup> September 2024, Graz

Dina Bacovsky, Doris Matschegg, Andrea Sonnleitner



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 Bundesministerium  
Klimaschutz, Umwelt,  
Energie, Mobilität,  
Innovation und Technologie

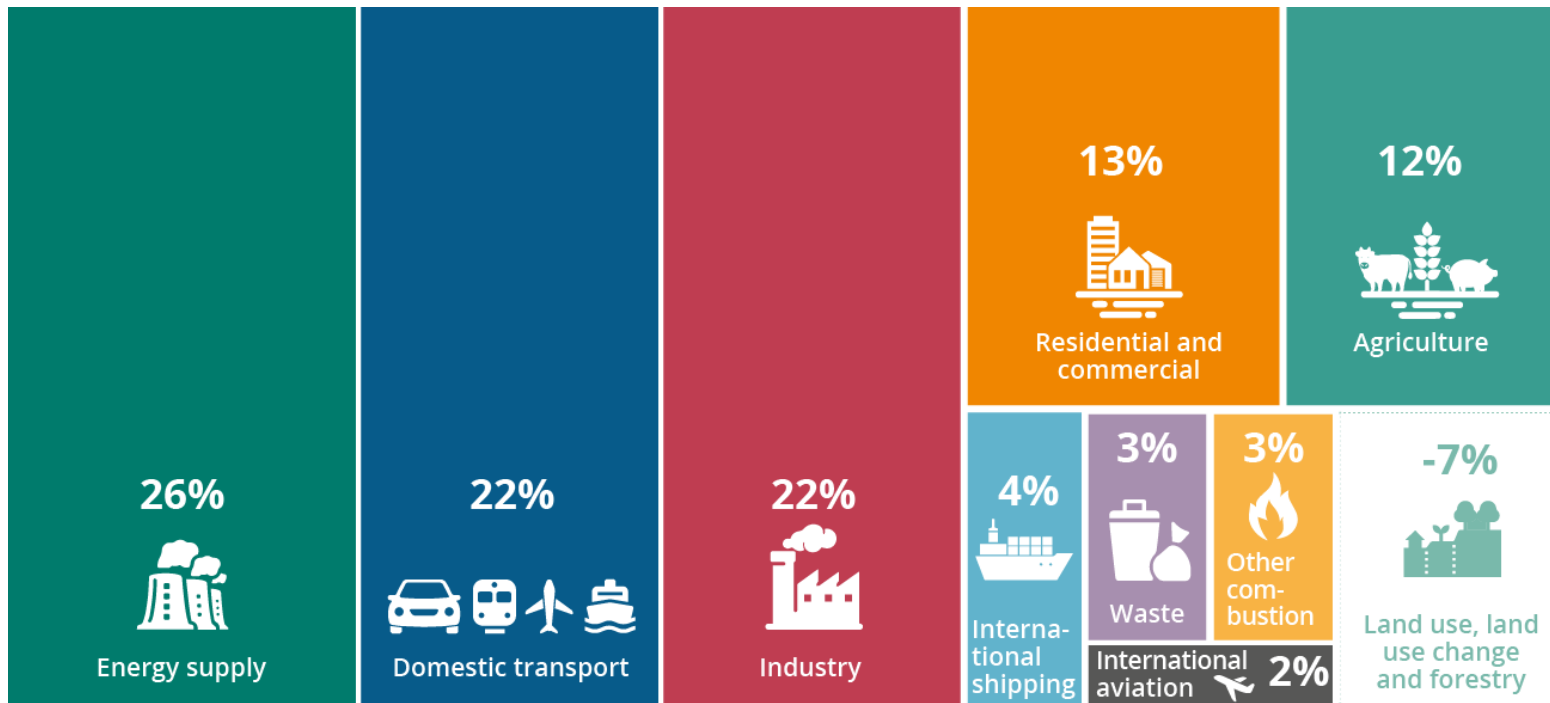


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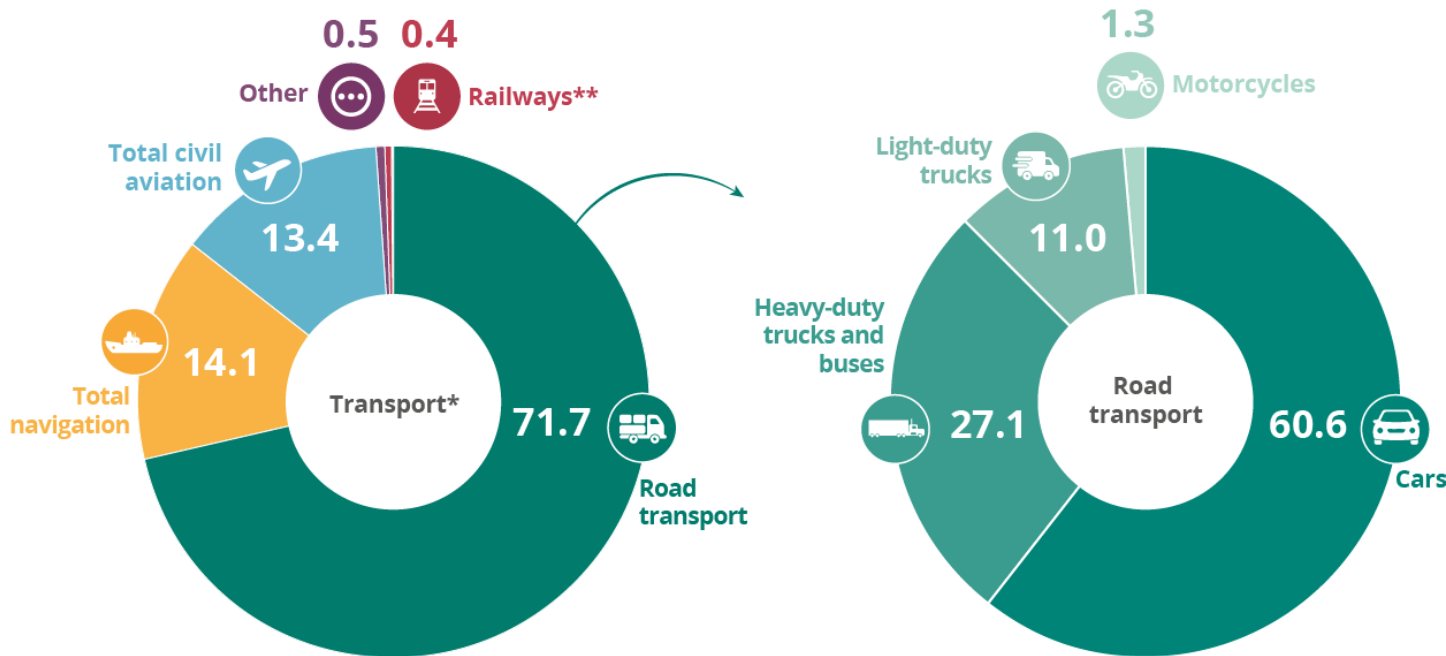
# European GHG emissions per sector (2022)



<https://www.eea.europa.eu/signals-archived/signals-2022/infographics/what-are-the-sources-of>



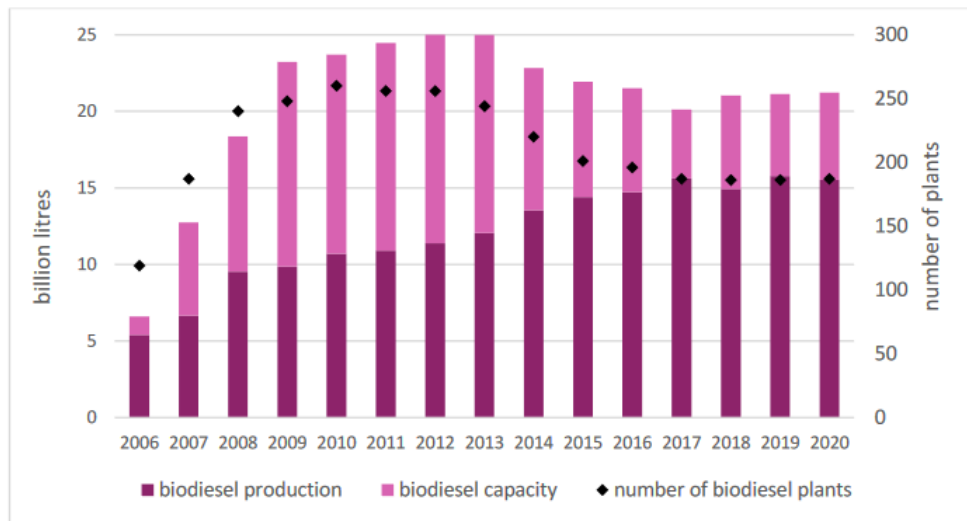
# European GHG emissions in the transport sector (2022)



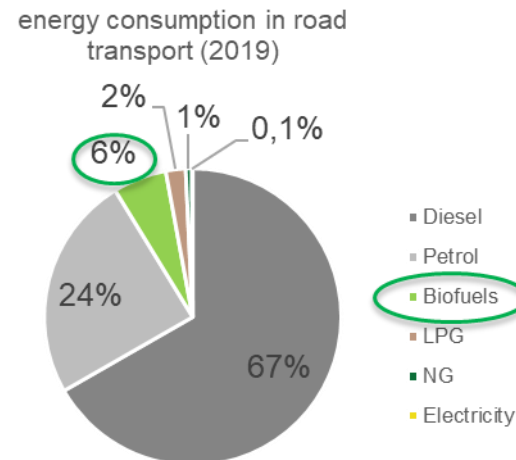
# EU biodiesel production and capacity



**Figure 6.** Evolution of biodiesel production and capacity in the EU



Source: (USDA Foreign Agricultural Service et al., 2021)



EEA Report No 02/2022. Transport and environment report 2021. **Decarbonising road transport — the role of vehicles, fuels and transport demand**

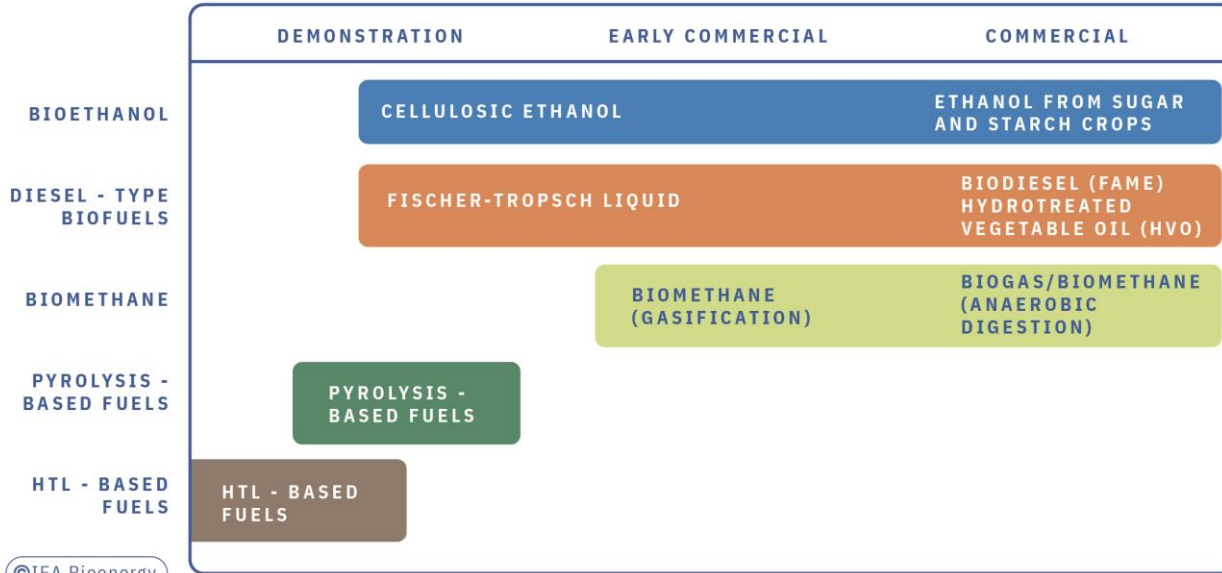
Hurtig O., Buffi M., Scarlat N., Motola V., Georgakaki A., Letout S., Mountraki A., Joanny G, **Clean Energy Technology Observatory: Advanced biofuels in the European Union – 2022 Status Report on Technology Development, Trends, Value Chains and Markets**, Publications Office of the European Union, Luxembourg, 2022, doi:10.2760/938743, JRC130727



# Technology pathways and TRLs



residues

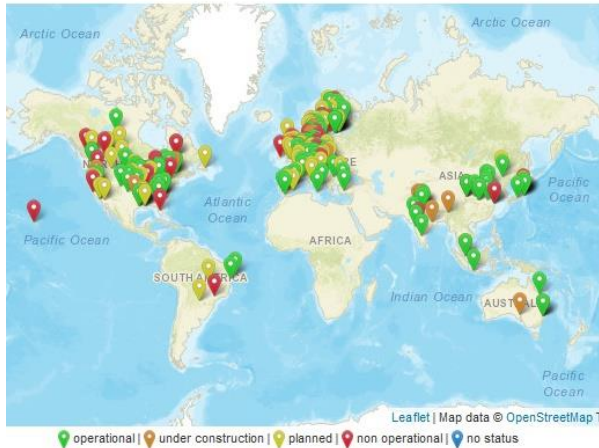


©IEA Bioenergy

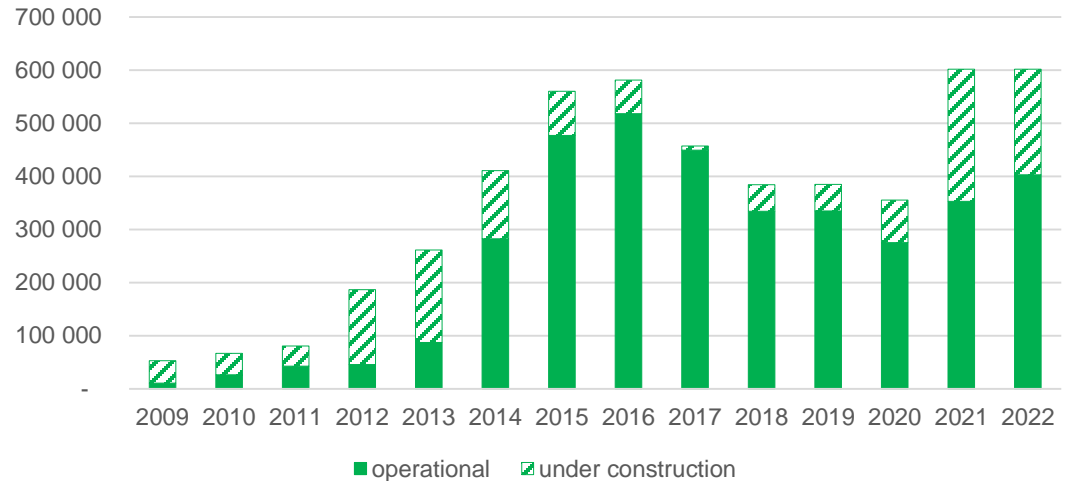
crops



# Deployment of advanced biofuel technologies



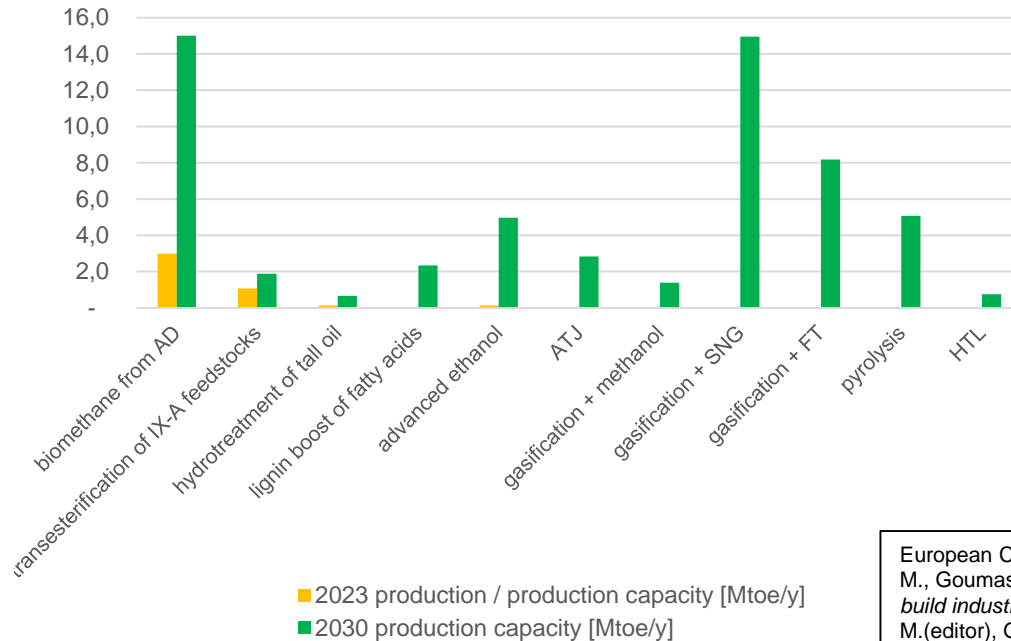
Total production capacity for cellulosic ethanol (worldwide) in t/y



<https://demoplants.best-research.eu/>



# Possible evolution of advanced biofuel production capacities [Mtoe/y]



2030 target for adv. Biofuels	15 – 19 Mtoe
Total possible 2030 production incl. all biomethane	58 Mtoe
Biomethane to other sectors	- 28 Mtoe
Total possible 2030 production with limited biomethane	30 Mtoe

European Commission, Directorate-General for Research and Innovation, Georgiadou, M., Goumas, T., Chiaramonti, D., *Development of outlook for the necessary means to build industrial capacity for drop-in advanced biofuels – Final report*, Georgiadou, M.(editor), Goumas, T.(editor), Chiaramonti, D.(editor), Publications Office of the European Union, 2024, <https://data.europa.eu/doi/10.2777/679307>

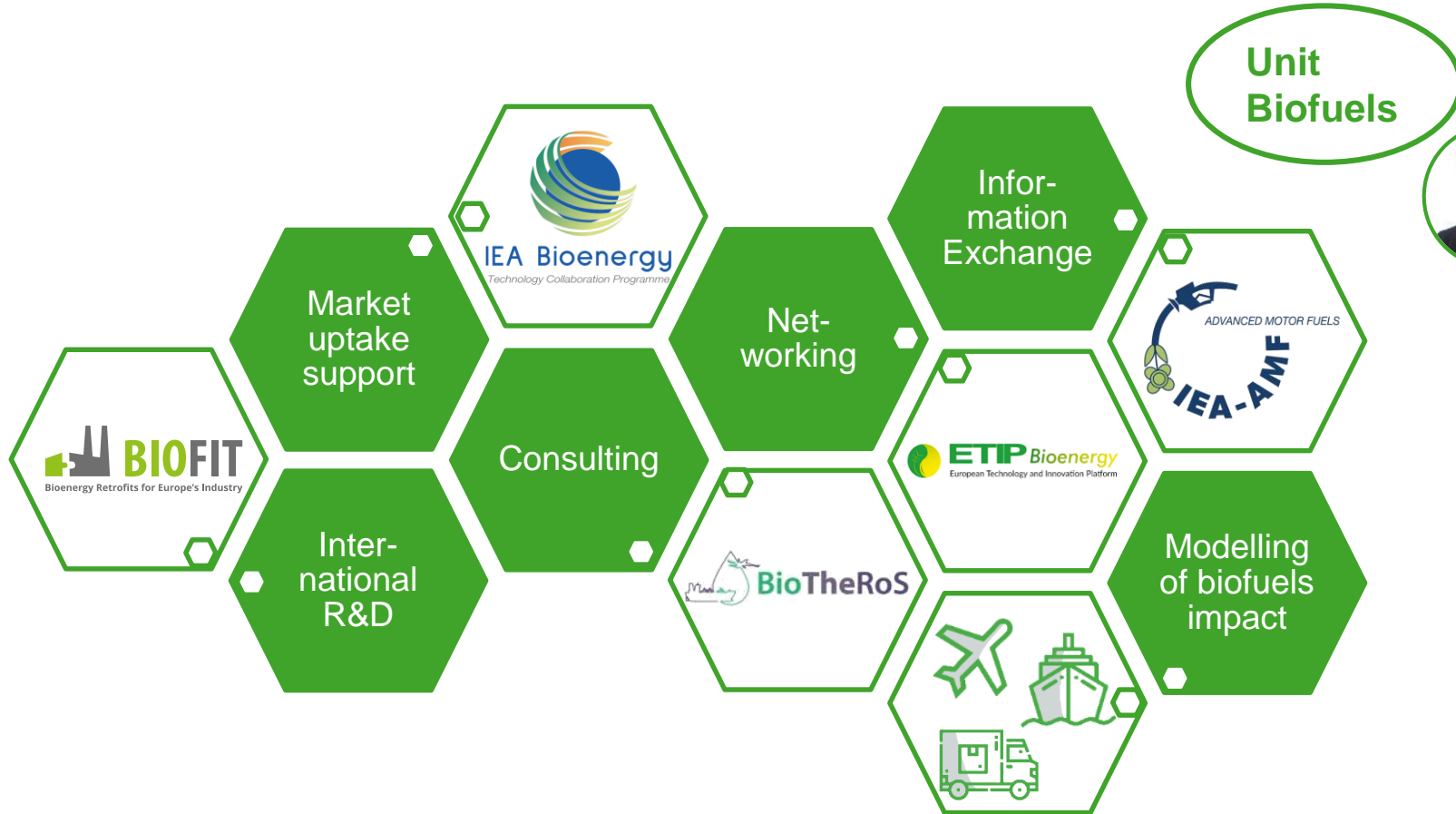
# Implementation barriers / opportunities

- High production **costs** of fuel
- **Financial risks** of demonstration and First-of-its-kind facility
- Uncertainty of regulatory framework and **policies**
- Availability and sustainability of **Feedstock**
- **Policy focus** on other options

- Based on broad variety of biomass feedstocks – **diversification of energy supply**
- Biomass production provides **regional income**
- Applicable in current vehicles now – offer **immediate GHG emission reductions**
- **High energy density** – alternative solution for sectors that are **hard-to-electrify**
- Passenger cars → trucks, ships, planes



# Biofuels – a crucial part of decarbonisation






# Lunch

12:00 – 13:00



 Bundesministerium  
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Klimaschutz, Umwelt,  
Energie, Mobilität,  
Innovation und Technologie



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 Das Land  
Steiermark  
→ Wirtschaft, Tourismus, Regionen,  
Wissenschaft und Forschung




# SPEED-UP ALGORITHMS for advanced simulations

Graz, 26.September.2024

Michael Eßl



 Bundesministerium  
Arbeit und Wirtschaft

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Klimaschutz, Umwelt,  
Energie, Mobilität,  
Innovation und Technologie

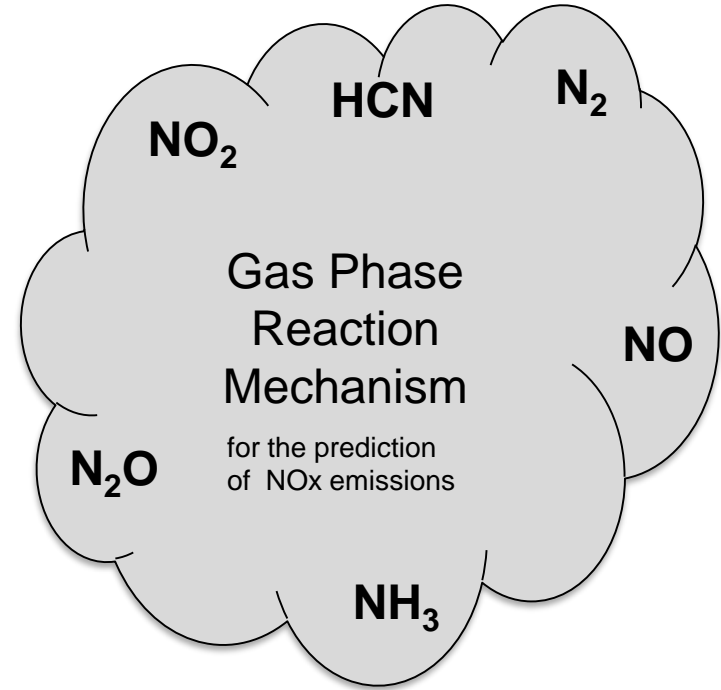
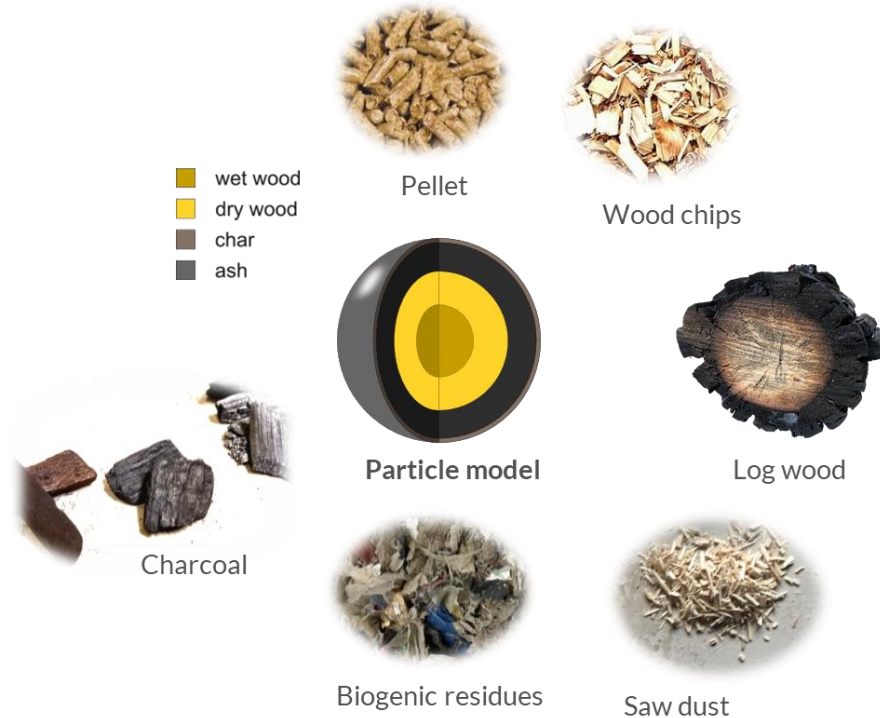


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# Areas in need of speed up

## solid phase and gas phase





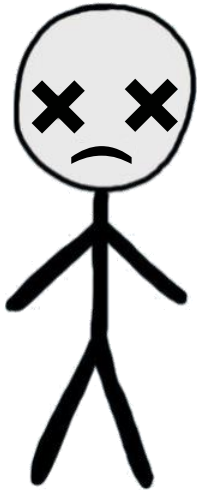
# Speed-up of gas phase

complexity of reaction mechanisms for NO<sub>x</sub> in biomass combustion



**global**

< 10 species  
< 10 reactions



**hybrid**

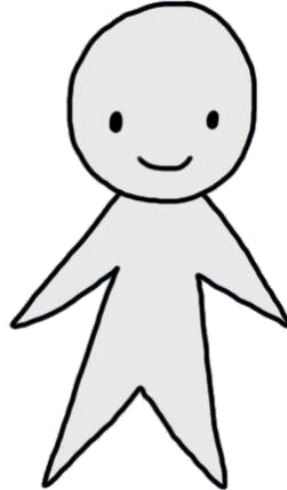
10-20 species  
< 100 reactions



Speed-up Factor: **2.04**

**reduced**

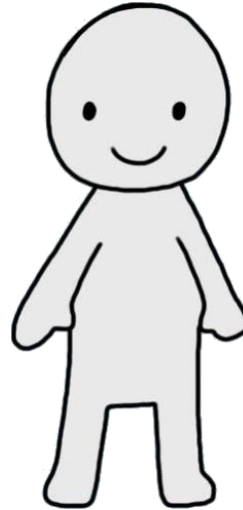
20-50 species  
100-400 reactions



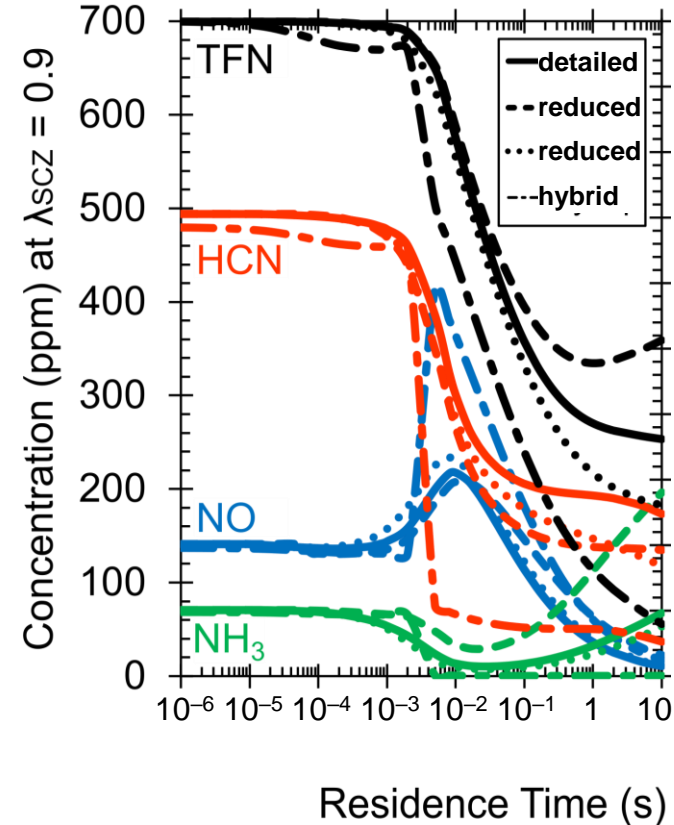
**1.58**

**detailed**

> 100 species  
> 1000 reactions



**1.00**



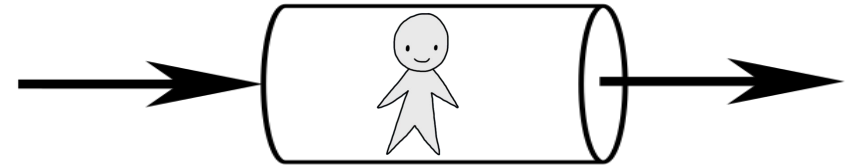
# Speed-up of gas phase

speed up methods for gas phase reactions

Test of different models and methods for the speed-up of gas phase chemistry calculation

Method	Speed up Factor
Base case	1.00
Chemkin solver	1.66
Dynamic Reduction	1.05
ISAT	5.00

## Plug Flow Reactor (PFR)

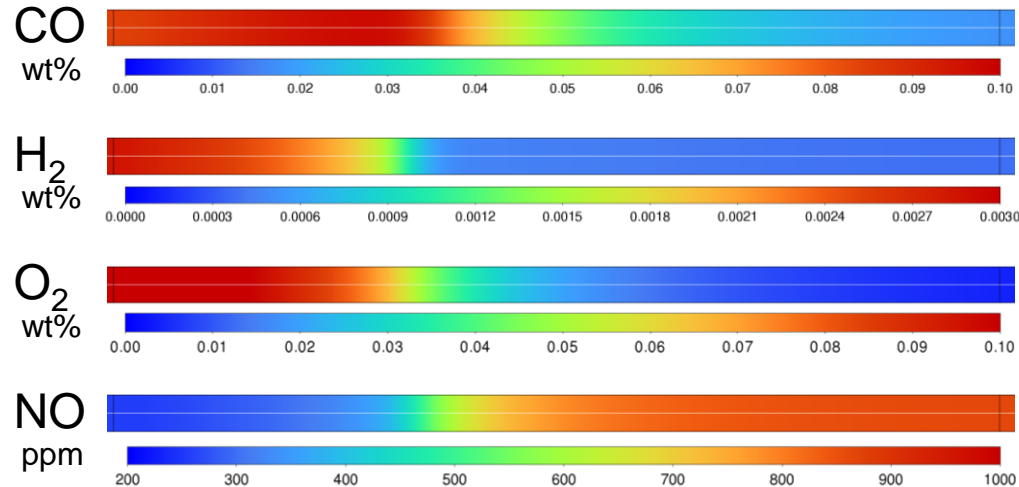


Temperature: 1000°C

Residence time: 0.01 s



## Result of CFD TestCase



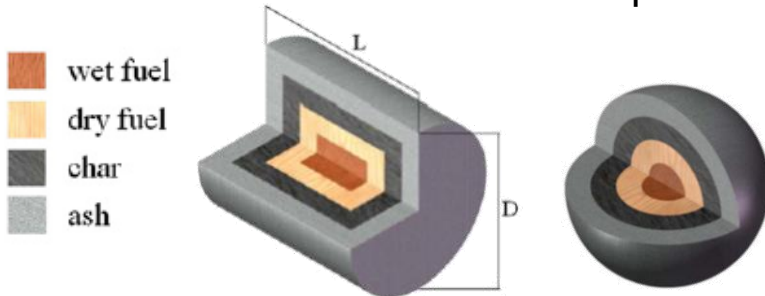
# Speed-up of particle models

## thermally thick vs. thermally thin



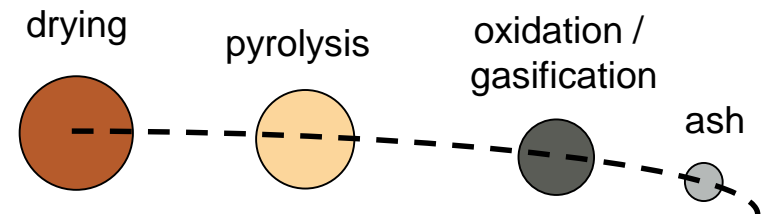
### Thermally thick model (Layer model)

- Resolved temperature gradient in particle
- Parallel decomposition reactions
- Three component pyrolysis model
- Volumetric gasification reactions
- More accurate description
- Simulation time: 1 – 20 min / particle



### Thermally thin model

- Equal temperature throughout the particle
- Serial decomposition reactions
- Single rate pyrolysis model
- Surface char reactions
- Simple models
- Simulation time: < 1 sec / particle

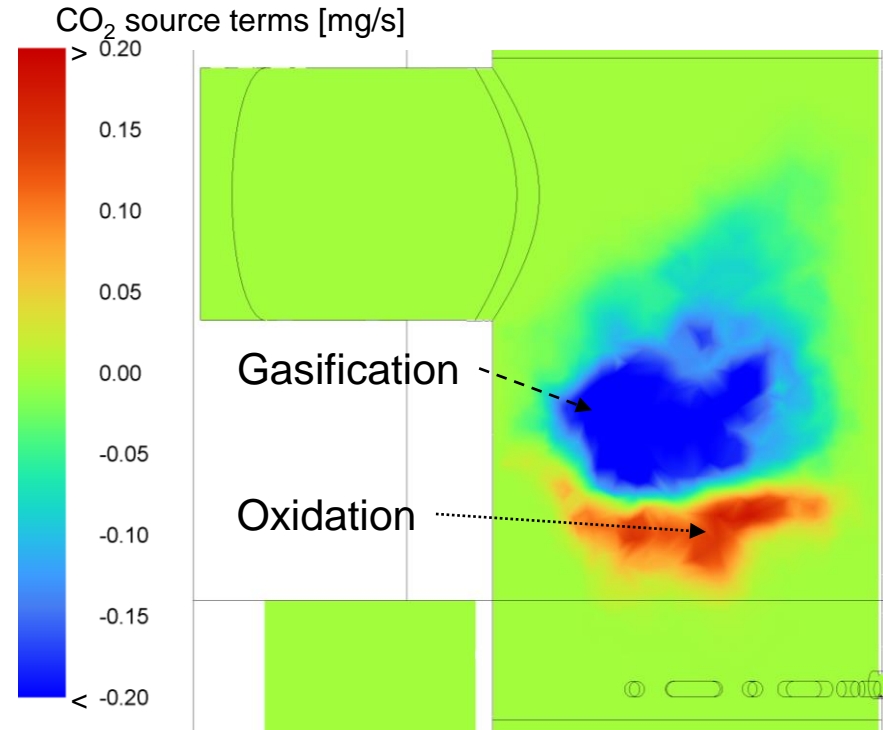
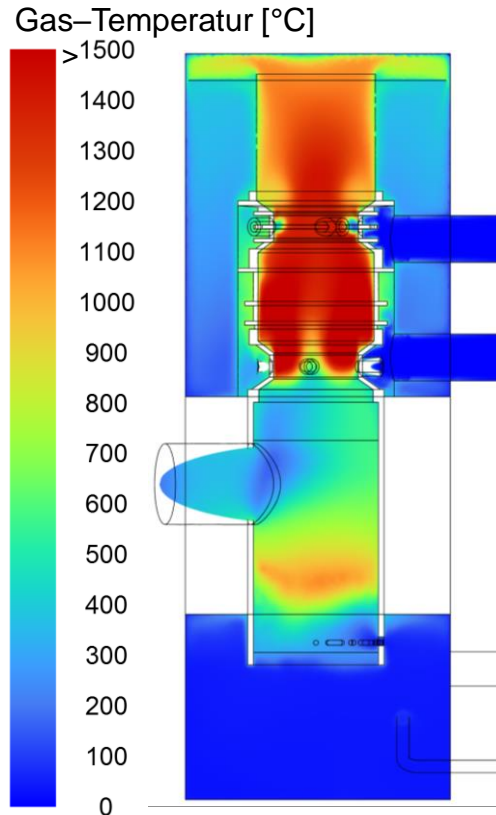


# Speed-up of particle models

## application of models to a small scale gasifier



- Example of a 30 kW gasifier
- for gasification applications an accurate description of char reactions is especially important
- Combination of thermally thin and thermally thick model



Speed-up Factor: ~ 5.0

# Outlook

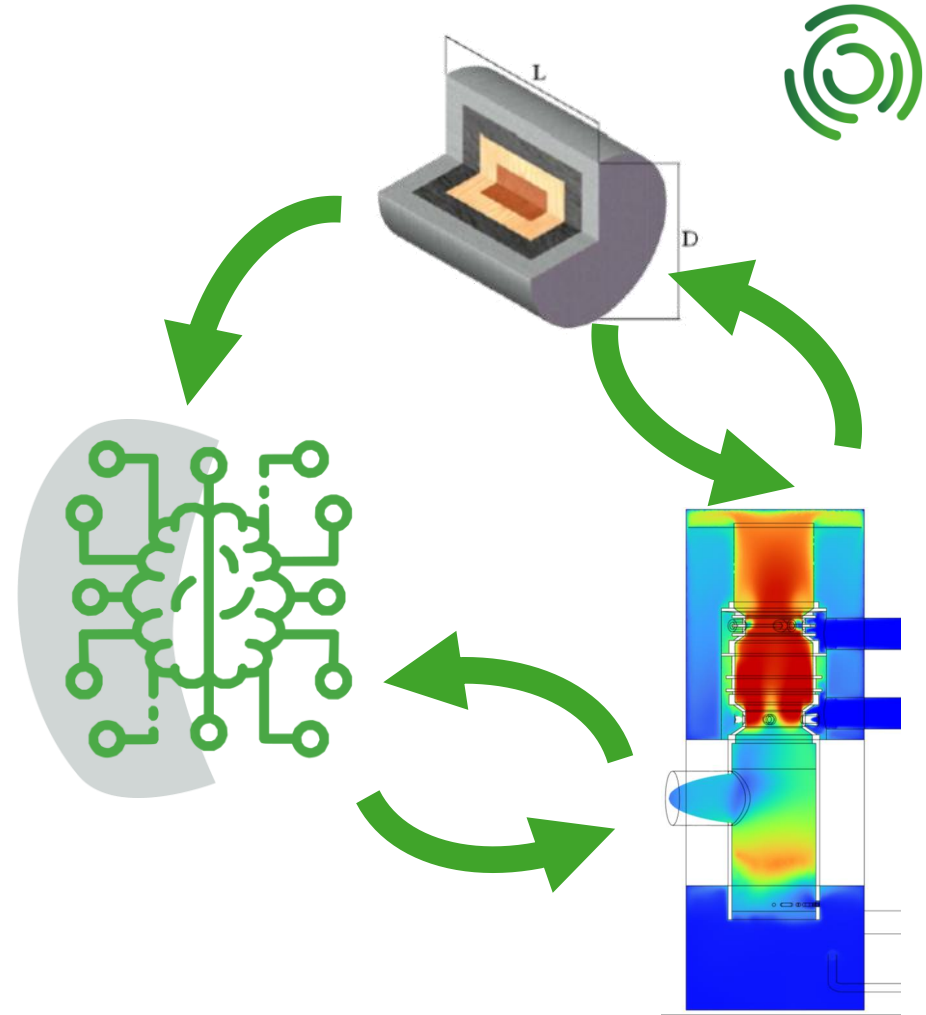
further development and current work

## Gas phase reactions

- Derivation of reactor networks via cell clustering → see poster of “Modular simulation framework”

## Particle model

- Relocate the layer model to an external solver (Julia) that can use several computing cores in parallel and also allows fast switching between models
- Implementation of a neural network that mimics the layer model




# Multiscale modeling of metal oxide and biomass conversion for chemical looping processes

BEST – Zentrumstag, Graz, 26.9.2024

Thomas Steiner, Andrés Anca-Couce, Kai Schulze



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Energie, Mobilität,  
Innovation und Technologie



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# Agenda

1. What are
  - chemical looping
  - multiscale modeling
2. Model development & validation
3. Model application



energy&fuels

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Article

## On the Applicability of Iron-Based Oxygen Carriers and Biomass-Based Syngas for Chemical Looping Hydrogen Production

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Thomas Steiner,\* Lukas von Berg, Andrés Anca-Couce, and Kai Schulze

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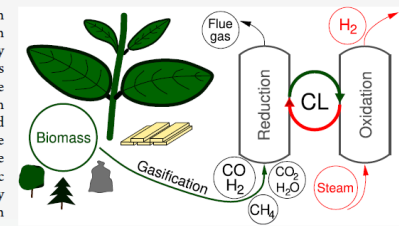
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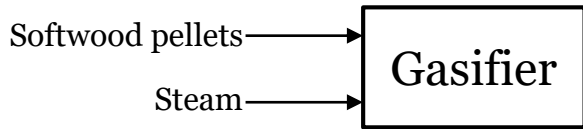
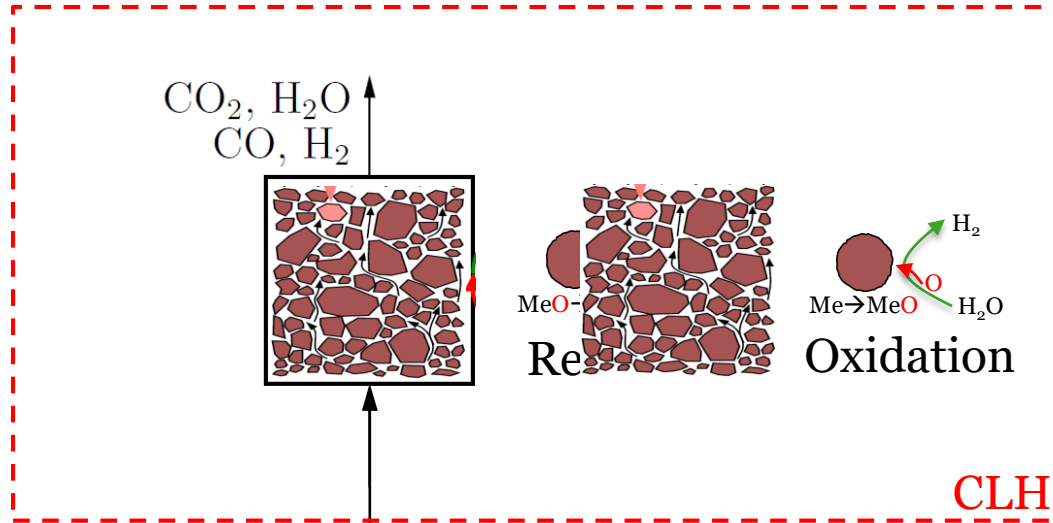
Metrics & More

Article Recommendations

**ABSTRACT:** The chemical looping hydrogen (CLH) production process typically uses iron-based oxygen carrier materials and can provide hydrogen with high purity. Chemical looping is particularly attractive when renewable fuels like syngas from biomass gasifiers are used. This work provides a novel assessment of the possible thermodynamic and kinetic limitations for iron-based oxygen carriers in CLH fueled by biomass-based syngas, with a detailed study employing synthetic ilmenite ( $\text{Fe}_2\text{O}_3 + \text{TiO}_2$ ). Its phase diagram with  $\text{H}_2/\text{H}_2\text{O}$ - or  $\text{CO}/\text{CO}_2$ -mixtures was compared to the typical Baur–Glaessner diagram for iron oxides. Thermogravimetric analyses underlined the necessity to consider  $\text{TiO}_2$  as a chemically active component for this material, in contrast to the common simplification of inert support materials. The validated phase



# Chemical looping hydrogen (CLH)

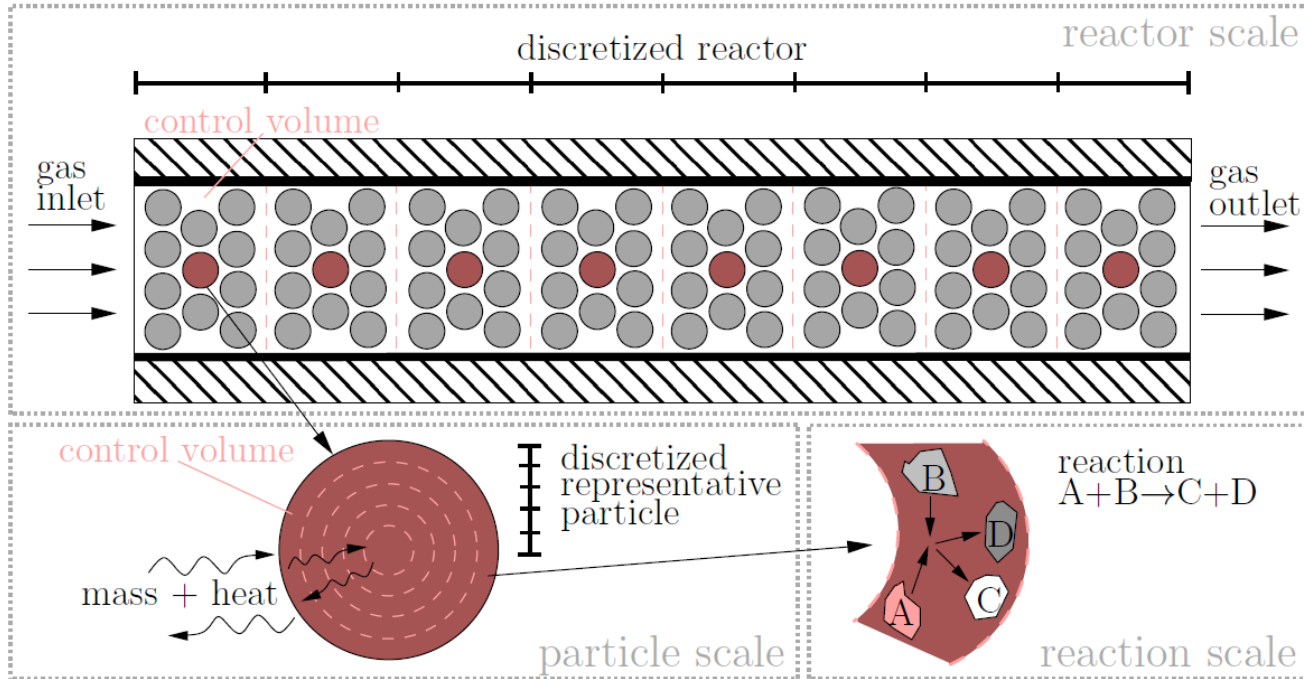


syngas composition

	H <sub>2</sub>	H <sub>2</sub> O	CO	CO <sub>2</sub>	CH <sub>4</sub>	N <sub>2</sub>
vol % w.b.	19.9	45.0	10.3	10.2	4.1	10.5



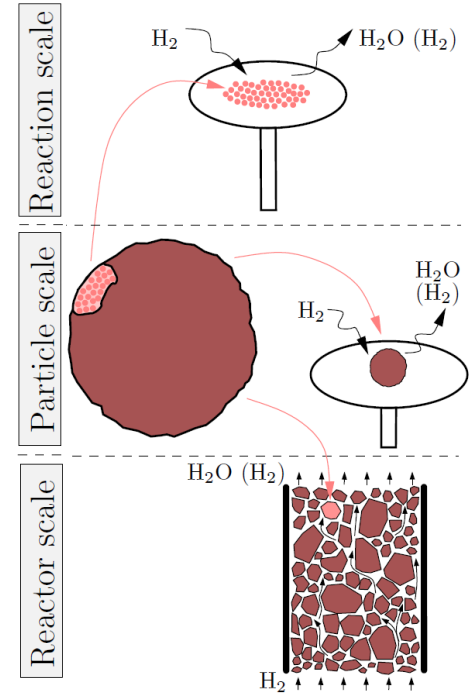
# Multiscale model development



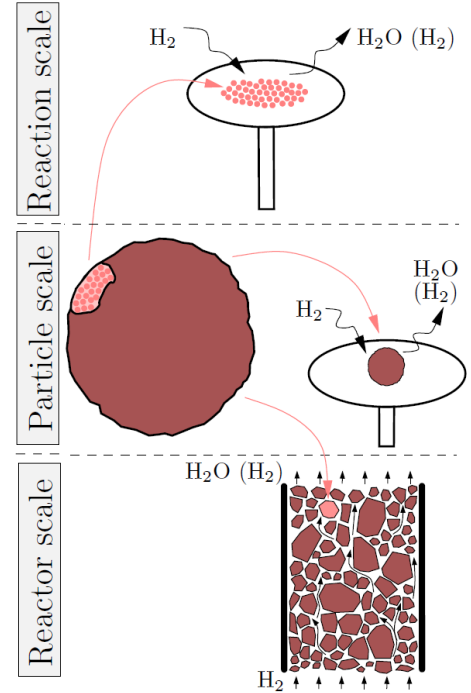
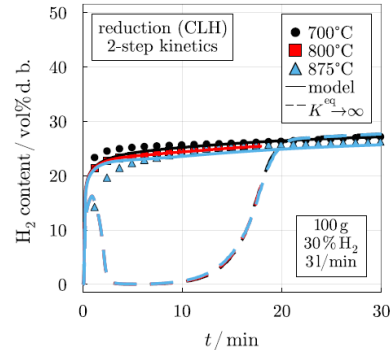
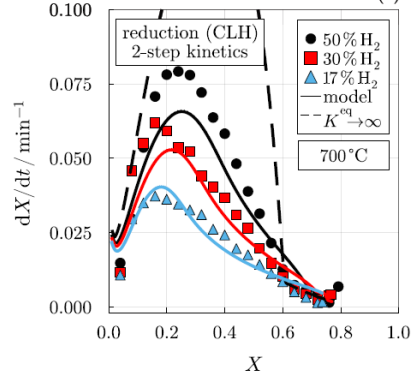
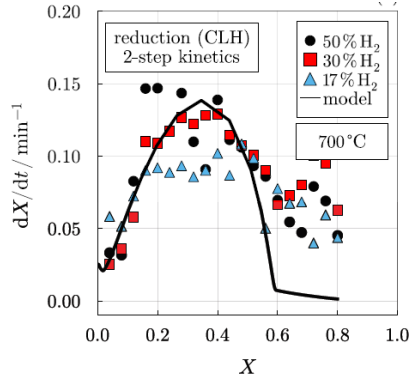
# Multiscale model validation



- OC: synthetic ilmenite ( $\text{Fe}_2\text{O}_3 + \text{TiO}_2$ )
- Fuel: syngas,  $\text{H}_2 / \text{H}_2\text{O}$
- Measurements at all three scales
  - reaction – thermogravimetry of powders
  - particle – thermogravimetry of pellets
  - reactor – fixed bed reactor (many pellets)

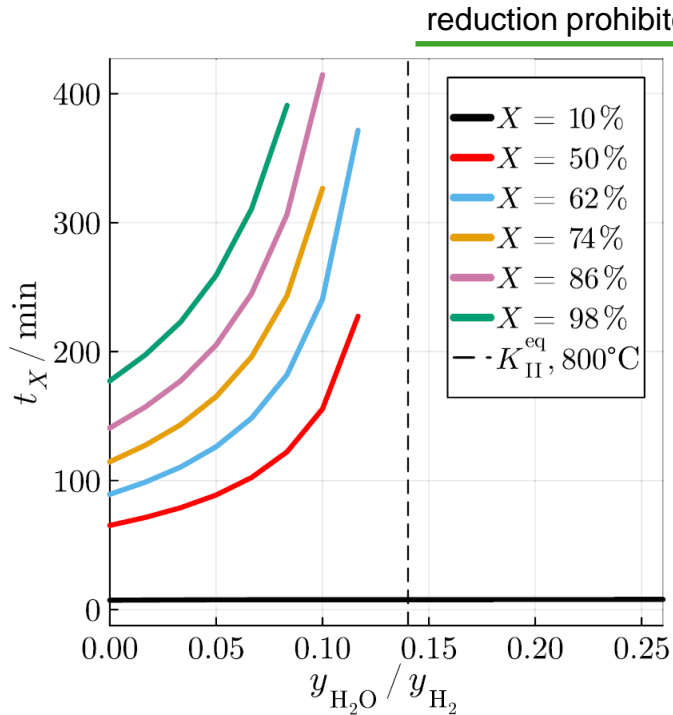


# Multiscale model validation (2)



$dX/dt$  ... conversion rate  
 $X$  ... conversion  
 $K^{eq}$  ... equilibrium constant

# Model application – Does fuel cleaning pay off?



- $t_x$  ... bed reduction time
- $X$  ... conversion (100% = reduced)
- $y_{\text{H}_2\text{O}}/y_{\text{H}_2}$  ... molar feed ratio
- $K_{\text{II}}^{\text{eq}}$  ... equilibrium constant



## Acknowledgement

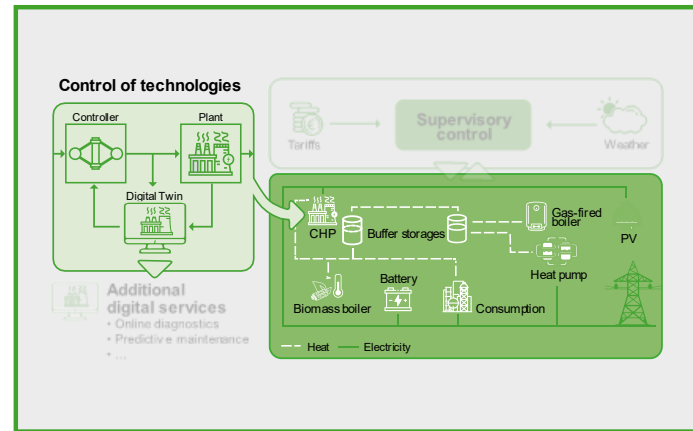
- *The COMET Module is funded within COMET – Competence Centers for Excellent Technologies – by BMK, BMDW as well as the co-financing federal province Styria. The COMET programme is managed by FFG. [www.ffg.at/comet](http://www.ffg.at/comet)*

# Model-Based Control of the Generated Steam Mass Flow in a Fluidized-Bed Waste Incineration Plant

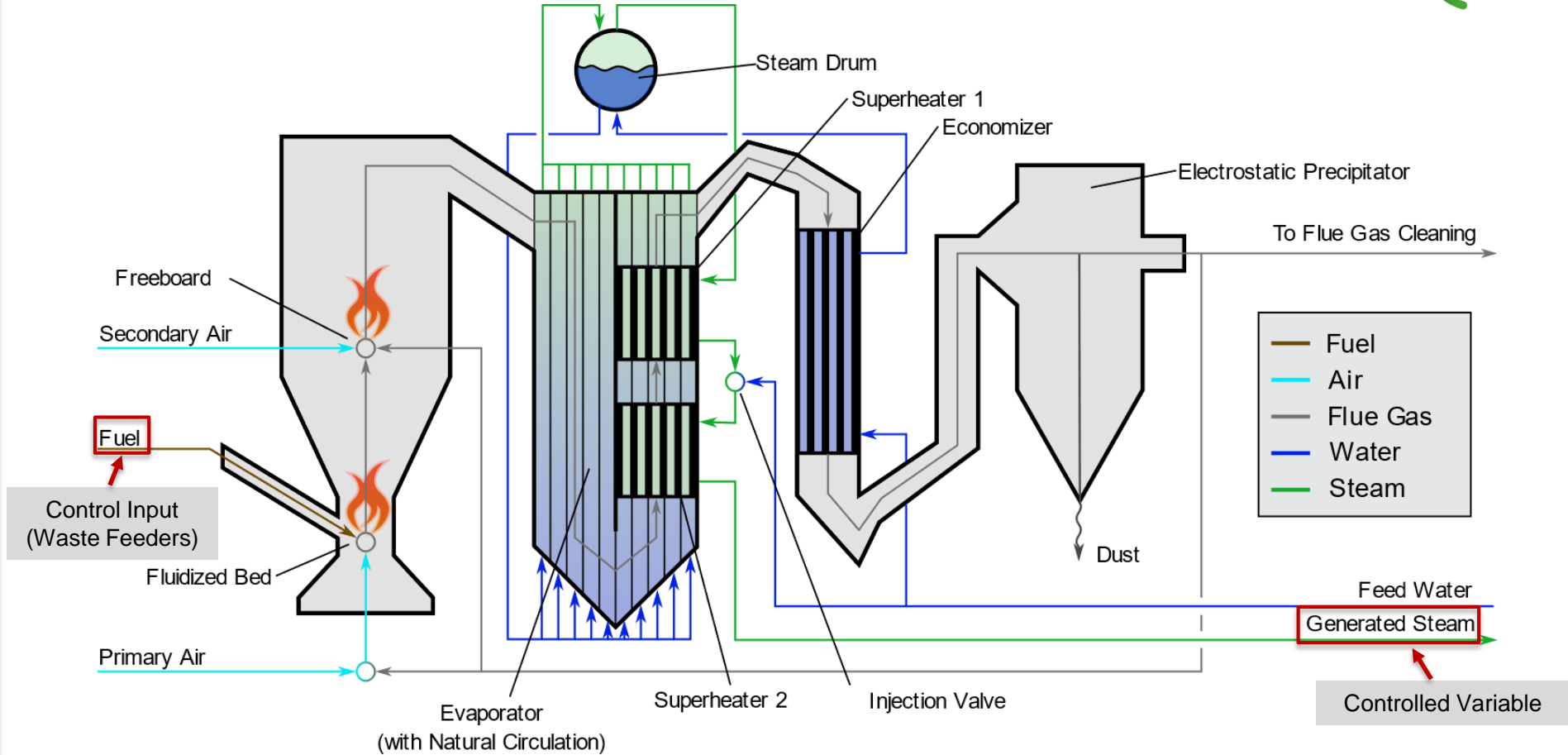
Graz, September 26th, 2024

Area 2.2

Helmut Niederwieser, Markus Gölles,  
Florian Jäger, Friedrich Kirnbauer

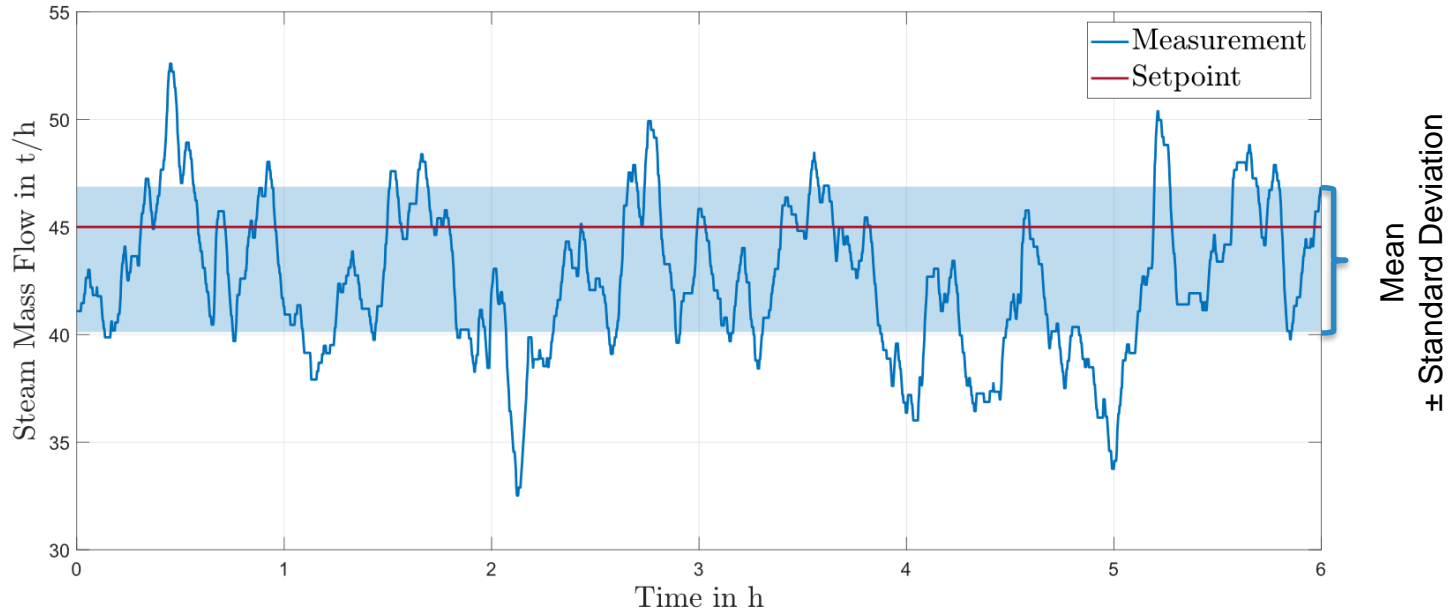


# Considered Waste Incineration Plant





# Motivation – Strong Fluctuations of the Generated Steam Mass Flow



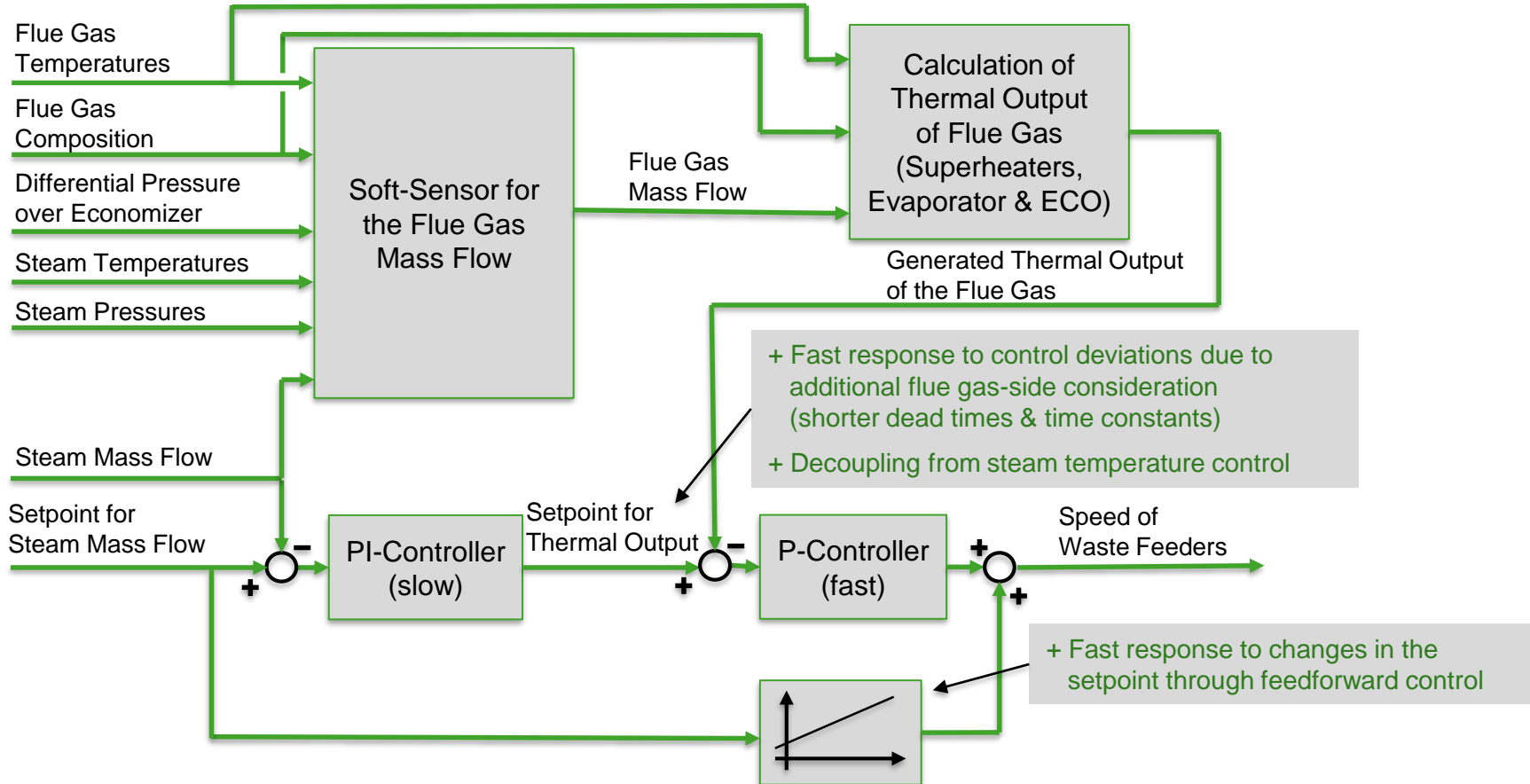
- Process fluctuations lead to...
  - increased wear
  - high failure rates
  - poor efficiency
- **Goal:** stable plant operation that is as constant as possible



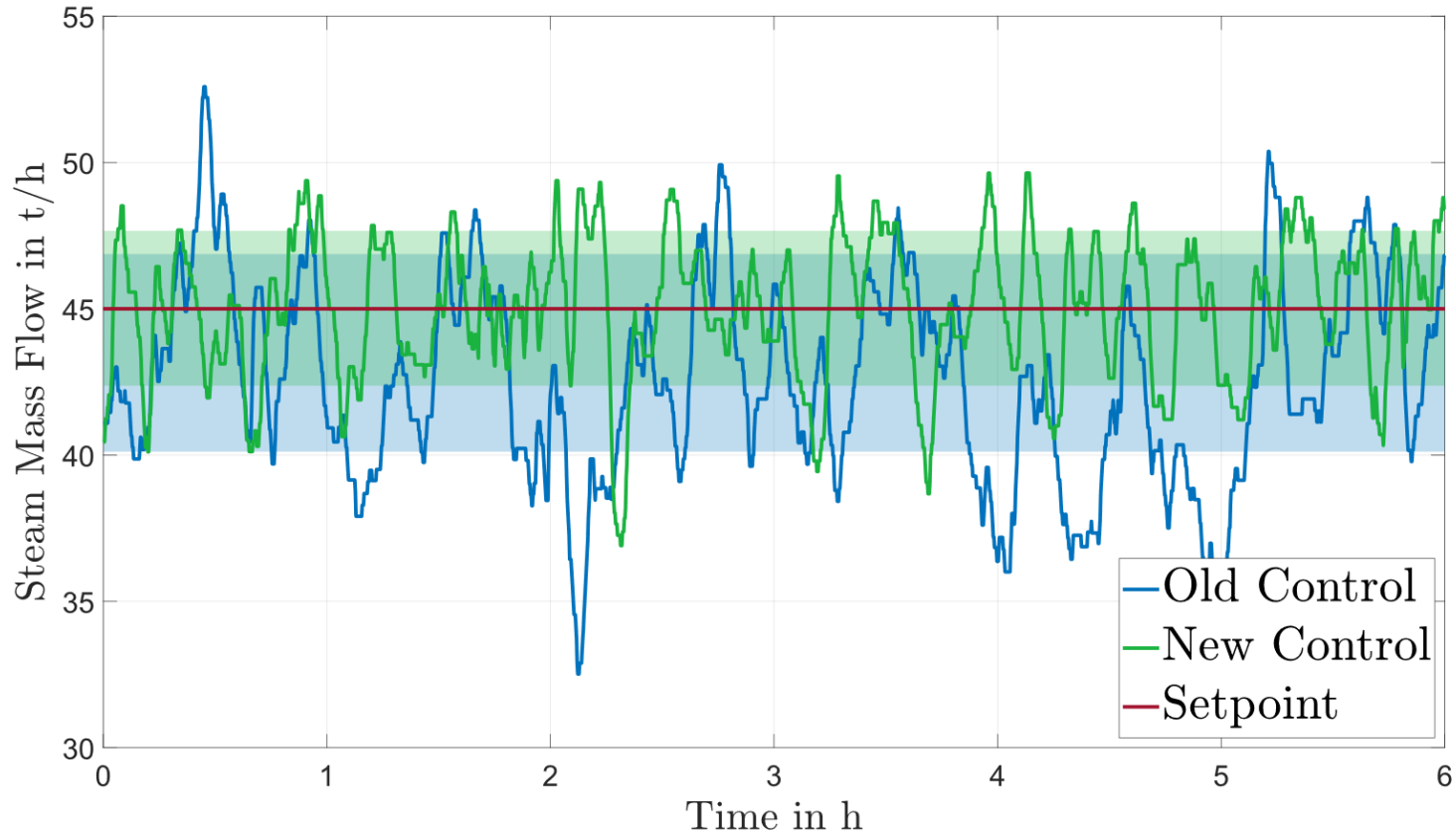
**model-based control**



# Model-Based Control Design

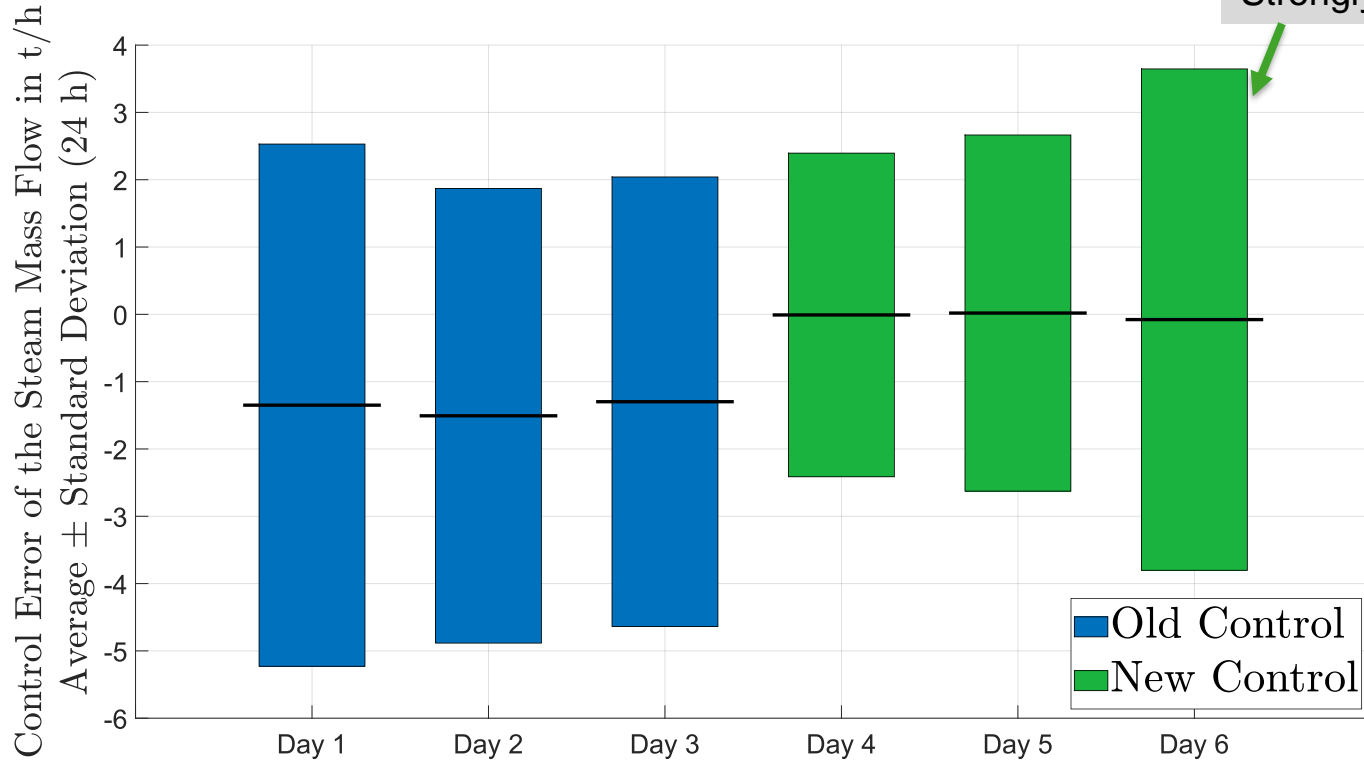


# Exemplary Results – Generated Steam Mass Flow





# Statistics of the Control Error



Strongly inhomogeneous fuel

Mean Error:

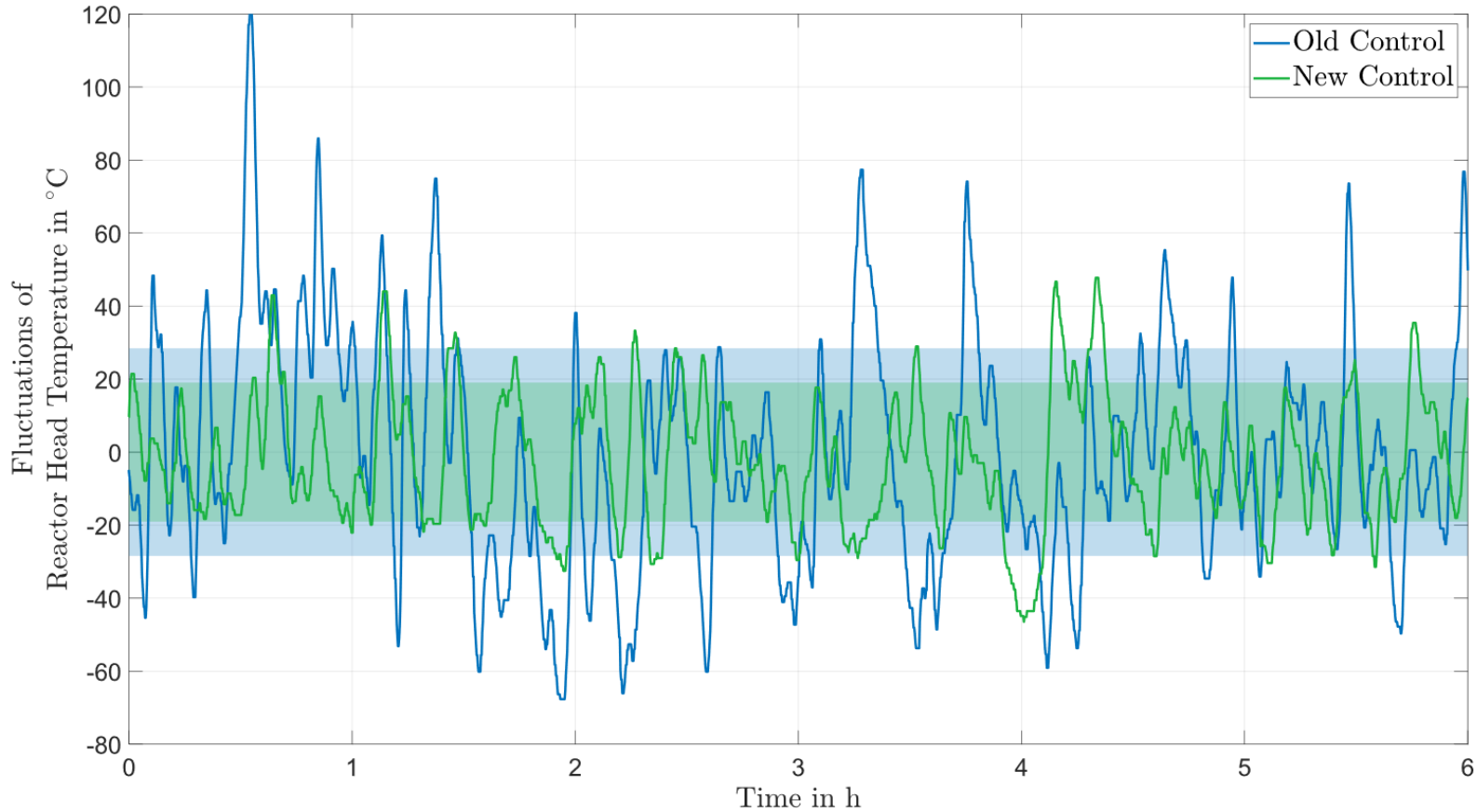
1.51 t/h (Old)  
0.01 t/h (New)

Standard Deviation:

3.38 t/h (Old)  
2.65 t/h (New)

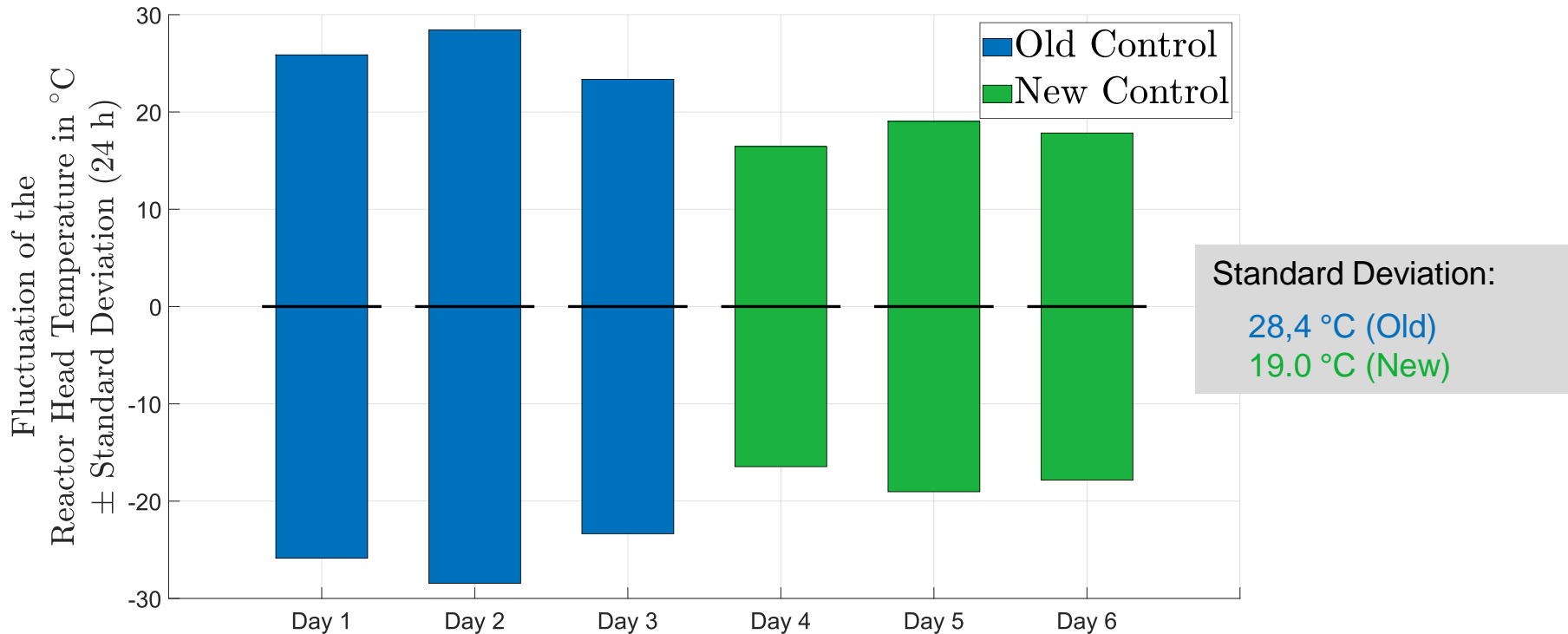


# Exemplary Results – Reactor Head Temperature





# Statistics of the Fluctuations of the Reactor Head Temperature



# Conclusion



- Model-based control for generated steam mass flow:
  - Realizable through **soft sensor for flue gas mass flow**<sup>1),2)</sup>
  - Implementation requires **software update** only
- Statistical evaluation (in terms of standard deviation):
  - Reduction of **generated steam mass flow** fluctuations by **23 %**
  - Reduction of **reactor head temperature** fluctuations by **34 %**
- Outlook:
  - Algorithm for systematic premixing of the fuel
  - Model-base control of the oxygen content in the flue gas



<sup>1)</sup>Niederwieser, H., Zemann, C., Goelles, M., & Reichhartinger, M. (2020). Model-Based Estimation of the Flue Gas Mass Flow in Biomass Boilers. *IEEE Transactions on Control Systems Technology*, 29(4), 1609-1622.

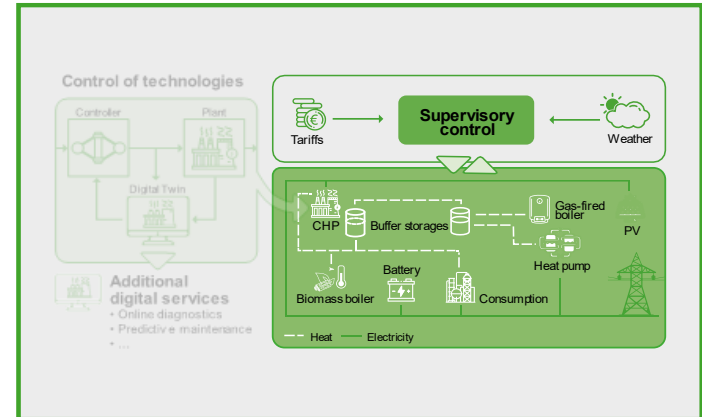
<sup>2)</sup>Niederwieser, H., Zemann, C., Gölles, M., & Reichhartinger, M. (2020, July). Soft-Sensor for the On-Line Estimation of the Flue Gas Mass Flow in Biomass Boilers with Additional Monitoring of the Heat Exchanger Fouling. In *28th European Biomass Conference & Exhibition* (pp. 280-284).

# Modular, predictive, optimization-based supervisory control of multi-energy systems: General introduction and practical application for the energy management in single-family homes

Graz, September 26th, 2024

Area 2.2

**Astrid Leitner**, Daniel Muschick,  
Valentin Kaisermayer, Andreas Moser,  
Bernd Riederer, Mathias Schwendt  
Markus Gölles, Uwe Poms



# Requirements for controlling multi-energy systems



## optimal operation

(efficiency, CO<sub>2</sub> emissions, ...)

- **optimization-based**  
ensures optimal operation of the system  
by targeted utilization of the different technologies

## volatility

of production and consumption

- **predictive**  
integration of weather and price forecasts  
calculation of forecasts for yields and consumptions

## variation range

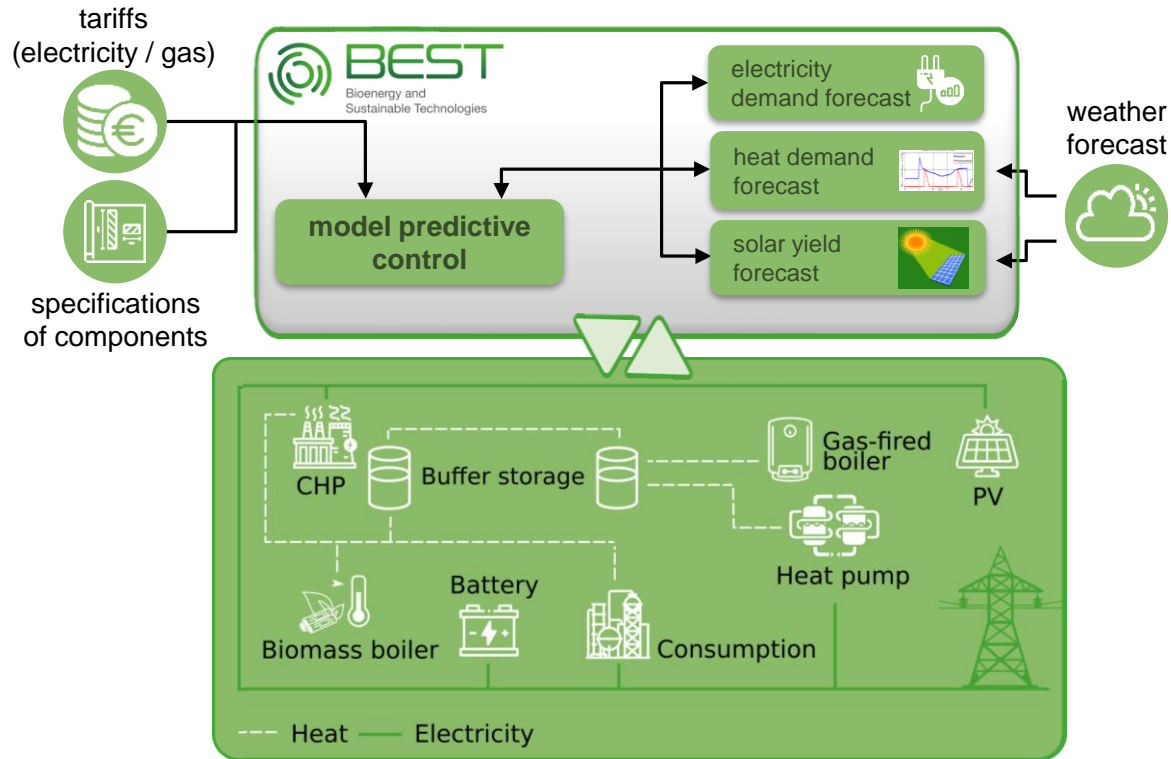
of the configurations

- **modular**  
automatic (re)formulation of the optimization problem  
based on the specifications of the components





# Modular, predictive, optimization-based supervisory control of multi-energy systems





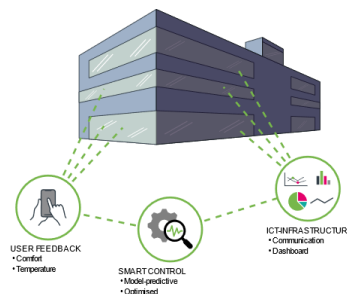
# Applications and commercial products

## ■ One software framework for various applications

- Single-family homes
- Commercial buildings
- District heating networks
- Industrial applications

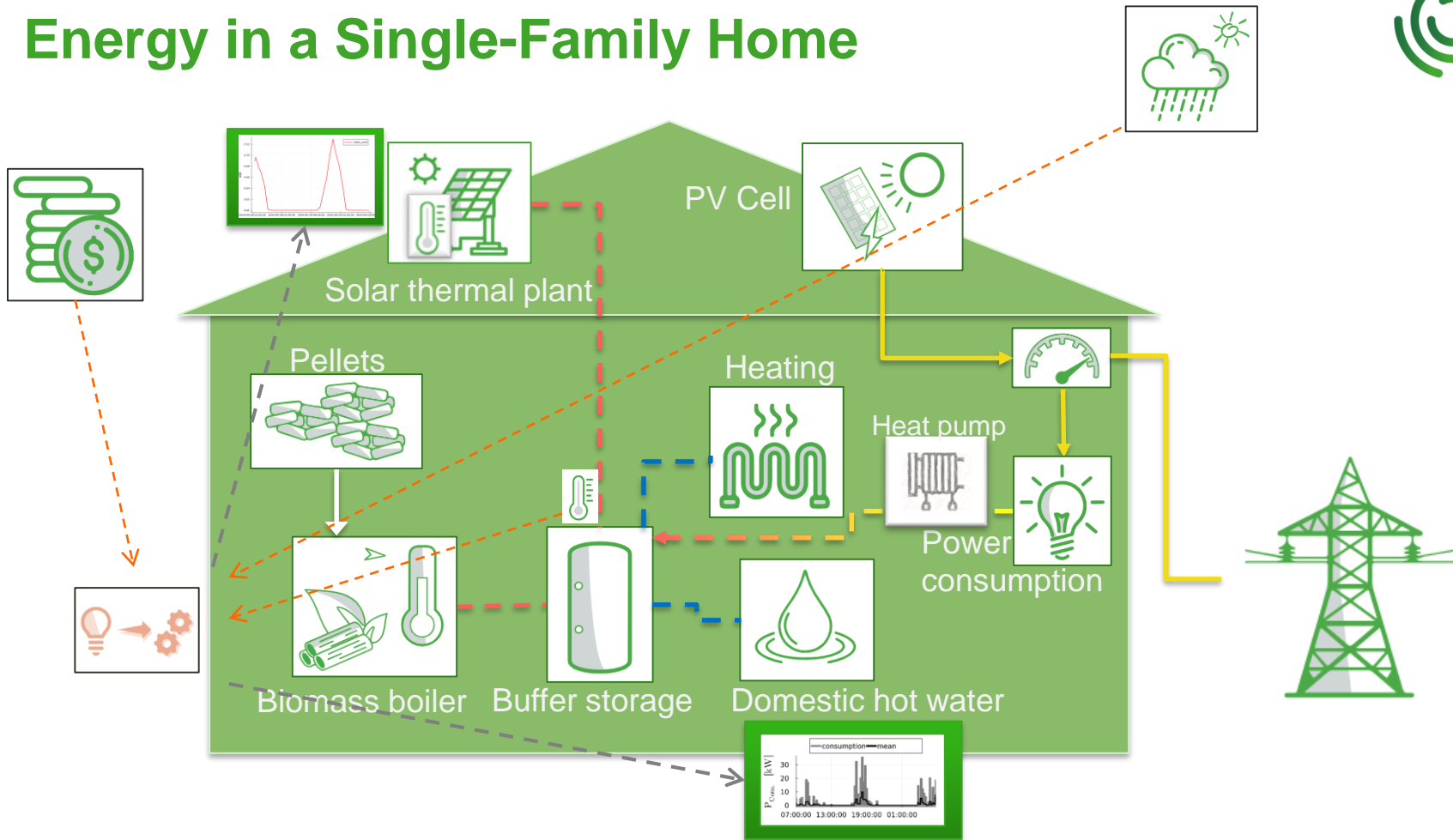


### Workshop

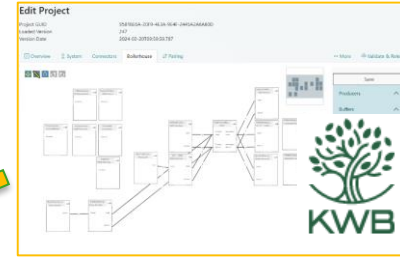


**Achievable improvements (efficiency, CO<sub>2</sub> emissions, ...): ~ 5-10%**

# Energy in a Single-Family Home



# Implementation: Product



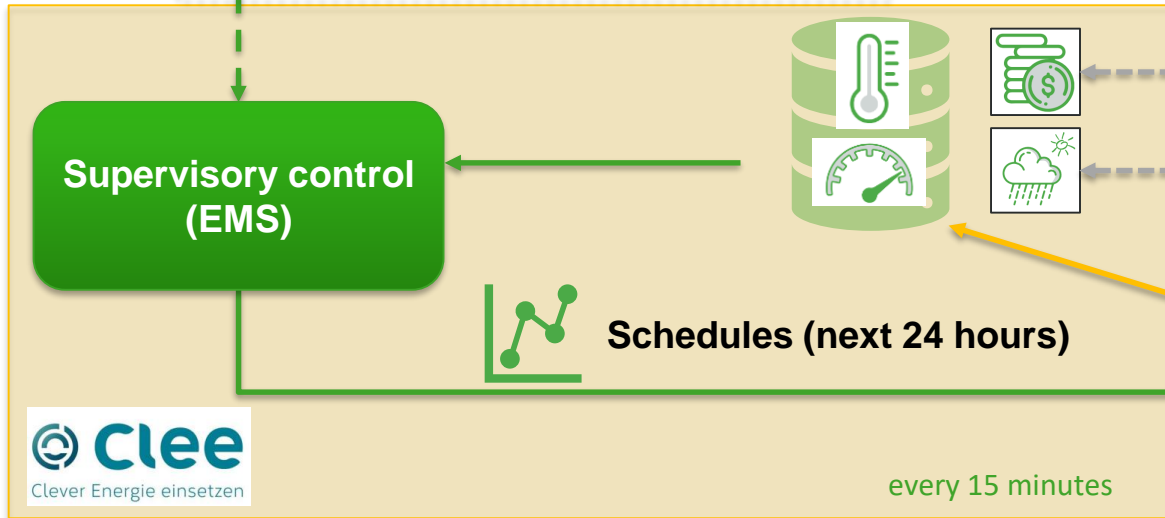
configuration

```

{
  "type": "EmissionPump",
  "name": "70F2c2b8-9844-4a25-8cdf-2a8c62ade98d",
  "properties": {
    "Nominal Feed Temperature": "60",
    "Maximum Inlet Temperature": "50",
    "Relative On off cost": "0.1",
    "Nominal Electrical Power": "1.17",
    "COP": "3.22",
    "Nominal Output Power": "4.2",
    "Minimum Operating Time": "1800",
    "Minimum Downtime": "900",
    "Is Optimized": "true"
  }
}

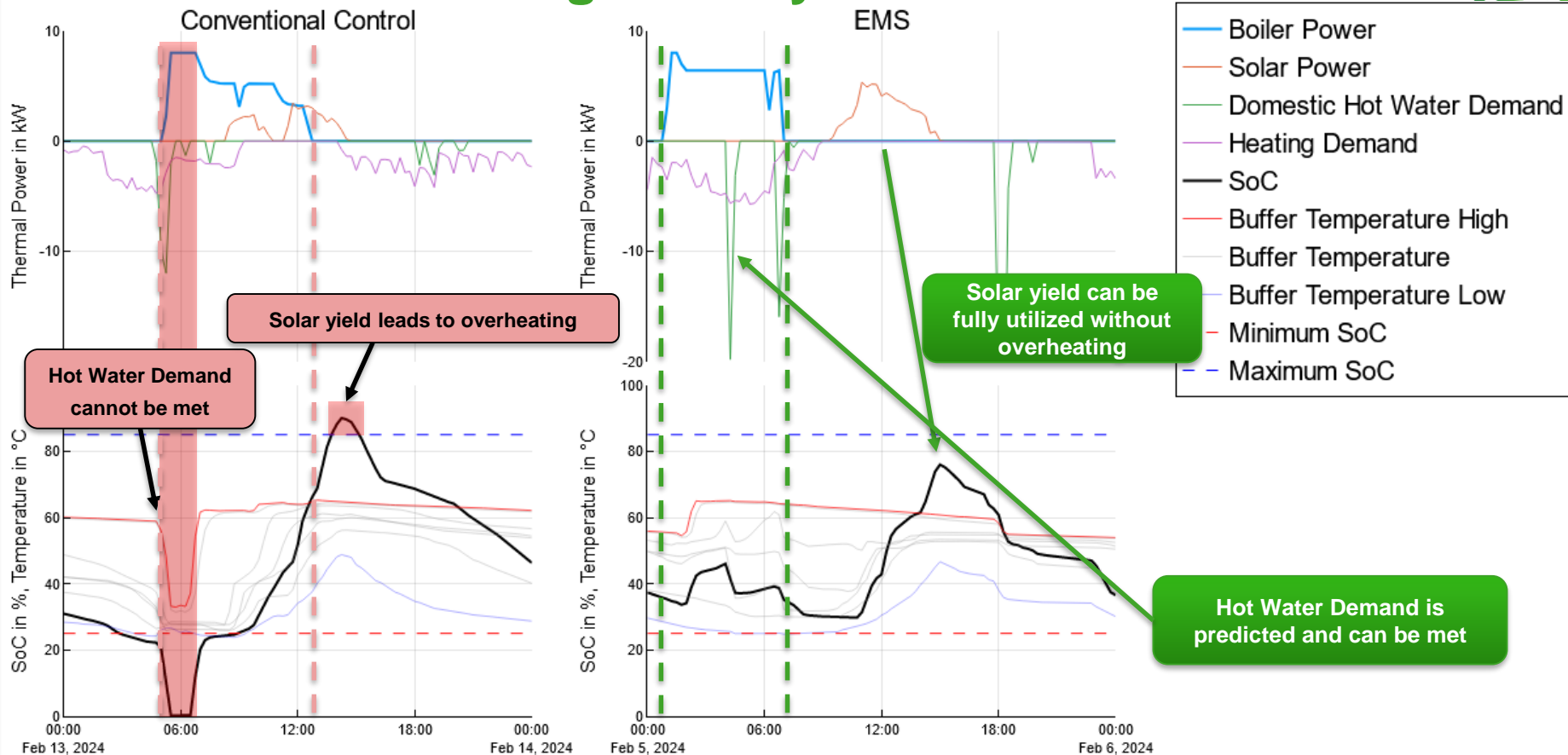
```

Initialization



Runs in more than 100 single-family homes

# Results from a single-family home in Graz





## Conclusion

- Multiple producers, storages and consumers with different constraints  
→ modular, predictive, optimization-based supervisory control
- Product for single-family homes



## Outlook

- Combining heat and electricity
- Dealing with faulty components

# Modular, predictive, optimization-based supervisory control of multi-energy systems: General introduction and practical application for the energy management in single-family homes

Graz, September 26th, 2024

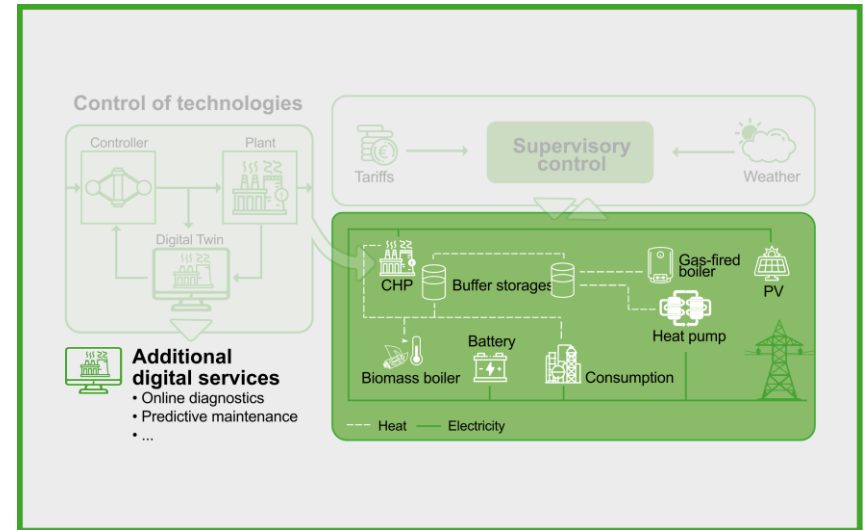
Area 2.2

**Astrid Leitner**, Daniel Muschick,  
Valentin Kaisermayer, Andreas Moser,  
Bernd Riederer, Mathias Schwendt  
Markus Gölles, Uwe Poms

# Monitoring of a Renewable Flow Battery

Graz, 26.09.2024

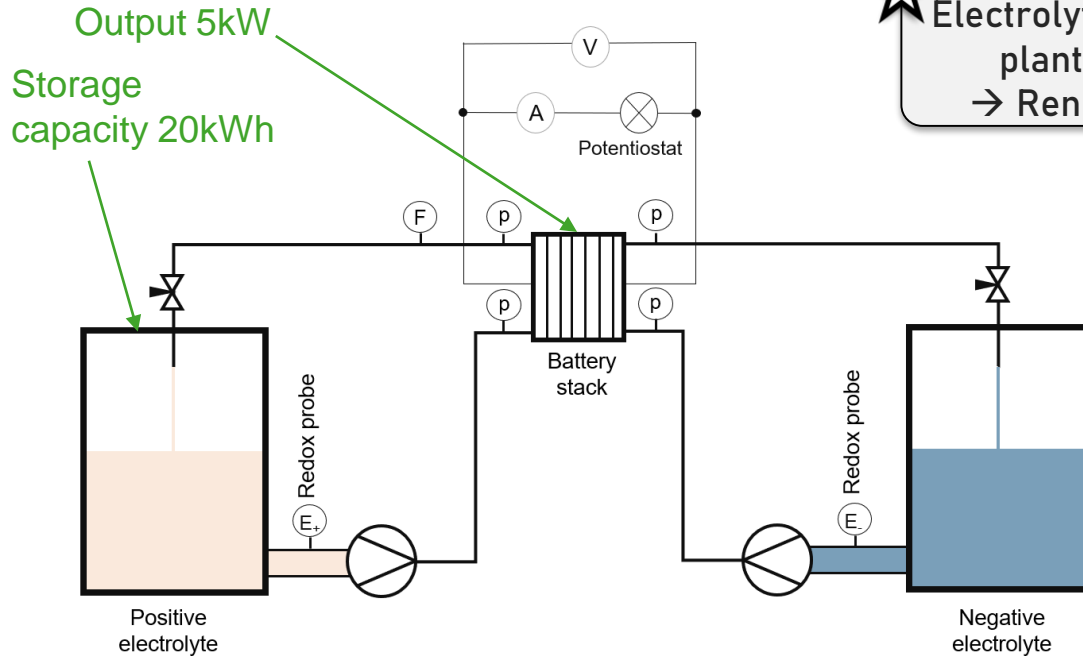
**Thomas Reiter-Nigitz**  
 Johannes Niederwieser  
 Uwe Poms  
 Dominik Wickenhauser  
 Stefan Spirk  
 Markus Gölles







# Research demonstrator of a renewable flow battery



★ Electrolyte is synthesized from plant-based resources  
→ Renewable flow battery

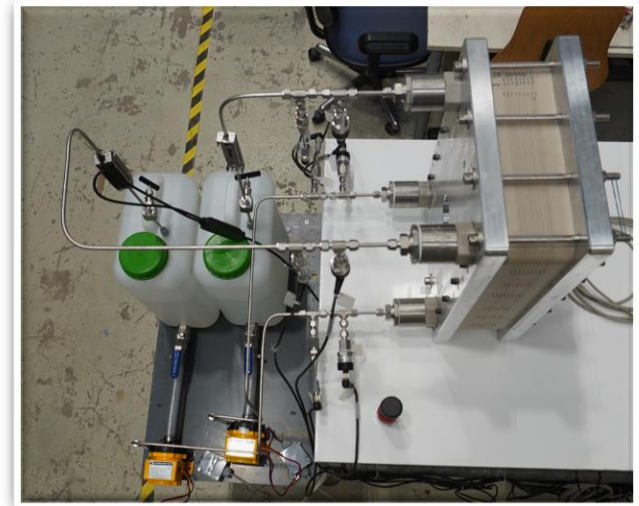
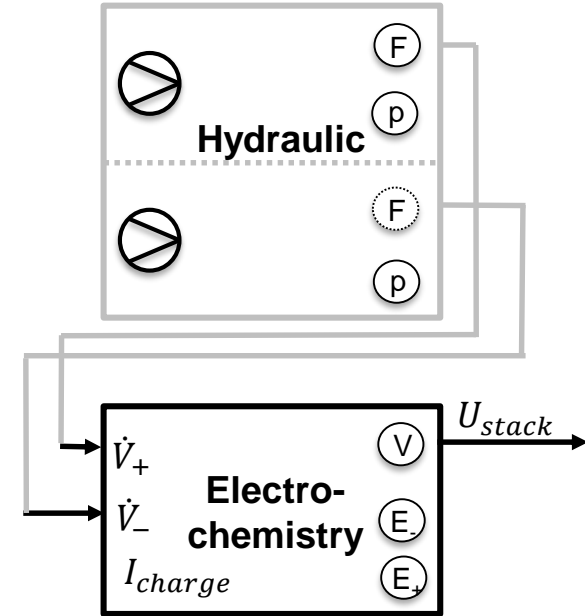
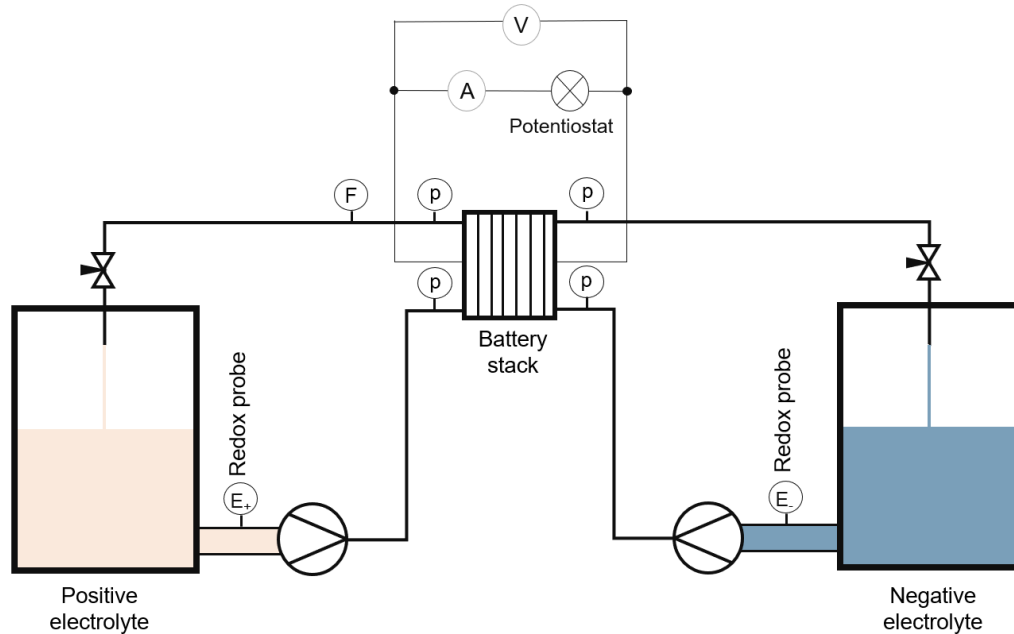


Photo © BEST



# Redraw the research demonstrator with block diagrams



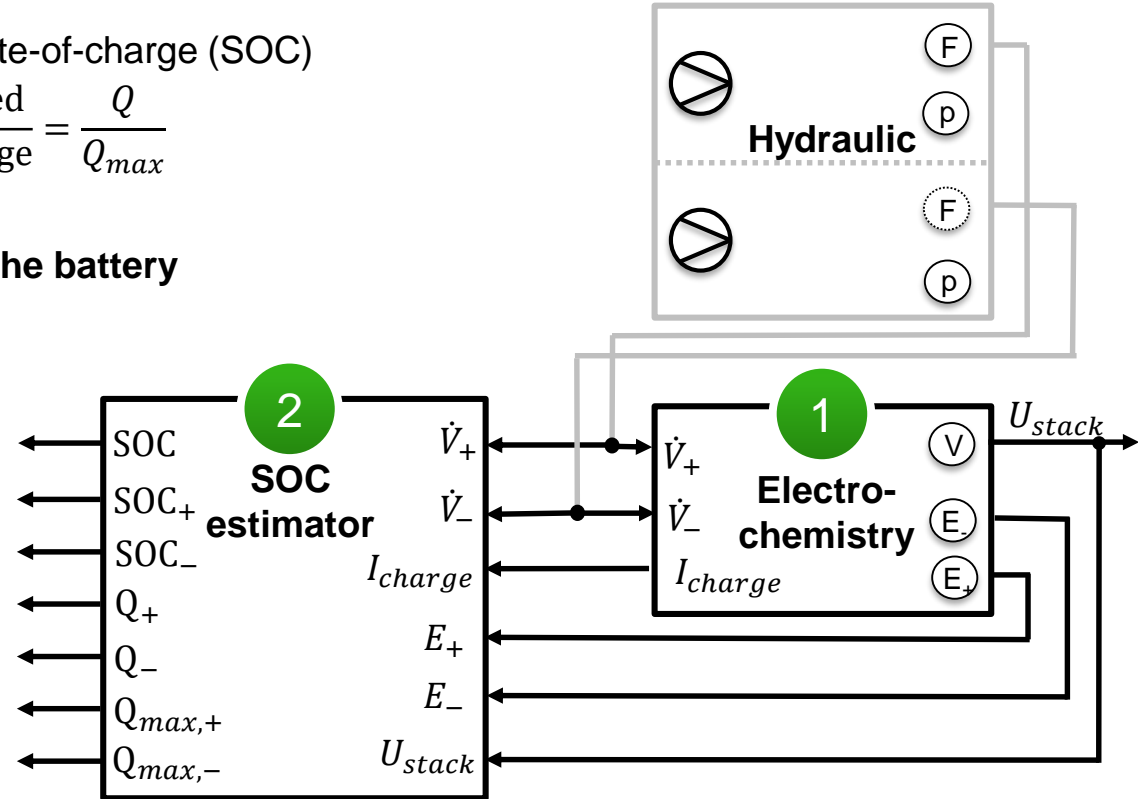
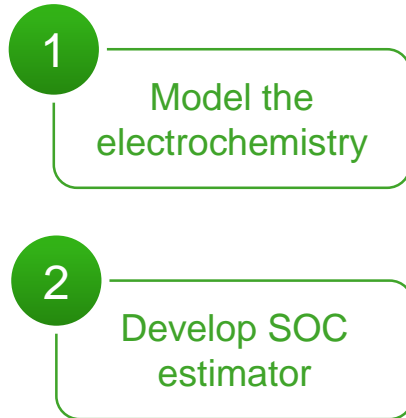


# Monitoring task

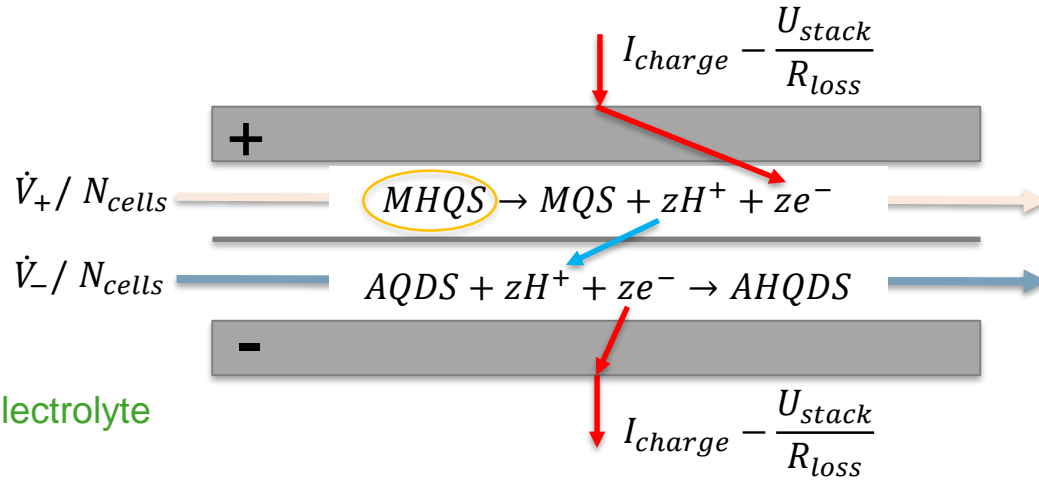
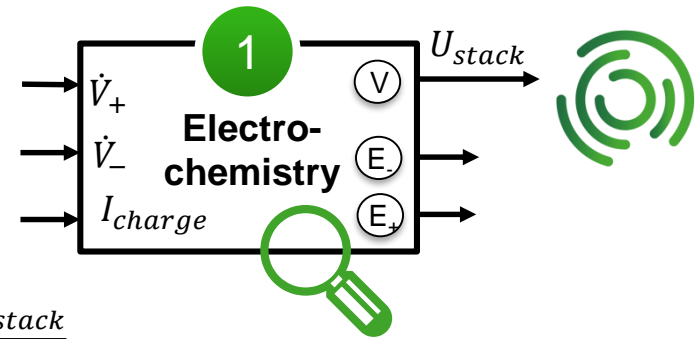
- Main monitoring variable is the state-of-charge (SOC)

$$\text{SOC} := \frac{\text{charge currently stored}}{\text{maximal storable charge}} = \frac{Q}{Q_{max}}$$

- SOC is NOT directly measurable
- **Estimate the state-of-charge of the battery**



# Detail: Model concentration of single species in one cell



Volume of one electrolyte in one cell

$$\frac{V_{stack}}{N_{cells}} \frac{dc_{MHQS,stack}}{dt} = \frac{\dot{V}_+}{N_{cells}} (c_{MHQS,tank} - c_{MHQS,stack}) - \frac{(I_{charge} - \frac{U_{stack}}{R_{loss}})}{zF}$$

Change of concentration due to volume flow

Change of concentration due to electric current

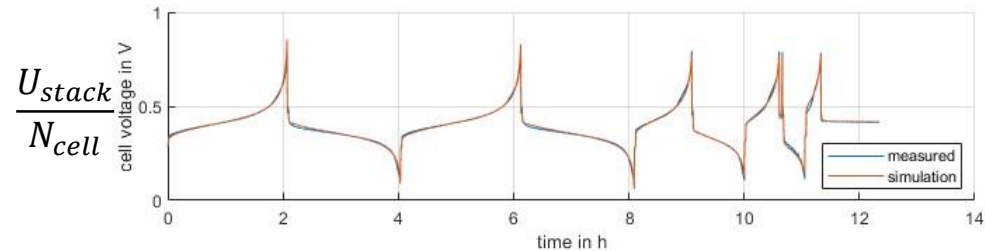
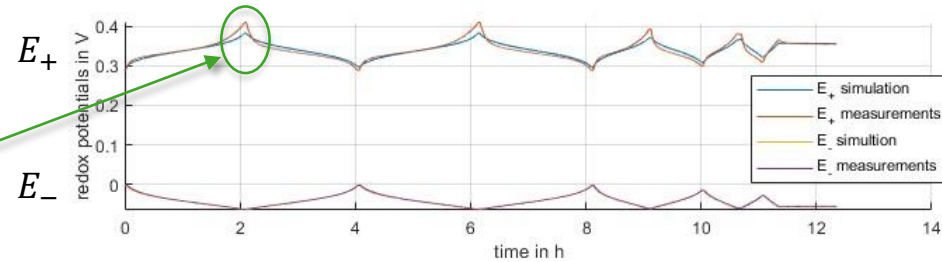
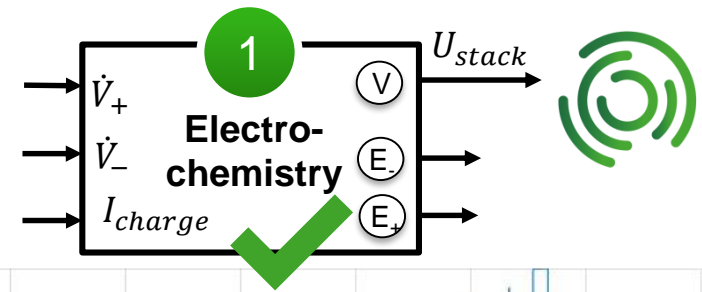
# Electrochemistry model: Validation

- Volume flows are kept constant
- Electric current alternates between charging and discharging
- Redox potentials and stack voltage can be described by the electrochemistry model

Model error at high SOC's



The developed electro-chemistry model can be used for SOC estimation



# SOC estimator: Validation

## Comparison

- of charge  $Q$  from SOC estimator
- with charge  $Q$  from coulomb counting

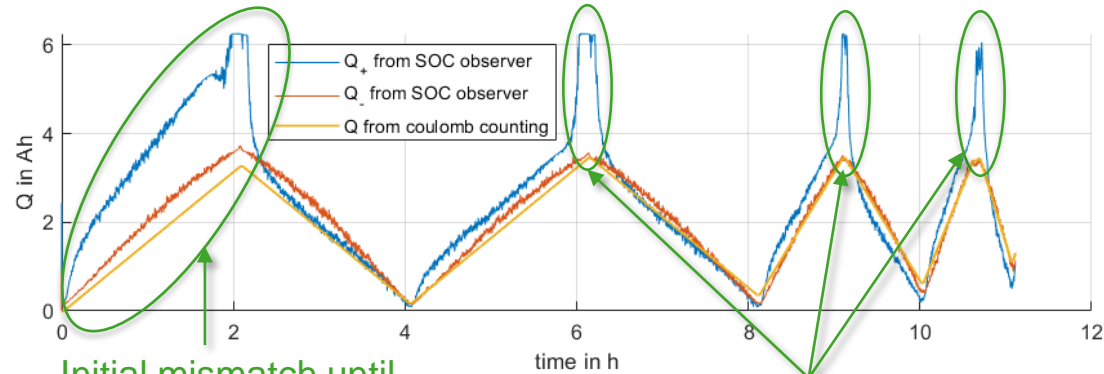
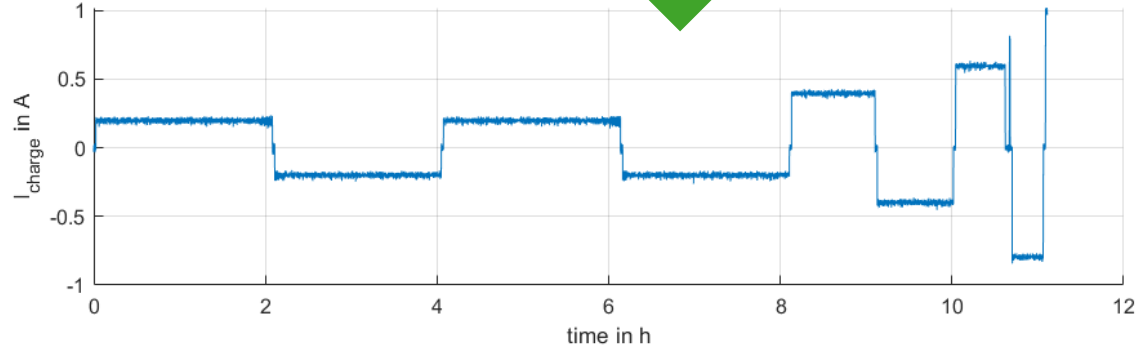
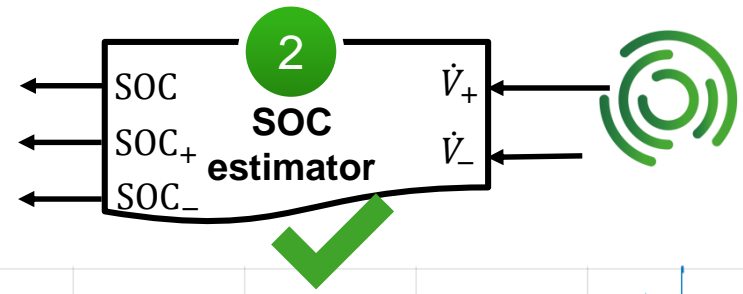
$$Q(t) = N_{cells} \int_0^t I_{charge}(\tau) d\tau$$

- Measurement data is chosen such that  $Q(0) = 0$  is a valid initial condition for the coulomb counting.

- Electric current alternates between charging and discharging



SOC estimator provides information about both electrolytes



Initial mismatch until SOC observer converges

Effect of model error at high SOC's

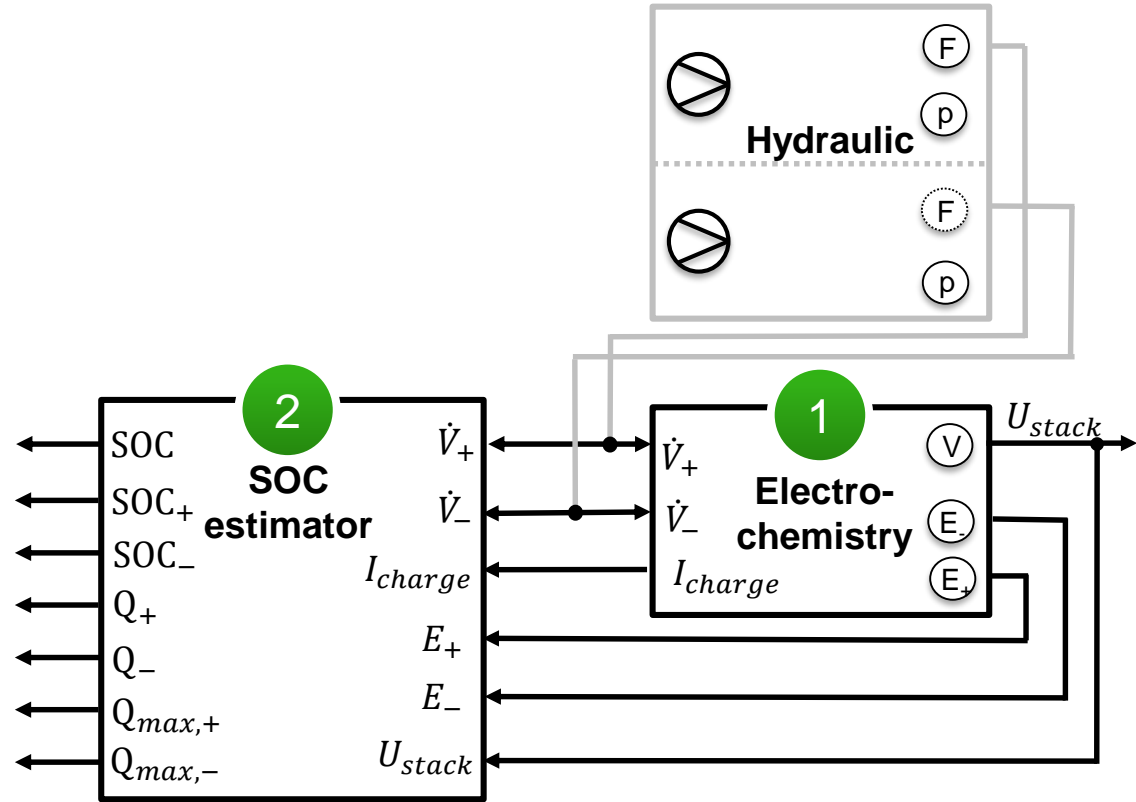
# Conclusion



★ Electrolyte is synthesized from plant-based resources  
→ Renewable flow battery

★  
1 The developed electro-chemistry model can be used for SOC estimation

★  
2 SOC estimator provides information about both electrolytes



# Use cases of optimally planned multi-energy systems with OptEnGrid: hotel resort and renewable energy communities


26.09.2024, Graz

Laurin Zillner

Area 2.3 Microgrids and Smart Energy Communities



 Bundesministerium  
Arbeit und Wirtschaft

 Bundesministerium  
Klimaschutz, Umwelt,  
Energie, Mobilität,  
Innovation und Technologie



 Für die  
Stadt Wien



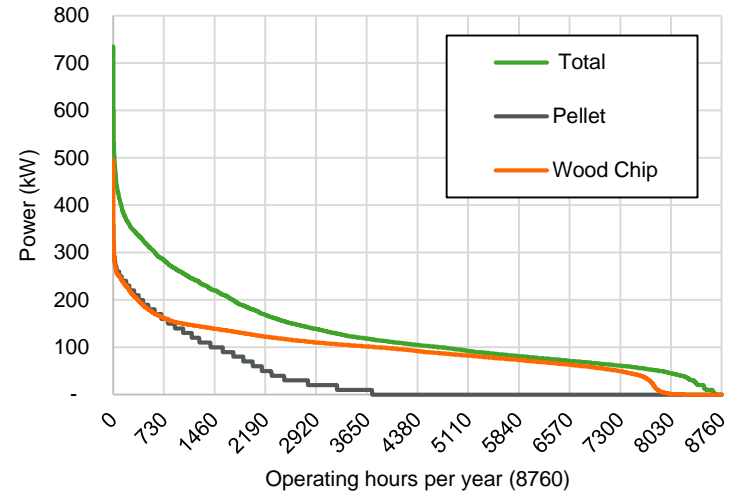




# Hotel Resort Kothmühle



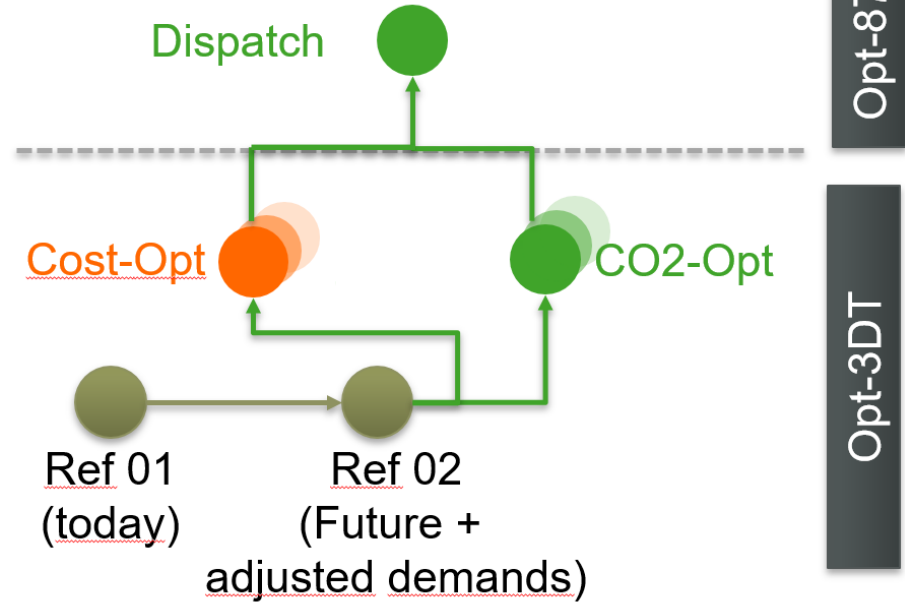
- 4 Star wellness and seminar hotel
- Planned:
  - Wellness area to be expanded
  - Laundry in house
  - Thermal insulation
  - E-charging stations to be expanded
- The goal is to be as self-sufficient as possible, through renewable energies



# Hotel Resort Kothmühle

Holistic optimized planning in OptEnGrid:

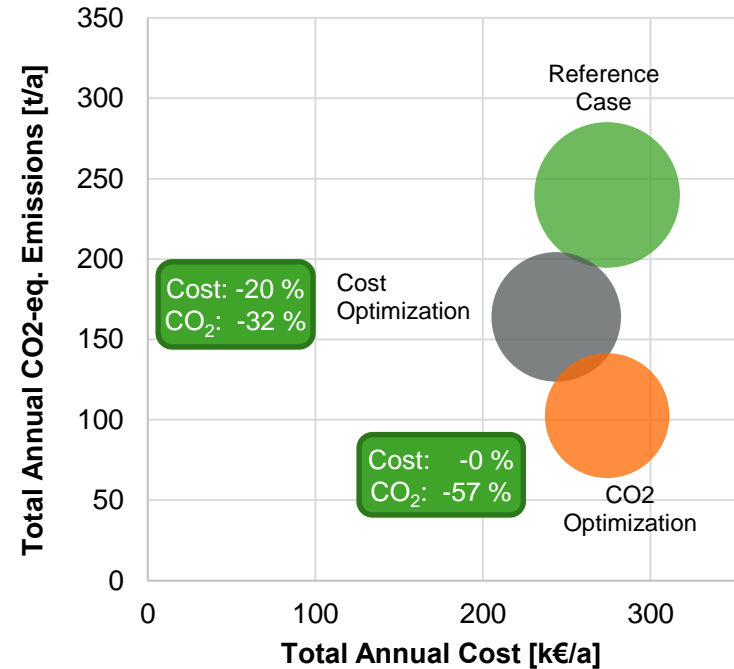
- PV-planning
- Modernisation of old systems
- Complex use case
  - 5 energy profiles used
  - Various technologies





# First Results Kothmühle

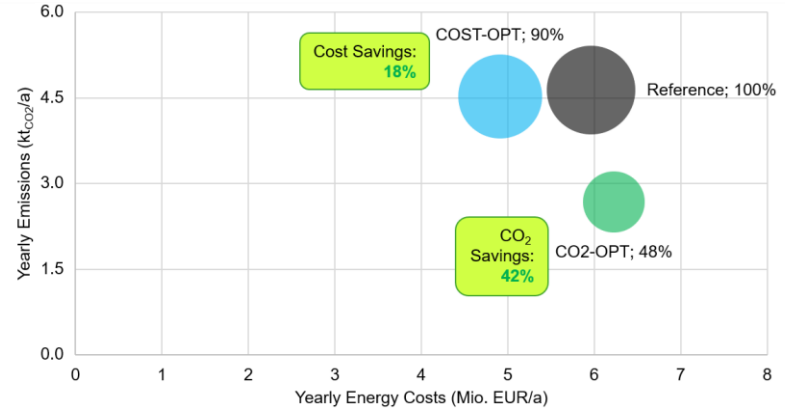
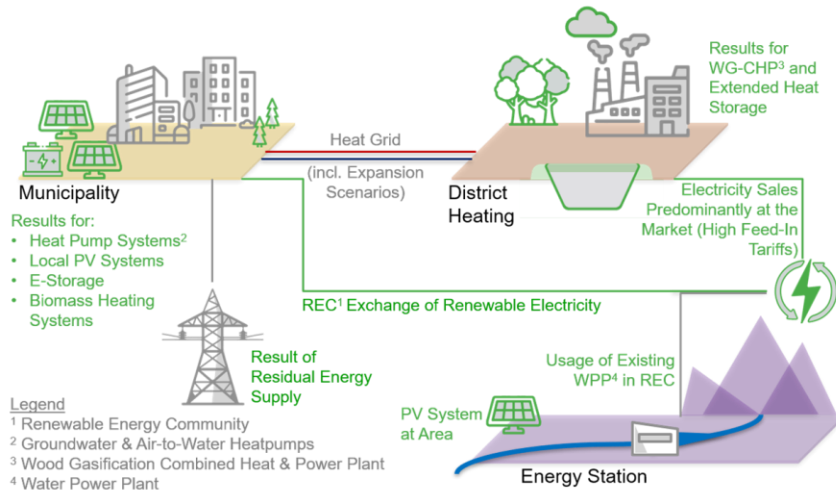
- Maximum PV installation 261kWp
- Battery storage system 65 kWh
- Expansion of heat storage +50 kWh
- Integration of cold storage 40 kWh
- Wood chip CHP 250kW<sub>e</sub> & 500kW<sub>th</sub>





# Optimized Planning of Energy Systems in more than 10 Austrian Communities

- Increasing the share of renewable energy technologies
- Increasing local energy self-sufficiency
- Achieving cost and CO<sub>2</sub> reductions



Public Grid Consumption of 100% = Reference Case  
 Public Grid Consumption of 0% = Total Self-Sufficiency



Adnet, Grödig, Hinterglemm, + 9 Ski Resorts



Maria Rain, Mallnitz



Perchtoldsdorf, Wieselburg, Wieselburg-Land



Ötztal, + 1 Ski Resort

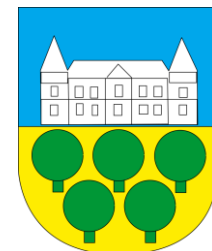
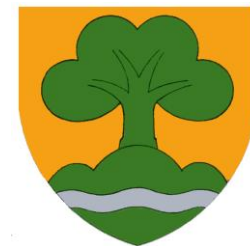


Möllersdorf, Mureck

# Renewable Energy Communities: InRegion South & InRegion North

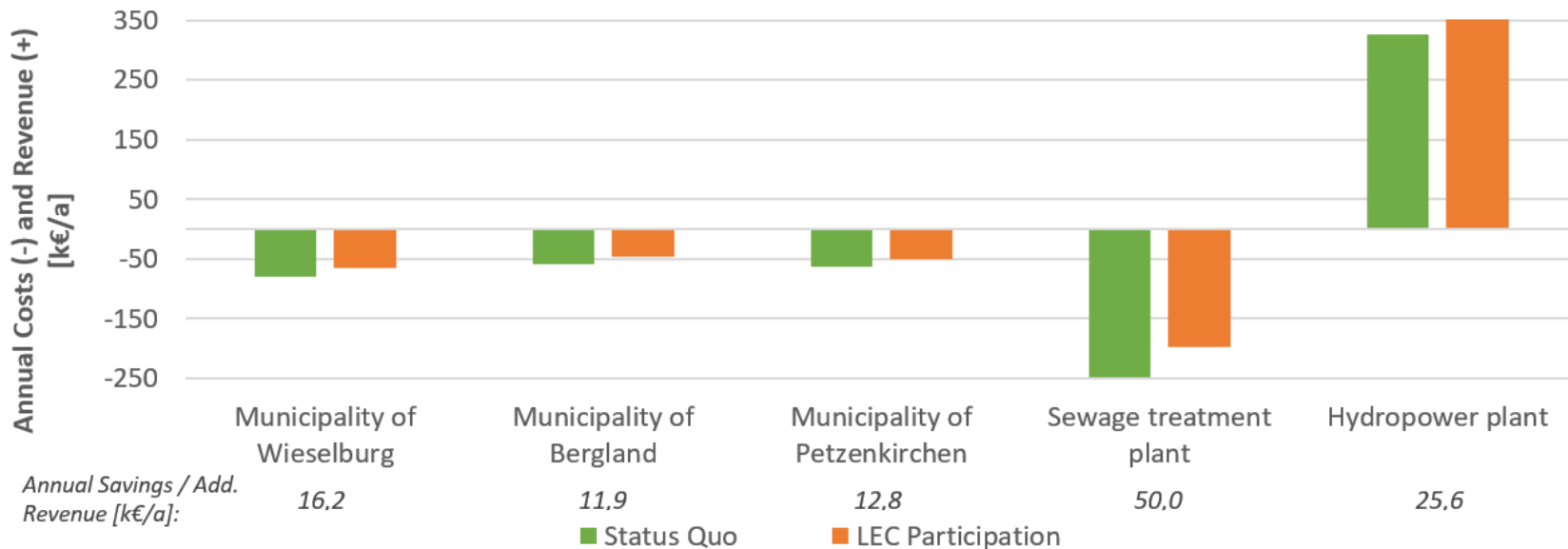


- 4 participating municipalities
- The goals of the project were to
  - Use most of the local generated electricity locally
  - Save money on energy purchases
- Division into 2 LECs due to grid levels
- Involved metering points were mostly municipality owned
  - South 111 metering points
  - North 48 metering points





# Renewable Energy Communities: InRegion North economic results



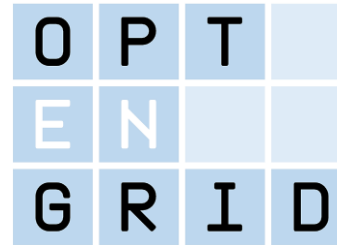
# Conclusion

- Complex data & data procurement
- Significant cost & emission reduction possible
- 2 Different time-resolution models
  - 8760 model: Precise operating schedules
  - 3D model: Fast calculations
- Challenge: no Standard use case → every project is unique
- Advantage: Because of the high flexibility a wide variety of projects are possible



# Optimal Design of Multi-Energy Systems using OptEnGrid

26.09.2024, Graz



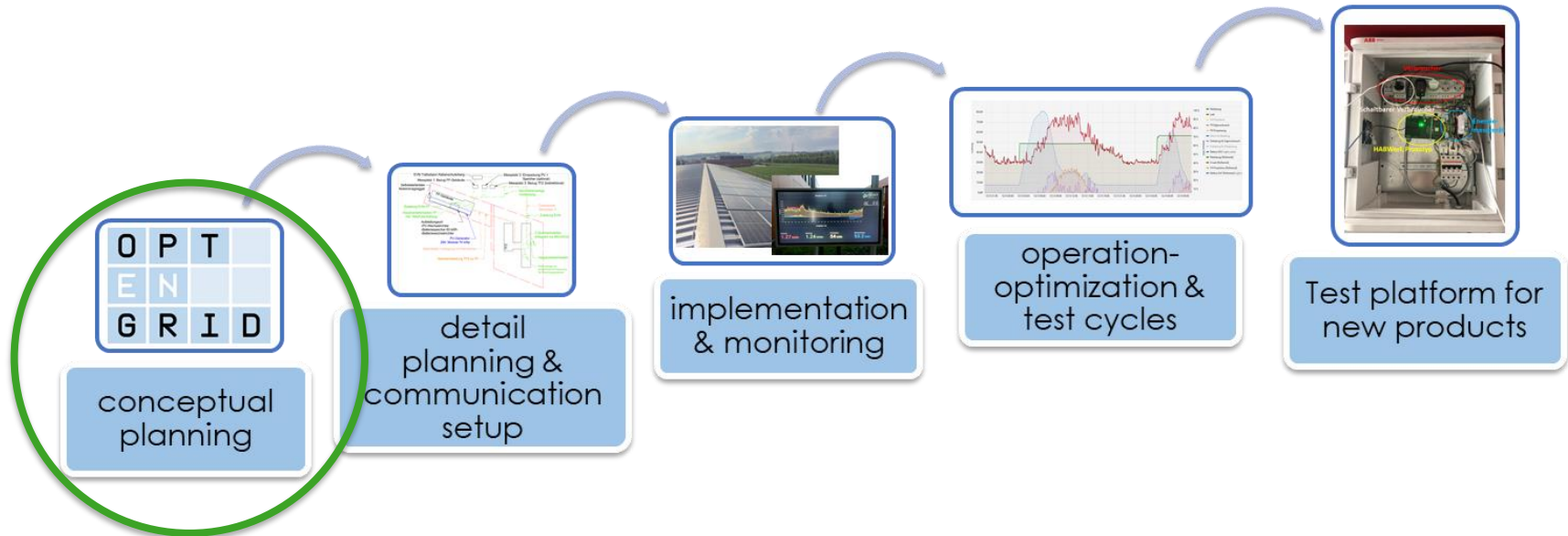
Christian Oberbauer  
Area 2.3 Microgrids and Smart Energy Communities





# Implementation Process of Decentralized (Multi-) Energy Systems

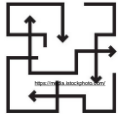
- Optimal planning of decentralized energy systems → OptEnGrid
- Testing and optimization of hard- and software in real use cases → Microgrid Lab



# Holistic Design of Multi-Energy Systems



## Challenges:



- **High complexity** related to the diversity of:
  - Sectors (electricity, heating, cooling, mobility, ...)
  - Energy sources (fossil and renewable fuels, etc.)
  - Technologies (generation, conversion, storage)

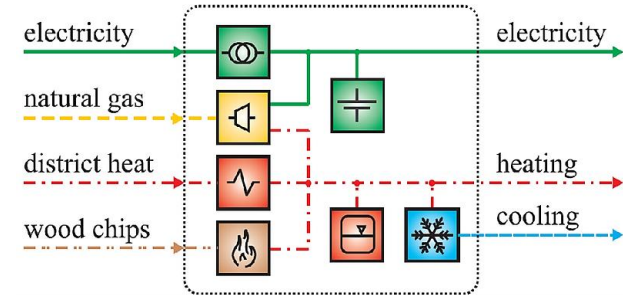


- Conventional planning methods **do not provide an "optimal" result** in terms of
  - Costs and emissions – due to oversizing
  - Calculation effort → high implementation costs

## Solution = mathematical optimization with OptEnGrid



- Simultaneous determination of optimal design in terms of
  - Capacities and operating schedule (hourly)
  - Costs (investment, O&M, fixed costs, energy tariffs)
  - and CO<sub>2-eq.</sub> emissions





# OptEnGrid: History & Validation



- 2000-2018: Development of DER-CAM<sup>1</sup> at LBNL<sup>2</sup> in Berkeley, California a.o. by Michael Stadler (founder of Area 2.3 at BEST); >1.500 users/institutions in >24 countries



- 2017- today: **advanced development** & renaming to **OptEnGrid**<sup>3</sup> at BEST as part of research projects:

→ **Extension of the optimization model**

O	P	T	
E	N		
G	R	I	D



- 2019 – 2022: **Validation** of OptEnGrid based on a **real use case**:
  - **Microgrid Lab** at the Technical Research Centre Wieselburg-Land, Lower Austria
  - Planning → implementation → monitoring → operation with the Microgrid Controller

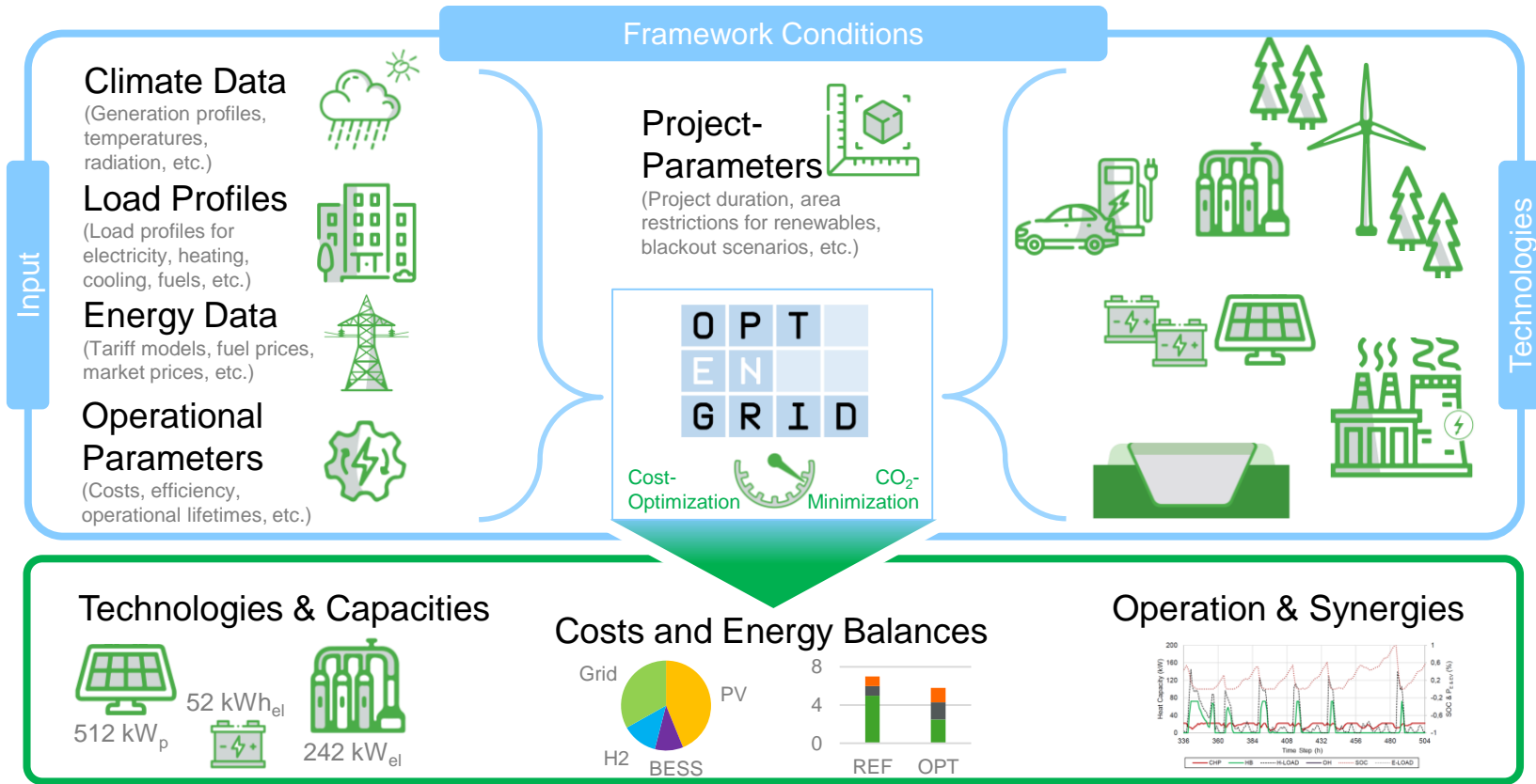
<sup>1</sup> Distributed Energy Resources – Customer Adoption Model

<sup>2</sup> Lawrence Berkeley National Laboratory

<sup>3</sup> Optimized Energy Grid

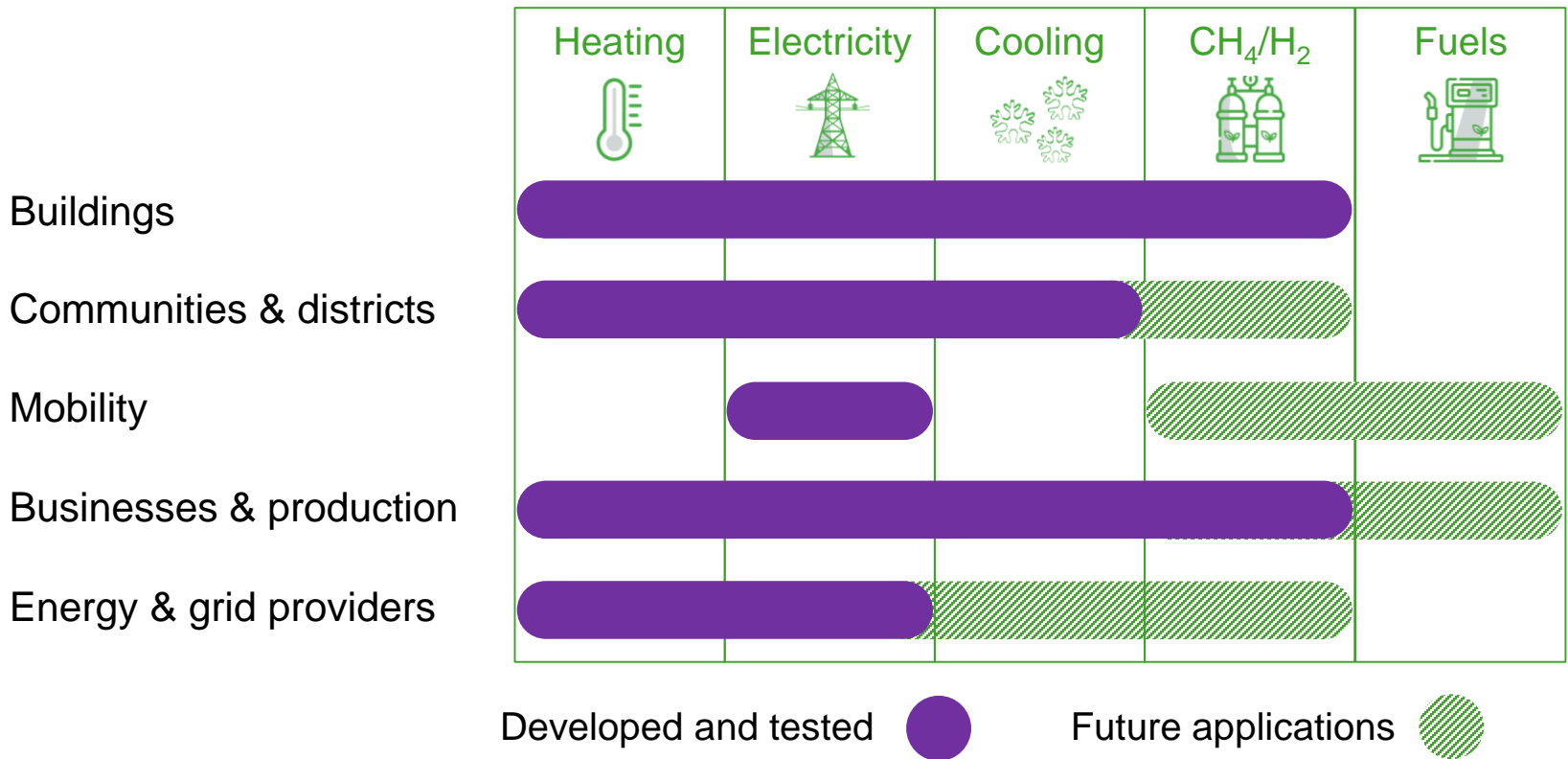


# Big Picture - Workflow





# Application Fields of OptEnGrid

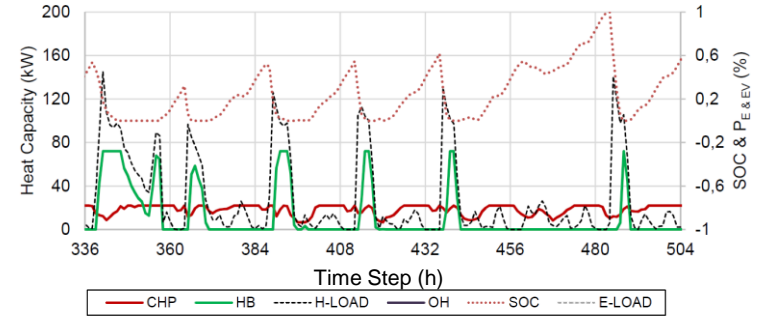




# Benefits, Potentials of OptEnGrid & Comparison of similar Tools

## Benefits:

- Determination of the optimal **technology-mix** with rated capacities & **operational dispatch**
- **Average savings<sup>1</sup>:**
  - ~ **15 to 27% cost savings**
  - ~ **8 to 87% emission savings**



## Potentials in Austria:

- 2.093 municipalities
- > 2.400 heating grids<sup>2</sup>
- ~ 5.000 energy communities<sup>3</sup>

Tool	Simulation		Optimization		Residential		District		Multiple Nodes		Day Types		Hourly		Objective Function		Utilized Technologies		Performance		Availability	
	Simulation	Optimization	Residential	District	Multiple Nodes	Day Types	Hourly	< hourly (30/15min)	CO <sub>2</sub> -Minimization	Other Objectives	Electricity	Heating	Cooling	Hydrogen	Mobility	Fuels	Energy Communities	Quick Results	Open Source			
OptEnGrid	0	1	1	1	1	1	1	1	1	0	1	1	0	1	1	1	1	1	1	1	1	0
HOMER	1	1	0	1	1	1	1	1	0	1	0,5	0	1	1	1	1	1	1	1	0	1	0
Reopt*	1	1	0	1	1	0	1	1	1	1	1	1	1	1	1	0	0	1	0	1	0	1
nPRO	0	1	1	1	0	1	0	1	0	1	0,5	0	1	1	1	1	1	1	0,5	1	0	1
urbs	0	1	0	1	1	0	1	0,5	1	1	0	1	1	0	0	0	0	0	0	0	0	1
ESYOPT*	0	1	1	1	?	0	0	1	1	1	1	1	1	1	0	0	0	1	0	?	0,5	?
KomMod	0	1	1	1	1	0	1	1	0,5	0	1	1	1	1	0	0,5	1	0	0,5	1	0	1
plan4energy	0	1	?	1	1	?	?	?	?	?	?	?	?	?	?	0,5	?	?	?	?	?	?
ENDOPT	0	1	0	1	1	?	?	?	?	1	1	0	1	0	0	0	0	0	0	0	0	?
Planungstool-EEG	0	1	0	1	1	?	?	?	?	1	1	0	1	1	1	?	0,5	?	?	?	?	?

## Advantages:

- ✓ Flexible Application
- ✓ Multi-Energy-Systems
- ✓ Energy Communities
- ✓ Fast Results

<sup>1</sup> <https://doi.org/10.1016/j.apenergy.2023.12091>; <https://doi.org/10.1016/j.energy.2021.121559>; [https://www.best-research.eu/files/publications/pdf/Liedtke\\_Ganzheitliche\\_Planung\\_DER.pdf](https://www.best-research.eu/files/publications/pdf/Liedtke_Ganzheitliche_Planung_DER.pdf)

<sup>2</sup> <https://www.klimafonds.gv.at/wp-content/uploads/sites/16/FEFahrplan-FernwaermeFernkaelte.pdf>

<sup>3</sup> <https://www.eda.at/fakten>

# Summary and Outlook – Future Developments



- **Advanced web-based graphical user interface** for ease of use and broad application (from private individuals to planners and energy consultants)
- **Automated data collection** for simplified and scalable planning processes (e.g. linked to GIS-databases)
- **Commercial planning tool** for utilities, industry, municipal planners and policy makers





# Sustainability assessment: mere obligation or a key to success?

Graz, 26.09.2024

Christa Dißauer, Monika Enigl, Marilene Fuhrmann,  
Doris Matschegg, Christoph Strasser



 Bundesministerium  
Arbeit und Wirtschaft

 Bundesministerium  
Klimaschutz, Umwelt,  
Energie, Mobilität,  
Innovation und Technologie



 Für die  
Stadt Wien





# What does „sustainability“ mean?



- United Nations Brundtland Commission 1987:

*„meeting the needs of the present without compromising the ability of future generations to meet their own needs“*

- The Environmental Protection Agency:

*„sustainable development and environmental factors relate to just about everything - including the ability to generate social sustainability, promote economic prosperity, and reach economic objectives“*

## SUSTAINABLE DEVELOPMENT GOALS



# The 3 dimensions of sustainability



- Ecological pillar
  - Protect the environment by reducing risks of organizations' activities
  - Saving and preserving natural energy or agricultural resources
  - Prevent water scarcity and reduce overall waste for current and future generations
- Social pillar
  - Promote equality and respect for individual rights, combat social exclusion and discrimination
  - Promote solidarity – e.g., prioritizing fair trade products
  - Contribute to the well-being of stakeholders – e.g., encouraging the exchange of information and transparency
- Economic pillar
  - Fostering Innovation and Adaptation
  - Promoting resource efficiency and minimizing waste throughout the production and consumption processes
  - Ensuring Financial Stability and resilience to external shocks and crises



# New rules on corporate sustainability reporting: The Corporate Sustainability Reporting Directive

On 5 January 2023, the [Corporate Sustainability Reporting Directive \(CSRD\)](#) entered into force

- **What?** modernises and strengthens the rules concerning the social and environmental information that companies have to report
- **Who?** Large companies, as well as listed SMEs and some non-EU companies if they generate over EUR 150 million on the EU market
- **Why?** To ensure that investors and other stakeholders have access to the information they need to assess the impact of companies on people and the environment and for investors to assess financial risks and opportunities arising from climate change and other sustainability issues
- **When?** The first companies will have to apply the new rules for the first time in the 2024 financial year, for reports published in 2025

# European Sustainability Reporting Standards



- Companies subject to the CSRD will have to report according to European Sustainability Reporting Standards (ESRS)
- The directive also requires verification of the sustainability information reported by companies and provides for a digital taxonomy for the electronic submission of sustainability information to the company register (Firmenbuch)
- The responsible department of the Federal Ministry of Justice has prepared an initial draft of a federal law (**Nachhaltigkeitsberichtsgesetz – NaBeG**) for implementation - the draft is currently undergoing political consultation



# European Sustainability Reporting Standards

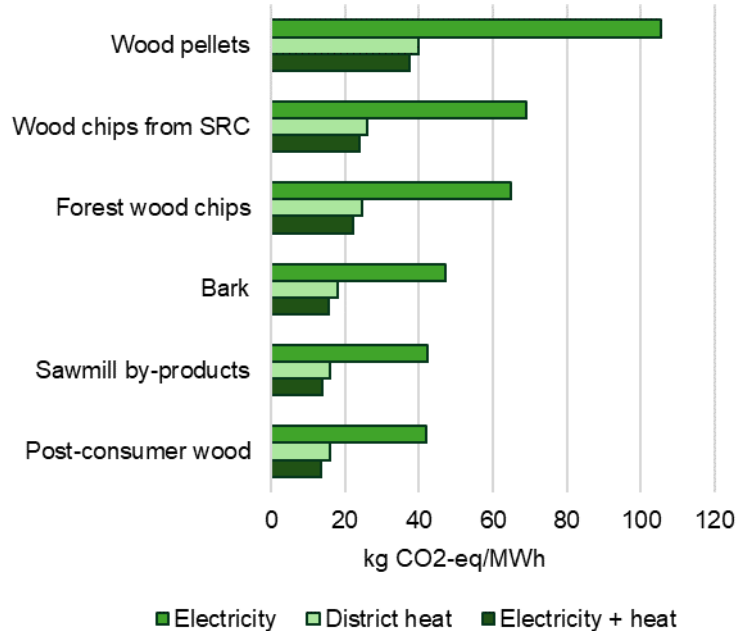
- Companies subject to the CSRD will have to report according to European Sustainability Reporting Standards (ESRS)
- The directive requires companies to report on sustainability information reported by companies. The question is: How to obtain scientifically based data required for reporting? Submission of information reported by companies.
- The responsible department of the Federal Ministry of Justice has prepared an initial draft of a federal law (**Nachhaltigkeitsberichtsgesetz – NaBeG**) for implementation - the draft is currently undergoing political consultation



# Sustainability assessment & science-based reporting support @BEST

- **BEST sustainability Quick-Check**
  - A quick check for the biobased systems and processes to identify “sustainability hot spots”
- **Life Cycle Assessment (LCA)**
  - LCA is a technique for assessing the environmental aspects associated with a product over its life cycle
- **Techno-Economic Assessment and Life Cycle Costing (LCC)**
  - Life cycle cost assessment is an economic evaluation of a product or an engineering project across its lifetime
- **The Bio-Value-Tool** (first developed in the BioEcon project as “**Wood-Value-Tool**”)
  - The calculation tool enables a techno-economic assessment of selected biomass value cycles; integrating the sustainability criteria facilitates to derive recommendations regarding sustainable supply and distribution strategies as well as to increase the resilience of bio-based systems
- **Social-Risk Matrix**

# Example: Global Warming Potential



kg CO <sub>2</sub> -eq/MWh	
Heating oil	344
Natural gas	249
AT electricity mix	226
AT district heat	179

## BIOSTRAT

Strategies for the optimal bioenergy use in Austria from societies point-of-view – Scenarios up to 2050

**Partners:** BEST GmbH  
 Austrian Research Centre for Forests (BFW)  
 Energy Economics Group, TU Wien  
 Subcontractor: Göran Berndes (IEA Task 45, TU Chalmers)

**Funding:** Austrian Climate Research Programme (ACRP)

# Sustainability assessment: a key to success



Sustainability assessment helps with

- identifying sustainability hotspots
- supporting the decision making process
- evaluating tradeoffs
- evaluating the effectiveness of actions taken
- tracking progress
- meeting new requirements
- establishing reward mechanisms and
- communicating goals and achievements

## Top 3 reasons that organizations address sustainability\*

- 1. Alignment**  
Align with company's business goals, mission or values
- 2. Reputation**  
Build, maintain, or improve corporate reputation
- 3. Cost cutting**  
Improve operational efficiency and lower costs

\*McKinsey Global survey results „Sustainability's strategic worth“  
2010-2018

**Sustainable as well as resilient biomass supply and technologies are key factors for the success and competitiveness of bio-based businesses**